



Report:

Mercury Emission Testing at the Clean Harbors Sarnia Facility (January 2018)

Date: February 8, 2018





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EXECUTIVE SUMMARY

ORTECH Consulting Inc. (ORTECH) was requested by Clean Harbors Canada Inc. (Clean Harbors) to conduct a mercury emission testing program at the incineration facility located in Corunna, Ontario.

Mercury emission tests were performed at the Incinerator Exhaust Stack following the procedures outlined in US EPA Method 30B, "Determination of Total Vapour Phase Mercury Emissions from Coal-Fired Combustion Sources Using Carbon Sorbent Traps" to determine the amount of total vapour phase mercury present in the gas stream.

The test method states that the recovery spike must be within 50 to 150 percent of the expected mass collected in the traps during sampling. Six pairs of tube samples were collected during one day of testing on January 10, 2018. To ensure that at least one of the spike concentrations would fall within the concentration range requirements of the test method one tube from each of the six pairs of adsorbent tubes were spiked with increasing amounts of mercury, ranging from 100 ng to 2600 ng, by the analytical laboratory prior to commencing the test program.

The results of three of the pairs of tubes, including the spike that best represented the mercury concentration in the stack gas at the time of testing, are reported.

The average combustion gas values for each test period were obtained from the plant continuous emission monitoring (CEM) system. The average oxygen concentration for each test was used to determine the dry reference concentration adjusted to 11% oxygen.

The average mercury emission data from the triplicate total vapour phase mercury tests reported is provided below:

Mercury Parameter	Average
Dry Reference Concentration (µg/Rm ³)*	2.33
Dry Adjusted Concentration (µg/Rm ³)**	2.26

* reference conditions are 25°C and 1 atmosphere

** at 25°C and 1 atmosphere, adjusted to 11% oxygen

During the emission testing program, the powdered activated carbon (PAC) injection rate was 22.4 lb/hr.



1. INTRODUCTION

ORTECH Consulting Inc. (ORTECH) was requested by Clean Harbors Canada Inc. (Clean Harbors) to conduct a mercury emission testing program at the incineration facility located in Corunna, Ontario.

Mercury emission tests were performed at the Incinerator Exhaust Stack following the procedures outlined in US EPA Method 30B to determine the amount of total vapour phase mercury present in the gas stream.

The average combustion gas values for each test period were obtained from the plant continuous emission monitoring (CEM) system. The average oxygen concentration for each test was used to determine the dry reference concentration adjusted to 11% oxygen.

Six pairs of adsorbent tubes were collected during one day of sampling on January 10, 2018. The spike tubes from each test pair were spiked with increasing amounts of mercury, ranging from 100 ng to 2600 ng, prior to commencing the test program to ensure that at least one of the spike concentrations would fall within the concentration range requirements of the test method. The test method states that the recovery spike must be within 50 to 150 percent of the expected mass collected in the traps during sampling. The results of three of the pairs of tubes, including the spike that best represented the mercury concentration in the stack gas at the time of testing, are reported.

All tables referenced herein are included in Appendix 1.

2. SAMPLING LOCATION

The Incinerator Exhaust Stack has an inside diameter of 1.52 meters at the sampling platform and 1.22 meters at the stack exit. The stack height above grade is 68.6 meters.

Mercury sampling was conducted at the breeching connecting the induced draft fan to the stack. Sampling was conducted at a single point in the center of the duct.

Previous testing programs conducted by ORTECH at the Clean Harbors Incinerator Exhaust Stack have shown that there is no stack gas stratification between the breeching connecting the induced draft fan to the stack and the stack sampling platform location.



3. SAMPLING METHODOLOGY

Mercury emission tests were performed following the procedures outlined in US EPA Method 30B, "Determination of Total Vapour Phase Mercury Emissions from Coal-Fired Combustion Sources Using Carbon Sorbent Traps".

ORTECH used a dual probe assembly so that the mercury traps are positioned 1 to 2 inches apart. Each probe was heated to approximately 135°C to prevent condensation of the stack gas on the sampling media. Each mercury trap was also specially designed for sampling at wet sources. Each tube had an extended section of glass to allow for the heating of the stack gas before it came into contact with the sampling media.

The sampling methodology is briefly described as follows. Each sorbent trap was removed from the clean sorbent trap storage container, the end caps were removed from the traps and the traps were attached to the end of the sampling probe and leak checked. The probe was inserted into the stack and the sample pumps were started. Stack gas was drawn through the traps and into the sampling probe and the sampled gas stream then passed through a series of empty impingers followed by a silica gel trap to remove any remaining traces of moisture prior to the pump and dry gas meter.

A run consisted of paired mercury traps, identified as either A or B, sampled simultaneously. In each tube pair one of either the A or B tube was spiked with a known quantity of mercury. Due to the variability in the mercury concentration in the stack gas and the necessity to have the spiked tubes prepared at least two weeks in advance of the testing program, six pairs of tubes were used for the sampling program to ensure that at least one of the spike concentrations would fall within the concentration range requirements of the test method.

Each test run was sixty minutes in duration at an approximate sampling rate of one liter per minute.

At five minute time increments throughout each test, the following information was measured and recorded for each sampling train:

- Elapsed sampling time
- Dry gas meter volume
- Dry gas meter temperatures
- Control module orifice pressure
- Sampling pump vacuum



At the start and finish of each sampling run the sampling trains were leak-checked. The leakage rate for each train must not exceed 4% of the average sampling rate for the collection period. If a trap pair did not have an acceptable initial leak check, the leak was found and repaired and/or the traps were replaced with a new pair until no leak was discernible. All the leak checks performed for the traps used showed no discernible leak through the test train.

Field testing data sheets for the mercury tests are provided in Appendix 2.

All of the sampling equipment used during the emission testing program was calibrated following the applicable reference method. Equipment calibration data is provided in Appendix 3.

4. ANALYSIS METHODOLOGY

At the end of each successful sampling run, the mercury traps were removed from the test train, capped and placed in their appropriate sample container. Each trap was labeled prior to being shipped to Ohio Lumex for analysis.

The traps were analyzed by thermal decomposition with atomic absorption following the procedures detailed in US EPA Method 7473 (direct thermal desorption with atomic absorption and no gold amalgamation). The method is applicable for total mercury "direct" testing of 40 CFR Part 75 Appendix K and EPA Method 30B sorbent traps.

The analysis is briefly described as follows. The sorbent trap tube end cap is removed; the glass wool plug closest to the appropriate carbon bed is carefully removed and separated from the carbon fraction. The sorbent is transferred into a quartz ladle and then covered with anhydrous sodium carbonate. The ladle is inserted into the heated analyzer thermo catalytic conversion chamber. Mercury is converted from a bound state to the atomic state by thermal decomposition in the furnace and is then detected by atomic absorption. The mercury concentration is measured and recorded using an automated data acquisition system. Both the glass wool plug and the sorbent of each bed are analyzed for the trap and the final mercury mass is the sum of the measurements.

The Ohio Lumex analytical report for total vapour phase mercury is provided in Appendix 4.



5. QUALITY ASSURANCE/QUALITY CONTROL PROGRAM

The analysis of samples for mercury was performed by thermal decomposition with atomic absorption. Specific analytical QC procedures for the mercury analysis are summarized below:

- Calibrations are performed on the day of the analysis.
- Three or more calibration points are used for the calibration curve.
- The field samples analyzed must fall within a calibrated range.
- For each calibration curve, $R^2 \ge 0.99$, and the analyzer response must be within ± 10% for each standard used in the calibration.
- Following calibration, a second source standard is analyzed. The measured value of the independently prepared standard must be within ± 10% of the expected value.
- A blank analysis is conducted prior to analyzing the samples and must be less than the method detection limit.
- At the end of each set of analysis, a calibration standard is tested which must be within ±10% of the expected value.

Six unspiked mercury traps and six pre-spiked mercury traps were ordered approximately two weeks before the field testing program from Ohio Lumex. The pre-spiked mercury traps were spiked with known quantities of mercury ranging from 100 ng to 2600 ng in order to ensure that at least one of the traps met the spiking criterion stated in the test method. The recovery spike must be within 50 to 150 percent of the expected mass collected in the traps during sampling according to the test method. The spiking levels for the field recovery traps was estimated using mercury emission data from previous testing programs conducted between 2014 and 2017. The pre-spiked mercury trap for Test No. 2 (250 ng) was used for spike recovery determination as the concentration best fit the requirements of the QA/QC criteria. The average mercury collected for Test No. 2, Test No. 4 and Test No. 5 (156 ng) was within 50% of the spike concentration (250 ng). The results from Test No. 1 and Test No. 3 were not used due to a suspected spiking error in the pre-spiked mercury traps that cannot be verified post-analysis.

The field spike recovery provides specific verification of the performance of the combined sampling and analytical approach for the test program. Six sets of paired samples, one of each pair which is spiked with a known quantity of mercury, were collected. The samples were analyzed and the spike concentration for Test No. 2 fell closest to the spike range criterion stated in the test method. The spike recovery for Test No. 2 was 108%. US EPA Method 30B requires the spike recovery to be between 85% and 115%.



US EPA Method 30B requires the paired sorbent trap agreement to be $\leq 10\%$ relative deviation for mercury concentrations greater than 1 µg/Rm³ or $\leq 20\%$ relative deviation for mercury concentrations less than 1 µg/Rm³. If the paired trap agreement is greater than the above stated limits the run is not valid. All of the traps collected during the test program had concentrations greater than 1 µg/Rm³. The average dry adjusted mercury concentration ranged from a low of 1.63 µg/Rm³ (Tube Pair No. 3, not reported) to a high of 2.74 µg/Rm³ (Tube Pair No. 1, not reported) for the six tests performed. The paired trap agreement was 5.8% for Test No. 2, 8.3% for Test No. 4, and 5.4% for Test No. 5.

6. **RESULTS**

Six mercury runs were collected during one day of sampling on January 10, 2018. A run consisted of paired mercury traps, identified as either A or B, sampled simultaneously. The spike tubes from each test pair were spiked with increasing amounts of mercury, ranging from 100 ng to 2600 ng, prior to commencing the test program to ensure that at least one of the spike concentrations would fall within the concentration range requirements of the test method. The results for Test No. 2, Test No. 4 and Test No. 5 are reported. The results from Test No. 1 and Test No. 3 were not used due to a suspected spiking error in the pre-spiked mercury traps that cannot be verified post-analysis.

The sampling schedule is summarized in Table 1. This information includes test dates and times for each of the mercury runs performed. All test times match plant time (i.e. daylight savings time).

Mercury emission sample analyses for Test No. 2, Test No. 4 and Test No. 5 are provided in Table 3. Mercury was detected in Section 1 of each trap in quantities greater than the method detection limit (0.46 ng) in all of the traps. Mercury was also collected in Section 2 in three of the six traps in quantities greater than or equal to the method detection limit. However, the amount detected in Section 2 was less than 0.8% of the mercury collected in Section 1, indicating that there was no breakthrough or potential loss of mercury. US EPA Method 30B states that <10% of the total mercury collected in Section 2 for mercury concentrations greater than 1 μ g/Rm³ or <20% of the total mercury collected should be collected should be collected in Section 2 for mercury concentrations less than 1 μ g/Rm³.

Included in Table 2 are the mercury concentration calculations for Test No. 2, Test No. 4 and Test No. 5. The average oxygen concentration measured by the Clean Harbors CEM system for each test was used to determine the dry reference concentration adjusted to 11% oxygen.

Six unspiked mercury traps and six pre-spiked mercury traps were ordered approximately two weeks before the field testing program from Ohio Lumex. The pre-spiked mercury traps were spiked with known quantities of mercury ranging from 100 ng to 2600 ng in order to ensure that at least one of the traps met the spiking criterion stated in the test method. The pre-spiked mercury traps for Test No. 2 (250 ng) was used for spike recovery determination as the concentrations best fit the requirements of the QA/QC criteria.



US EPA Method 30B states that it is acceptable to use the field recovery runs as test runs for emission testing as long as they meet the paired trap agreement criteria. The mass of the mercury spike initially present in each of the spiked traps was subtracted from the total mercury collected in Section 1 of the trap. The difference represents the amount of mercury in the stack gas.

The paired trap agreement was 5.8% for Test No. 2, 8.3% for Test No. 4, and 5.4% for Test No. 5. The mercury emission data from the total vapour phase mercury tests is provided below:

Mercury Parameter	Test 2	Test 4	Test 5	Average
Dry Reference Conc. (µg/Rm ³)*	2.50	1.93	2.57	2.33
Dry Adjusted Conc. (μg/Rm ³)**	2.54	1.87	2.38	2.26

- * Reference conditions are 25°C and 1 atmosphere
- ** At 25°C and 1 atmosphere, adjusted to 11% oxygen

The incinerator exhaust stack mercury concentration limit as stated in Environmental Compliance Approval No. 8-1030-94-006 (formerly Certificate of Approval (Air) No. 8-1030-94-006) is 50 μ g/Rm³ adjusted to 11% oxygen. The mercury concentrations were below this limit during the test program.

The spiked mercury trap recovery calculations for Test No. 2 are shown in Table 3; the spike recovery for Test No. 2 was 108.0%. US EPA Method 30B requires the spike recovery to be between 85% and 115%.

7. FACILITY PROCESS DATA

Incinerator process data was supplied by Clean Harbors personnel for the emission test periods. The process data is provided in Appendix 5 as average values for each test for the following process parameters:

- incinerator feed rates (rich, lean, emulsion and alkaline streams)
- volumetric flowrates (secondary air and stack gases)
- temperatures (primary zone, secondary zone, spray dryer inlet and outlet, stack gases)
- pressures (burner, spray dryer outlet, baghouse differential)
- combustion gas stack concentrations (CO, HCl, CO₂, H₂O, THC, O₂, SO₂)
- stack gas opacity
- carbon injection rate

During the emission testing program, the average powdered activated carbon (PAC) injection rate was 22.4 lb/hr.



APPENDIX 1

Data Tables (2 pages)



Table 1: Mercury Test Schedule

Test Number	Test Date	Samplin	g Period	Sampling Time
Number		Start	Finish	min
1	January 10, 2018	9:15	10:15	60
2	January 10, 2018	10:25	11:25	60
3	January 10, 2018	11:35	12:35	60
4	January 10, 2018	12:53	13:53	60
5	January 10, 2018	14:45	15:45	60
6	January 10, 2018	15:55	16:55	60

Note: All test times match plant time (i.e. daylight savings time).



Table 2: Mercury Emission Data

ID	Section 1	Section 2	Total	Volume	Dry	Dry	Trap
				Sampled	Reference	Adjusted	Agreement
	ng	ng	ng	Rm ³ *	µg/Rm ³ *	µg/Rm ³ **	%
	148.2	<0.46	148	0.0629	2.36	2.40	-
***	183.0	<0.46	183	0.0692	2.65	2.69	-
verage					2.50	2.54	5.8
	112.4	0.8	113	0.0640	1.77	1.71	-
***	148.7	0.7	149	0.0715	2.09	2.02	-
verage					1.93	1.87	8.3
***	165.0	1.9	167	0.0616	2.71	2.51	-
	174.8	<0.46	175	0.0720	2.43	2.25	-
verage					2.57	2.38	5.4
			156		2.33	2.26	
* * *	erage ** erage **	*** 183.0 rerage 112.4 *** 148.7 rerage *** *** 165.0 174.8	*** 183.0 <0.46	*** 183.0 <0.46	*** 183.0 <0.46	** 183.0 <0.46 183 0.0692 2.65 erage 2.50 ** 112.4 0.8 113 0.0640 1.77 ** 148.7 0.7 149 0.0715 2.09 erage 1.93 1.93 1.93 1.93 erage 2.57 2.57	** 183.0 <0.46 183 0.0692 2.65 2.69 erage 2.50 2.54 2.54 2.54 2.54 ** 112.4 0.8 113 0.0640 1.77 2.09 2.02 erage 148.7 0.7 149 0.0715 2.09 2.02 erage 1.9 1.67 0.0616 2.71 2.51 2.51 erage 1.71 1.67 0.0720 2.71 2.51 2.51 erage 1.5 1.67 0.0720 2.71 2.38 2.51

Note: Concentration data is only reported for three tests as required by US EPA Method 30B

* At 25°C and 1 atmosphere

** At 25°C and 1 atmosphere, adjusted to 11% oxygen

*** Spiked tube, mercury collected corrected for the original spike (250 ng for Test No. 2, 800 ng for Test No. 4, and 1400 ng for Test No. 5).

Table 3: Mercury Spike Tube Recovery

Test		Spike Tube			Unspike Tube	2	Spike	Spike
No.	Total	Volume	Mercury	Total	Volume	Mercury	Concentration	Recovery
	Collected	Sampled	Concentration	Collected	Sampled	Concentration		
	ng	Rm ³ *	ng/Rm ³ *	ng	Rm ³ *	ng/Rm ³ *	ng/Rm ³ *	%
2	433	0.0692	6260	148.2	0.0629	2356	3904	108.0
4	949	0.0715	13282	113.2	0.0640	1770	11513	NA
5	1567	0.0616	25422	174.8	0.0720	2429	22993	NA
Average								108.0

Note: The spike tubes were spiked with mercury by the analytical laboratory prior to sampling. The original spike concentrations were 250 ng for Test No. 2, 800 ng for Test No. 4, and 1400 ng for Test No. 5.

"NA" Not Applicable. Spike recovery was not calculated as spike concentration was outside the range specified in US EPA Method 30B.



APPENDIX 2

Mercury Field Data Sheets (7 pages)

Clean Harbors, Sarnia Mercury Tube Sampling Train Sample Volume Corrections

Incinerator Exhaust Stack

Test # - Tube	DGMCF	Initial DGM	Final DGM	Actual Vol.	Barometric	Average DGM	Average DGM	Corrected	Corrected
(tube pair field ID)		Reading	Reading	Sampled	Pressure	Pressure	Temperature	Volume	Volume
		(1)	(1)	(1)	(in Hg)	del H (in H ₂ O)	(c)	(T)*	(Rm ³)*
T1A OL421340 Spiked	0.979	36.00	102.20	66.20	29.5	2.6	7.9	68.17	0.0682
T1B OL445633	1.001	69.20	132.30	63.10	29.5	1.5	3.5	67.31	0.0673
		c c	C L L		L C C	u r	۲ ۲	62 01	0 0630
1 ZA UL445644	0.979	3.20	05.50	02.3U	C.62 7.00	0.7	7.01	10.20	C 000 0
12B ULCU38415 Spiked	TOO'T	33.30	98.30	00.00	C.62	0.T	5.	17.00	70000
T3A OL426826 Spiked	0.979	67.10	130.00	62.90	29.4	2.6	7.6	64.69	0.0647
T3B OL445572	1.001	22.00	94.00	72.00	29.4	1.6	4.9	76.28	0.0763
T4A 445635	0.979	54.30	117.00	62.70	29.4	2.6	9.5	63.96	0.0640
T4B OL331377 Spiked	1.001	97.20	165.00	67.80	29.4	1.6	5.9	71.48	0.0715
T5A OL335256 Spiked	0.979	19.20	79.40	60.20	29.3	2.6	7.9	61.64	0.0616
T5B 0L445603	1.001	72.30	140.30	68.00	29.3	1.5	4.0	71.98	0.0720

T6A OL445677	0.979	80.00	139.80	59.80	29.3	2.6	9.8	60.79	0.0608
T6B OL336417 Spiked	1.001	40.70	104.10	63.40	29.3	1.5	5.0	66.85	0.0668

* dry at 25°C and 1 atmosphere

Plant:	Clean Harbors		Test location:	Stack Breeching
Plant Location:	Corunna		Date:	January 10, 2018
Test No.:			Project No.:	21830
			Measuring Device	MII
Train A			Control Module	10117
		Spiked (Yes No	Barometer	ENV. CAN.
Spike Concentration	<u>1020 ng</u>			- <i>FP</i> :PG
	: 1월 2013년 1월 2017년 1월 1917년 1월 2017년 1 1월 2017년 1월 2		Barometric Pressure	
Clock				
	Dry Gas	Average	Meter	Pump
Time	Meter	Meter	Pressure	Vacuum
		Temperature °C	ΔH "H ₂ U	"Hg Gauge
0	369			
5	768	<u> </u>	2.6	<u> </u>
10		<u>_</u>	1 2.6	
15	36.2		2.6	<u> </u>
		<u> </u>	2.6	<u> </u>
20			2.6	
25	63.2			
30	- 453	<u> </u>		<u> </u>
35	1-1-2	<u> </u>		<u>+ </u>
40	10.4 9.7 C	<u> </u>	2.6	
		C.L	26	10
45				
50	\$8.5	名	2.6	10
50 55	88.5 85.9		2.6	10
50		- Zo Zo	2.6 7.6 2.6	
50 55 60	88.5 85.9	<u> </u>	2.6	10
50 55 60 Start Time: 915	Initial Leak Check 2,0 LPM	<u> </u>	DGMCF: Sample Volume:	10
50 55 60 Start Time: 915	Initial Leak Check 2,0 LPM	<u>м@ /)</u> "Нg	DGMCF: Sample Volume: Average DGM Temp:	10
50 55 60 Start Time: 915	Initial Leak Check 2,0 LPM	<u>м@ /)</u> "Нg	DGMCF: Sample Volume:	0.379
50 55 60 Start Time: 915	Initial Leak Check 2,0 LPM	<u>м@ /)</u> "Нg	DGMCF: Sample Volume: Average DGM Temp:	0.379
50 55 60 Start Time: 915 Finish Time: 7075	Initial Leak Check 2,0 LPM	<u>м@ /)</u> "Нg	DGMCF: Sample Volume: Average DGM Temp:	0.379
50 55 60 Start Time: 915 Finish Time: 7075	Initial Leak Check Z _i O (LPP Final Leak Check Z _i O (LPP	Л@ ("Нg Л@ /"Нg	DGMCF: Sample Volume: Average DGM Temp: Average DGM Δ H:	0.979 63.39 3.4 2.6
50 55 60 Start Time: 915 Finish Time: 7075 Train B Tube Identification:	Initial Leak Check 200 LPM Final Leak Check 200 LPM	<u>м@ /)</u> "Нg	DGMCF: Sample Volume: Average DGM Temp: Average DGM Δ H:	0.979 0.979 3.4 2.6
50 55 60 Start Time: 915 Finish Time: 7075 Train B Tube Identification:	Initial Leak Check Z _i O (LPP Final Leak Check Z _i O (LPP	Л@ ("Нg Л@ /"Нg	DGMCF: Sample Volume: Average DGM Temp: Average DGM Δ H:	0.979 63.39 3.4 2.6
50 55 60 Start Time: 915 Finish Time: 70 Train B Tube Identification: Spike Concentration	Initial Leak Check 200 LPM Final Leak Check 200 LPM	A@ / Hg M@ / Hg Spiked Yes No	DGMCF: Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module	0.379 63.39 3.4 2.6 Mil i.ocharg
50 55 60 Start Time: 415 Finish Time: 70 Train B Tube Identification: Spike Concentration Clock	Initial Leak Check Z _i LPN Final Leak Check Z _i LPN Final Leak Check Z _i LPN	A@ / Hg M@ / Hg Spiked Yes No Average	DGMCF: Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter	0.379 65.31 8.4 2.6 Mil (octang
50 55 60 Start Time: 915 Finish Time: 70 Train B Tube Identification: Spike Concentration	Initial Leak Check 200 LPM Final Leak Check 200 LPM	A@ / Hg M@ / Hg Spiked Yes No Average Meter	DGMCF: Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure	A.S.S. B.U Z.C MII Costang Pump Vacuum
50 55 60 Start Time: 915 Finish Time: 70 Train B Tube Identification: Spike Concentration Clock	Initial Leak Check Z _i LPN Final Leak Check Z _i LPN Final Leak Check Z _i LPN	A@ / Hg M@ / Hg Spiked Yes No Average	DGMCF: Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter	0.379 65.31 8.4 2.6 Mil (octang
50 55 60 Start Time: 415 Finish Time: 70 Train B Tube Identification: Spike Concentration Clock	Initial Leak Check Z _i LPN Final Leak Check Z _i LPN Final Leak Check Z _i LPN OL-445633 ng Dry Gas Meter L	A@ / Hg M@ / Hg Spiked Yes No Average Meter Temperature	DGMCF: Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H	A STA STA STA STA STA STA STA MII Costants Pump Vacuum "Hg
50 55 60 Start Time: 715 Finish Time: 70 Train B Tube Identification: Spike Concentration Clock Time	Initial Leak Check Z _i LPN Final Leak Check Z _i LPN Final Leak Check Z _i Dry Gas Meter	A@ / "Hg M@ / "Hg Spiked Yes No Average Meter Temperature °C	DGMCF: Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U	A. 37 M A. 37 M A. 37 M A. 4 A. 4 A.4
50 55 60 Start Time: 915 Finish Time: 7075 Train B Tube Identification: Spike Concentration Clock Time 0 5	Initial Leak Check Z _i LPN Final Leak Check Z _i LPN Final Leak Check Z _i LPN OL-445633 ng Dry Gas Meter L	A@ / "Hg M@ / "Hg Spiked Yes No Average Meter Temperature °C 1	DGMCF: Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U	Pump Vacuum "Hg Gauge
50 55 60 Start Time: 915 Finish Time: 7075 Train B Tube Identification: Spike Concentration Clock Time 0 5 10	Initial Leak Check Z ₁₀ LPM Final Leak Check Z ₁₀ LPM Final Leak Check Z ₁₀ LPM Dry Gas Meter L L 69.2 75.0 75.0 75.0	A@ / "Hg M@ / "Hg Spiked Yes No Average Meter Temperature °C 1 2	DGMCF: Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U	Pump Vacuum "Hg Gauge
50 55 60 Start Time: 915 Finish Time: 7075 Train B Tube Identification: Spike Concentration Clock Time 0 5 10 15	Initial Leak Check Z _i LPN Final Leak Check Z _i LPN Final Leak Check Z _i LPN OL-445633 ng Dry Gas Meter L	A@ / "Hg M@ / "Hg Spiked Yes No Average Meter Temperature °C 1	DGMCF: Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U	A CONTRACTOR OF
50 55 60 Start Time: 70 Finish Time: 70 Train B Tube Identification: Spike Concentration Clock Time 0 5 10 15 20	Bit Bit <thbit< th=""> <thbit< th=""> <thbit< th=""></thbit<></thbit<></thbit<>	Average Average Meter Temperature *C 1 2 4 4 4 4 4 4 4 4 4 4 4 4 4	DGMCF: Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U	A STANDARD
50 55 60 Start Time: 75 Finish Time: 70 Train B Tube Identification: Spike Concentration Clock Time 0 5 10 15 20 25	Bit Bit <thbit< th=""> <thbit< th=""> <thbit< th=""></thbit<></thbit<></thbit<>	Average Me Yes No Spiked Yes No Average Meter Temperature °C	DGMCF: Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U	A CONTRACTOR OF
50 55 60 Start Time: 915 Finish Time: 705 Train B Tube Identification: Spike Concentration Clock Time 0 5 10 15 20 25 30	Bit Bit <thbit< th=""> <thbit< th=""> <thbit< th=""></thbit<></thbit<></thbit<>	Ale / "Hg M@ / "Hg Spiked Yes No Average Meter Temperature °C I 2 3 4 4 4 4 4	DGMCF: Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U	A STANDARD
50 55 60 Start Time: 70 Finish Time: 70 Train B Tube Identification: Spike Concentration Clock Time 0 5 10 15 20 25 30 35	Bit Bit <thbit< th=""> <thbit< th=""> <thbit< th=""></thbit<></thbit<></thbit<>	A@ /] "Hg M@ /] "Hg Spiked Yes No Average Meter Temperature °C 1 2 3 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	DGMCF: Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U	A STANDARD
50 55 60 Start Time: 915 Finish Time: 7075 Train B Tube Identification: Spike Concentration Clock Time 0 5 10 15 20 25 30 35 40	Initial Leak Check 2,01 Initial Leak Check 2,01 Final Leak Check 2,01 Dry Gas ng Dry Gas Meter L 69.2 15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0 15.0	Ale / "Hg M@ / "Hg Spiked Yes No Average Meter Temperature °C I 2 3 4 4 4 4 4	DGMCF: Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U	A STANDARD
50 55 60 Start Time: 915 Finish Time: 70 Train B Tube Identification: Spike Concentration Clock Time 0 Clock Time 0 5 5 10 15 20 25 30 35 40 40 45	Вид 107<7	A@ / "Hg M@ / "Hg Spiked Yes No Average Meter Temperature °C 1 2 3 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	DGMCF: Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U	A STANDARD
50 55 60 Start Time: 915 Finish Time: 7015 Train B Tube Identification: Spike Concentration Clock Time 0 5 5 10 15 20 25 30 35 40	B B C C L L L Dry Gas Meter L C <thc< th=""> C <thc< th=""> <thc< th=""> C <thc< <="" td=""><td>A@ /] "Hg M@ /] "Hg Spiked Yes No Average Meter Temperature °C 1 2 3 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4</td><td>DGMCF: Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H₂U 1.5 1.5 1.5 1.5 1.5 1.5 1.5 1.5 1.5 1.</td><td>A STANDARD</td></thc<></thc<></thc<></thc<>	A@ /] "Hg M@ /] "Hg Spiked Yes No Average Meter Temperature °C 1 2 3 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	DGMCF: Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U 1.5 1.5 1.5 1.5 1.5 1.5 1.5 1.5 1.5 1.	A STANDARD

Start Time: 9/5	Initial Leak Check Z. () LPM@) 3 "Hg	DGMCF: 1.001
Finish Time: 10 15	Final Leak Check Loj LPM@ 15 "Hg	Sample Volume: 63.
		Average DGM Temp: 3,5
Operator:	2142	Average DGM Δ H:

Plant:	Clean Harbors		Test location:	Stack Breeching
Plant Location:	Corunna	김 씨는 것 같은 것 같은	Date:	January 10, 2018
Fest No.:	C-		Project No.:	21830
Train A			Measuring Device Control Module	MI
Fube Identification:	01-445644	Spiked Yes No	Barometer	<u> </u>
Spike Concentration		ng	Barometer	LIVV. CAIV.
		<u></u>	Barometric Pressure	29.45
Clock	Dry Gas	Average	Meter	Pump
Time	Meter	Meter	Pressure	Vacuum
		Temperature °C	Δ H ``H ₂ U	"Hg
0	37	<u> </u>	1	Gauge
5	- 2.d	6	2.0	
10	<u> </u>	I IV		
15	126	 ;\		
20		- G	56	
25		ic	54	é
30		1 12	510	- é
35	老儿	- R	5.6	
40	100%	14		5
45	ida	14		3
50	1 28:3	1 14	56	
55	Loci	1 12	5.6	- E
60	1551	16	21_	6
Start Time: 1025		LPM@ 15"Hg	DGMCF:	0.979
Finish Time: 11 23	Final Leak Check 2,0	LPM@ KG"Hg	Sample Volume:	-62:2
			Average DGM Temp:	
			LAVerage DGM A H.	
	and a second		Average DGM Δ H:	- Brt Life
			Average DGM Δ H:	bt Life
		Collect of Can		<u>Bit Lib</u>
Tube Identification:	0LC 038415	Spiked (Yes) No	Measuring Device	MII
Tube Identification:		Spiked Yes? No		MII <i>COE 2015</i>
Tube Identification: Spike Concentration	251	ng	Measuring Device Control Module	CUE 200195
Tube Identification: Spike Concentration Clock	250 Dry Gas	ng Average	Measuring Device Control Module Meter	COE 200193
Tube Identification: Spike Concentration	251	ng Average Meter	Measuring Device Control Module Meter Pressure	COE 200193 Pump Vacuum
Tube Identification: Spike Concentration Clock	250 Dry Gas	ng Average	Measuring Device Control Module Meter	COE 200193
Tube Identification: Spike Concentration Clock	250 Dry Gas Meter	ng Average Meter Temperature	Measuring Device Control Module Meter Pressure Δ H "H ₂ O	COE 200193 Pump Vacuum "Hg
Tube Identification: Spike Concentration Clock Time	Dry Gas Meter L	ng Average Meter Temperature	Measuring Device Control Module Meter Pressure Δ H	COE 200195 Pump Vacuum "Hg Gauge
Tube Identification: Spike Concentration Clock Time 0	Dry Gas Meter L 33. 3	ng Average Meter Temperature	Measuring Device Control Module Meter Pressure Δ H "H ₂ O	COE 200195 Pump Vacuum "Hg Gauge
Tube Identification: Spike Concentration Clock Time 0 5	Dry Gas Meter L 333.5	ng Average Meter Temperature °C	Measuring Device Control Module Meter Pressure Δ H "H ₂ O	COE 200195 Pump Vacuum "Hg Gauge
Tube Identification: Spike Concentration Clock Time 0 5 5 10	Dry Gas Meter L 333.5	ng Average Meter Temperature °C	Measuring Device Control Module Meter Pressure Δ H "H ₂ O	COE 200195 Pump Vacuum "Hg Gauge
Tube Identification: Spike Concentration Clock Time 0 5 10 15	Dry Gas Meter L 333.5	ng Average Meter Temperature °C	Measuring Device Control Module Meter Pressure Δ H "H ₂ O	COE 200195 Pump Vacuum "Hg Gauge
Tube Identification: Spike Concentration Clock Time 0 5 10 15 20	Dry Gas Meter L 333.5	ng Average Meter Temperature °C	Measuring Device Control Module Meter Pressure Δ H "H ₂ O	COE 200195 Pump Vacuum "Hg Gauge
Tube Identification: Spike Concentration Clock Time 0 5 10 15 20 25	Dry Gas Meter L 333.5	ng Average Meter Temperature °C Y Y Y Y Y Y	Measuring Device Control Module Meter Pressure Δ H ¨H ₂ O	COE 200195 Pump Vacuum "Hg Gauge
Tube Identification: Spike Concentration Clock Time 0 5 5 10 15 20 25 30	Dry Gas Meter L 333.5	ng Average Meter Temperature °C Y Y Y Y Y Y	Measuring Device Control Module Meter Pressure Δ H ¨H ₂ O	COE 200195 Pump Vacuum "Hg Gauge
Tube Identification: Spike Concentration Clock Time 0 5 10 15 20 25 30 35	Dry Gas Meter L 333.5	ng Average Meter Temperature °C Y Y Y Y Y Y	Measuring Device Control Module Meter Pressure Δ H ¨H ₂ O	COE 200195 Pump Vacuum "Hg Gauge
Tube Identification: Spike Concentration Clock Time 0 5 10 15 20 25 30 35 40	Dry Gas Meter L 333.5	ng Average Meter Temperature °C Y Y Y Y Y Y	Measuring Device Control Module Meter Pressure Δ H ¨H ₂ O	COE 200195 Pump Vacuum "Hg Gauge
Tube Identification: Spike Concentration Clock Time 0 5 10 15 20 25 30 25 30 35 40 45 50	Dry Gas Meter L 333.5	ng Average Meter Temperature °C Y Y Y Y Y Y	Measuring Device Control Module Meter Pressure Δ H ¨H ₂ O	COE 200195 Pump Vacuum "Hg Gauge
Tube Identification: Spike Concentration Clock Time 0 5 10 15 20 25 30 25 30 35 40 45	250 Dry Gas Meter L 33.3 36.7 44.3 44.3 44.3 44.3 44.3 44.3 44.3 44	ng Average Meter Temperature °C Y Y Y Y Y Y	Measuring Device Control Module Meter Pressure Δ H ¨H ₂ O	COE 200195 Pump Vacuum "Hg Gauge
Tube Identification: Spike Concentration Clock Time 0 5 10 15 20 25 30 25 30 35 40 45 50 55 60	Dry Gas Meter L 333.5	ng Average Meter Temperature °C Y Y Y Y Y Y Y Y Y Y Y Y Y Y Y Y Y Y	Measuring Device Control Module Meter Pressure Δ H H_2U I = U I	COE 200195 Pump Vacuum "Hg Gauge
Tube Identification: Spike Concentration Clock Time 0 5 10 15 20 25 30 25 30 35 40 45 50 55 60 Start Time: 10725	Dry Gas Meter L 33.3 34.7 44.5 44.5 44.5 44.5 44.5 44.5 44.5 4	Average Meter Temperature "C	Measuring Device Control Module Meter Pressure Δ Η Π+Ω (Γ Γ Γ Γ Γ Γ Γ Γ Γ Γ Γ Γ Γ Γ Γ Γ Γ Γ Γ	COE 200195 Pump Vacuum "Hg Gauge
Tube Identification: Spike Concentration Clock Time 0 5 10 15 20 25 30 25 30 35 40 45 50 55 60 Start Time: 10725	Dry Gas Meter L J J J J J J J J J J J J J J J J J J	ng Average Meter Temperature °C Y Y Y Y Y Y Y Y Y Y Y Y Y Y Y Y Y Y	Measuring Device Control Module Meter Pressure Δ Η Π+ Δ ((((((((((((((((((COE 200195
Time 0 5 10 15 20 25 30 35 40 45 50 55 60 Start Time: 1025	Dry Gas Meter L J J J J J J J J J J J J J J J J J J	Average Meter Temperature "C	Measuring Device Control Module Meter Pressure Δ Η Π+Ω (Γ Γ Γ Γ Γ Γ Γ Γ Γ Γ Γ Γ Γ Γ Γ Γ Γ Γ Γ	COE 200195

Plant:	Clean Harbors		Test location:	Stack Breeching
Plant Location:	Corunna		Date:	January 10, 2018
Test No.:	3		Project No.:	21830
			Measuring Device	MI
Train A		\sim	Control Module	10177
Tube Identification: C	1426826	Spiked Yes No	Barometer	ENV. CAN.
Spike Concentration	Sje ng			
			Barometric Pressure	299.41
Clock	Dry Gas	Average	Meter	Pump
Time	Meter	Meter	Pressure	Vacuum
		Temperature	ΔH	"Hg
		° C	"H₂U	Gauge
0	67.1	5	2.6	?
5	72.2	5	2.6	5
10	17.3	6	2.6	U U
15	52.4	b		6
20	87 5	<u> </u>		6
25	92.6	7	5.6	Ţ,
30	\$1.7	9	1.6	9
35	102.8	9	2.6	6
40	107,9	q	7.6	E E
45	113.1	3	216	6
50 🥠	18.2	4	E.C	6
55	上発年、ひ	9	2.6	1.2
	130 0	A M	(,	- C
	ارم کے استقلا	M@ 1 6 "Hg M@ 1 6 "Hg	DGMCF: Sample Volume: Average DGM Temp:	0.979
Start Time: 💡	ر کار کار کار کار کار کار کار کار کار کا		Sample Volume:	0.979
Start Time:	ر کار کار کار کار کار کار کار کار کار کا		Sample Volume: Average DGM Temp:	0.979
Start Time:	35 Initial Leak Check 200 LPI 35 Final Leak Check 201 LPI		Sample Volume: Average DGM Temp: Average DGM ∆ H:	0.979 63.0 7.6 2.6
Start Time:	35 Initial Leak Check 200 LPI 35 Final Leak Check 201 LPI	M@ 16"Hg	Sample Volume: Average DGM Temp:	
Start Time:	Initial Leak Check Zo(LPI Final Leak Check Zo(LPI	M@ 16"Hg	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device	
Start Time:	Initial Leak Check Zo(LPI Final Leak Check Zo(LPI	M@ 16"Hg	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device	
Start Time:	35 Initial Leak Check Loi LPI 35 Final Leak Check Loi LPI 01 YYSS TrZ ng	M@ {{ "Hg Spiked Yes	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module	MII Eore 2015 Pump Vacuum
Start Time:	35 Initial Leak Check 201 LPI 35 Final Leak Check 201 LPI 35 Final Leak Check 201 LPI 35 Final Leak Check 201 LPI 36 Model 201 LPI 37 Final Leak Check 201 LPI 36 Model 201 Model 37 Model Model Model 38 Model Model Model 39 Model Model Model 39 Model Model Model Model 39 Model Model Model Model Model 39 Model	M@ Yes No Spiked Yes No Average Meter Temperature	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H	MII Ears 2015 Pump Vacuum "Hg
Start Time: Finish Time:	Dry Gas L	M@ C "Hg Spiked Yes No Average Meter	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure	MII Erezare Pump Vacuum "Hg Gauge
Start Time: Finish Time: Train B Tube Identification: Spike Concentration Clock Time 0	Dry Gas Meter L	M@ Yes No Spiked Yes No Average Meter Temperature	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H	MII Corectants Pump Vacuum "Hg Gauge
Start Time:	Dry Gas Meter L 256.0	M@ C"Hg Spiked Yes/No Average Meter Temperature °C	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H	MII Erezare Pump Vacuum "Hg Gauge
Start Time: Finish Time: Train B Tube Identification: Spike Concentration Clock Time 0 5 10	Dry Gas Meter L	M@ 1 6 "Hg Spiked Yes No Average Meter Temperature °C 3	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H	MII Corectants Pump Vacuum "Hg Gauge
Start Time:	Dry Gas Meter L 25 25 0 25 0 25 0 25 0 25 0 25 0 25 0 2	M@ C "Hg Spiked Yes No Average Meter Temperature °C S	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H	MII Corectants Pump Vacuum "Hg Gauge
Start Time: Finish Time: Train B Tube Identification: Spike Concentration Clock Time 0 5 10 15 20	Dry Gas Meter L 256.0	M@ C "Hg Spiked Yes No Average Meter Temperature °C 3 5 5 5	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H	MII Core Zans Pump Vacuum "Hg Gauge 5 5 5
Start Time: Finish Time: Train B Tube Identification: Spike Concentration Clock Time 0 5 10 15 20 25	Dry Gas Meter L 25 25 0 25 0 25 0 25 0 25 0 25 0 25 0 2	M@ C "Hg Spiked Yes No Average Meter Temperature °C 3 5 5 5 5	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H	MII Core Zans Pump Vacuum "Hg Gauge 5 5 5
Start Time: Finish Time: Train B Tube Identification: Spike Concentration Clock Time 0 0 5 10 15 20 25 30	35 Initial Leak Check 2.0(LPI 35 Final Leak Check 2.0(LPI 35 Final Leak Check 2.0(LPI O1	M@ C "Hg Spiked Yes/ No Average Meter Temperature °C 3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H	MII Core Zans Pump Vacuum "Hg Gauge 5 5 5
Start Time:	Dry Gas Meter L 25 25 0 25 0 25 0 25 0 25 0 25 0 25 0 2	M@ 1 6 "Hg Spiked Yes/No Average Meter Temperature °C 3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H	MII CAB Last S Pump Vacuum "Hg Gauge S S S S S S S S S S S S S
Start Time:	35 Initial Leak Check 2.01 LPI 35 Final Leak Check 2.01 LPI 35 Final Leak Check 2.01 LPI 01 4455 772 ng 01 9455 772 ng 02 945 70 1 03 945 0 1 1 045 0 5 0 5 1 03 1645 0 5 1 1	M@ C "Hg Spiked Yes/ No Average Meter Temperature °C 3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ O 	MII Earge 2arls Pump Vacuum "Hg Gauge 5 6 6 6 6 6 6 6 6 6 6 6 6 6
Start Time: Finish Time: Train B Tube Identification: Spike Concentration Clock Time 0 0 5 10 15 20 25 30 35 40 45	35 Initial Leak Check 201 LPI 35 Final Leak Check 201 LPI 35 Final Leak Check 201 LPI 01 9455 772 ng Dry Gas Meter 1 1 L 2.2.0 3 440 4450 572.0 573.0 573.0 573.0 6.4.0 573.0 573.0	M@ C "Hg Spiked Yes No Average Meter Temperature °C 3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ O 	MII Earge 2arls Pump Vacuum "Hg Gauge 5, 6 6 6 6 6 6 6 6 6 6 6 6 6
Start Time: Finish Time: Train B Tube Identification: Spike Concentration Clock Time 0 0 5 10 15 20 25 30 35 40 45 50	$\begin{array}{c c} \hline \\ \hline $	M@ C "Hg Spiked Yes No Average Meter Temperature °C 3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ O 	MII Corectants Pump Vacuum "Hg Gauge S. Corectants Pump Vacuum "Hg Gauge Corectants Pump Vacuum "Hg Gauge Corectants Pump Vacuum "Hg Gauge Corectants Pump Vacuum "Hg Gauge Corectants Corectants Pump Vacuum "Hg Gauge Corectants Corectant
Start Time: Finish Time: Train B Tube Identification: Spike Concentration Clock Time 0 0 5 10 15 20 25 30 35 40 45 50 55	Initial Leak Check Zot LPI 35 Final Leak Check Zot LPI 35 Meter L L 1 Zot Zot D 2 Zot D L 1 Zot D L 2 Zot D L 3 U U L 3 U U D 3 U U D 3 U U D 3 U U U 3 U U U 4 U U U 4 U U U <t< td=""><td>M@ C "Hg Spiked Yes No Average Meter Temperature °C 3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5</td><td>Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H₂U </td><td>MII COE Carls Pump Vacuum "Hg Gauge S. Carls</td></t<>	M@ C "Hg Spiked Yes No Average Meter Temperature °C 3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U 	MII COE Carls Pump Vacuum "Hg Gauge S. Carls
Start Time: Finish Time: Train B Tube Identification: Spike Concentration Clock Time 0 0 5 10 15 20 25 30 35 40 45 50	$\begin{array}{c c} \hline \\ \hline $	M@ C "Hg Spiked Yes No Average Meter Temperature °C 3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U 	MII Corectants Pump Vacuum "Hg Gauge S. Corectants Pump Vacuum "Hg Gauge Corectants Pump Vacuum "Hg Gauge Corectants Pump Vacuum "Hg Gauge Corectants Pump Vacuum "Hg Gauge Corectants Corectants Pump Vacuum "Hg Gauge Corectants Corectant
Start Time: Finish Time: Train B Tube Identification: Spike Concentration Clock Time 0 Clock Time 0 5 10 15 20 25 30 35 40 45 50 55 60	Initial Leak Check Zot L 35 Final Leak Check Zot L 35 Final Leak Check Zot L 01	M@ C "Hg Spiked Yes/ No Average Meter Temperature "C 3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U 	MII Corectants Pump Vacuum "Hg Gauge 5 5 6 6 6 6 6 6 6 6 6 6 6 6 6
Start Time:	$\begin{array}{c c} \hline \\ \hline $	M@ / 6"Hg Spiked Yes/ No Average Meter Temperature °C 3 5 5 5 5 5 5 5 5 5 5 5 5 5	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U 	MII COE Carls Pump Vacuum "Hg Gauge S. Carls
Start Time: Finish Time: Train B Tube Identification: Spike Concentration Clock Time 0 0 5 10 15 20 25 30 35 40 45 50 55 60	$\begin{array}{c c} \hline \\ \hline $	M@ C "Hg Spiked Yes/ No Average Meter Temperature "C 3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U 	MII Corectants Pump Vacuum "Hg Gauge 5 5 6 6 6 6 6 6 6 6 6 6 6 6 6

ant:	Clean Harbors		Test location:	Stack Breeching
ant Location:	Corunna		Date:	January 10, 2018
st No.:			Project No.:	21830
			Measuring Device	MII
ain A		<u> </u>	Control Module	form
be Identification: OL	the second se	Spiked Yes No	Barometer	ENV. CAN.
ike Concentration	ng	\sim	Barometric Pressure	39.37
Clock	Dry Gas	Average	Meter	Pump
Time	Meter	Meter	Pressure	Vacuum
		Temperature	ΔΗ	"Hg
		°C	"H₂U	Gauge
0	543	-7	2.6	.
5	1059.5	B	7.6	5
10	1 65.0	Q	7.6	6
15	-10.0	1Ò	7.10	(1)
20	-150	10	5.6	E E
25	\$0.3	10	120	6
30	1 45.5	10	6.6	6
35	TRAET	, <u>v</u>	710	6
40	1 25 0		36	
45	160.0	10		6
50	100.9	10	2.6	6
55	1165	4.2		¥
33		10	3.4	6
60				1 10
	Initial Leak Check Log LPN Final Leak Check Log LPN	Л@ / (, "Hg	DGMCF: 0. Cf Sample Volume: Cf Average DGM Temp: Af Average DGM Δ H: Z	19 12,1 10 ~(c
art Time: 1757 hish Time: 1353		Л@ / (, "Hg	Sample Volume:	79
art Time: 7333	Final Leak Check Z BALLPN	Λ@"Hg Λ@"Hg	Sample Volume: Average DGM Temp: Average DGM Δ H: Z	19 iz 1 -6
ain B be Identification:	Final Leak Check Z B LPN	Л@ / (, "Hg	Sample Volume:	13 ;z.1 ;8 -{
art Time: 733	Final Leak Check Z BALLPN	Λ@"Hg Λ@"Hg	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device	19 iz 1 -6
art Time: 7353 ish Time: 7353 ain B be Identification: 07	Final Leak Check Z B LPN	Λ@"Hg Λ@"Hg	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device	13 ;z.1 ;8 -{
ish Time: 1353	Final Leak Check Z / LPN	N@ / (, "Hg N@ M "Hg Spiked Yes No	Sample Volume:	73 22 19 -(0 MII <u>cot 200</u> 5 Pump Vacuum
rt Time: 7 < ish Time: 3 < 3 in B be Identification: 0 ke Concentration Clock	Final Leak Check Z / LPN	A@ / (, "Hg A@ "Hg Spiked Yes No Average Meter Temperature	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H	7 2 2 3 2 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3
rt Time: 7 < ish Time: 3 < in B be Identification: 0 ke Concentration Clock	Final Leak Check Z / LPN	A@ / (, "Hg A@ "Hg Spiked Yes No Average Meter	Sample Volume:	73 221 18 -6 MII ect 20013 Pump
rt Time: 7 < ish Time: 3 < in B ne Identification: 0 ke Concentration Clock	Final Leak Check Z / LPN	A@ / (, "Hg A@ / "Hg Spiked Yes No Average Meter Temperature °C	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H	7 \$ 22.5 1 0
rt Time: 725 sh Time: 735 in B se Identification: 77 see Concentration Clock Time	Final Leak Check Z / LPN	A@ / (, "Hg A@ / "Hg Spiked Yes No Average Meter Temperature °C	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H ····································	7 \$ 22 1 1 0
rt Time: 7 sh Time: 7 in B be Identification: 07 ke Concentration Clock Time 0	Final Leak Check Z / LPN	A@ / (, "Hg A@ / "Hg Spiked Yes No Average Meter Temperature °C	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H ····································	2 \$ 22,5 1 1 Ø -< € MII COE 2,001 S Pump Vacuum "Hg Gauge 3,5
rt Time: 7 < ish Time 0 5	Final Leak Check Z / LPN	A@ / (, "Hg A@ / "Hg Spiked Yes No Average Meter Temperature °C	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H ····································	73 72 19 -(- MII COE 2001 TO Pump Vacuum "Hg Gauge 2 3,5 5 5 5 5 5 5 5 5 5 5 5 5 5
rt Time: 7 < ish Time: 7 < ish Time: 7 < in B be Identification: 07 ke Concentration Clock Time 0 5 10	Final Leak Check 2, 1, LPN	A@ / (, "Hg A@ , "Hg Spiked Yes No Average Meter Temperature °C G	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H ····································	73 72 19 -(- MII COE 2001 TO Pump Vacuum "Hg Gauge 2 3,5 5 5 5 5 5 5 5 5 5 5 5 5 5
rt Time: 17 < 1 ish Time: 13 < 3 in B pe Identification: 0 ke Concentration Clock Time 0 5 10 15	Final Leak Check 2, 1, 1 LPN	A@ / (, "Hg A@ / "Hg Spiked Yes No Average Meter Temperature °C U U	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H ····································	2 \$ 22,5 1 1 Ø -< € MII COE 2,001 S Pump Vacuum "Hg Gauge 3,5
rt Time: 7 < ish Time: 7 < ish Time: 7 < in B be Identification: 7 ke Concentration Clock Time 0 5 10 15 20 25	Final Leak Check 2 13 LPN	A@ / ("Hg A@ "Hg Spiked Yes No Average Meter Temperature °C	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H ····································	73 72 18
rt Time: 7 < ish Time: 7 < ish Time: 7 < in B be Identification: 7 ke Concentration Clock Time 0 5 10 15 20 25 30	Final Leak Check 2 10 LPN	A@ / ("Hg A@ "Hg Spiked Yes No Average Meter Temperature °C ((Sample Volume:	7 \$ 22 1 19 -6 Mil COE 20015 Pump Vacuum "Hg Gauge 7 3,5 5 6 6 7 7 8 7 8 8 9 9 9 9 9 9 9 9 9 9 9 9 9
rt Time: 7 < 1 ish Time: 7 < 1 ish Time: 7 < 1 in B be Identification: 0 ke Concentration Clock Time 0 5 10 5 10 15 20 25 30 35	Final Leak Check 2 13 LPN	A@ / ("Hg A@ "Hg Spiked Yes No Average Meter Temperature °C ((Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H H H ₂ U	7 \$ 22 1 19 -6 Mil COE 20015 Pump Vacuum "Hg Gauge 7 3,5 5 6 6 7 7 8 7 8 8 9 9 9 9 9 9 9 9 9 9 9 9 9
rt Time: 7 < ish Tim	Final Leak Check 2, 1, LPN	A@ / ("Hg A@ "Hg Spiked Yes No Average Meter Temperature °C (Sample Volume:	7 \$ 22 1 19 -6 Mil COE 20015 Pump Vacuum "Hg Gauge 7 3,5 5 6 6 7 7 8 7 8 8 9 9 9 9 9 9 9 9 9 9 9 9 9
in Time: ish Time: ish Time: ish Time: ish Time: ish Time: ish Time Clock Time 0 5 10 15 20 25 30 35 40 45	Final Leak Check 2, 1, 1 LPN	A@ / ("Hg A@ "Hg Spiked Yes No Average Meter Temperature °C (C C C C C C C C C C C C C C C C C	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H H H ₂ U	7 \$ 22 1 19 -6 Mil COE 20015 Pump Vacuum "Hg Gauge 7 3,5 5 6 6 7 7 8 7 8 8 9 9 9 9 9 9 9 9 9 9 9 9 9
ain B be Identification: ke Concentration Clock Time 0 5 10 15 20 25 30 35 40 45 50	Final Leak Check 2, 1, 1 LPN	A@ / ("Hg A@ "Hg Spiked Yes No Average Meter Temperature °C (Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H H H ₂ U	73 72 19 -(p -(p -(p -(p -(p -(p)
art Time: Art Time Art T	Final Leak Check 2 10 LPN	A@ / ("Hg A@ "Hg Spiked Yes No Average Meter Temperature °C ((((((((((((((((((Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H H H ₂ U	7 2 2 2 2 2 2 2 2 3 5 5 5 5 5 5 5 5 5 5 5 5 5
art Time: 1253 aish Time: 253 ain B be Identification: 07 ike Concentration Clock Time 0 5 10 5 10 15 20 25 30 35 40 45 50	Final Leak Check 2, 1, 1 LPN	A@ / ("Hg A@ "Hg Spiked Yes No Average Meter Temperature °C (C C C C C C C C C C C C C C C C C	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H H H ₂ U	7 2 2 3 4 6
ain B be Identification: Clock Time 0 5 10 15 20 25 30 35 40 45 50 55 60	Final Leak Check 2 10 LPN	A@ / ("Hg A@ "Hg Spiked Yes No Average Meter Temperature °C (Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H ····································	7 22 19 -6 -6 -6 -6 -7 -6 -7 -7 -7 -7 -7 -7 -7 -7 -7 -7
ain B be Identification: Clock Time 0 5 10 15 20 25 30 35 40 45 50 55 60 wrt Time: 12,53	Final Leak Check 2 10 LPN	A@ / C "Hg A@ "Hg Spiked Yes No Average Meter Temperature °C C C C C C C C C C C C C C C C C C C	Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H ····································	7 22 19 -6 -6 -6 -6 -7 -6 -7 -7 -7 -7 -7 -7 -7 -7 -7 -7
ain B be Identification: (ke Concentration) Clock Time 0 5 10 15 20 25 30 25 30 35 40 45 50 55 60	Final Leak Check 2 10 LPN	A@ / ("Hg A@ "Hg Spiked Yes No Average Meter Temperature °C (Sample Volume: Average DGM Temp: Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H ····································	7 22 19 -6 -6 -6 -6 -7 -6 -7 -7 -7 -7 -7 -7 -7 -7 -7 -7

Plant:	Clean Harbors		Test location:	Stack Breeching
Plant Location:	Corunna		Date:	January 10, 2018
Test No.:			Project No.:	21830
			Measuring Device	MII
Train A	<u></u>		Control Module	KOILT
Tube Identification:	01535256	Spiked Yes No	Barometer	ENV. CAN.
Spike Concentration	1020	ng		
			Barometric Pressure	39.30
Clock	Dry Gas	Average	Meter	Pump
Time	Meter	Meter	Pressure	Vacuum
		Temperature	ΔΗ	"Hg
		°C	₩₂U	Gauge
0	97	6	12.0	1 2 -
5 (Contraction)	174.E	8	2.4	7
10	19.3	<u> </u>	2.8	A State
15	1 <u><u>n</u><u>4</u>, <u>n</u></u>	- A	2.0	170
20	29.1	ğ	26	10
25	<u> </u>	8	2.6	10
30	<u> 49.3</u>	R R	26	10
35	54.3	8	2.6	10
40	39.0	8	1.6	10
45	<u>EQU</u>	8	26	10
50	69.5	8	2.0	10
55	13:6	8	2.6	10
60	<u> </u>	<u> </u>	2.6	10
Start Time: 1445	Initial Leak Check 20(LPM@ /5 "Hg	DGMCF:	7990
Finish Time: 1543		LPM@ ("Hg	Sample Volume:	90 102
		<u> </u>	Average DGM Temp:	4:5
			Average DGM Δ H:	26
				2.6
Train B		<u>.</u>		2.6
Train B	NL-44563	Sniked Yes No.	Average DGM Δ H:	2.6
Tube Identification:	06445603	Spiked Yes No	Average DGM Δ H:	2.6 MI L 0/E 2.00 iS
		Spiked Yes No	Average DGM Δ H:	2.6 MI CUE 2001S
Tube Identification:		ng	Average DGM Δ H: Measuring Device Control Module	COE 20019
Tube Identification: Spike Concentration		๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛๛	Average DGM Δ H: Measuring Device Control Module Meter	COE 200 is
Tube Identification: Spike Concentration Clock	Dry Gas Meter	Average Meter Temperature	Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H	Pump Vacuum "Hg
Tube Identification: Spike Concentration Clock	Dry Gas	Average Meter	Average DGM Δ H: Measuring Device Control Module Meter Pressure	Pump Vacuum
Tube Identification: Spike Concentration Clock Time 0	Dry Gas Meter	Average Meter Temperature	Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U	Pump Vacuum "Hg
Tube Identification: Spike Concentration Clock Time 0 5	Dry Gas Meter L 72.3 18.0	Average Meter Temperature	Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U 1.5 1.5	Pump Vacuum "Hg Gauge
Tube Identification: Spike Concentration Clock Time 0 5 10	Dry Gas Meter L 72.3 18.0	Average Meter Temperature	Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U 1.5 1.5 1.5	Pump Vacuum "Hg
Tube Identification: Spike Concentration Clock Time 0 5 10 15	Dry Gas Meter L 72.3 18.0	Average Meter Temperature	Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U 1.5 1.5 1.5	Pump Vacuum "Hg Gauge
Tube Identification: Spike Concentration Clock Time 0 5 10 15 20	Dry Gas Meter L 72.3 18.0	Average Meter Temperature	Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U 1.5 1.5 1.5	Pump Vacuum "Hg Gauge
Tube Identification: Spike Concentration Clock Time 0 5 10 15 20 25	Dry Gas Meter L 772.3 18.0 63.6 63.6 772.3 18.0 63.6 63.6 772.3 18.0 63.6 6 772.3 18.0 6 772.3 18.0 6 772.3 18.0 6 772.3 18.0 6 772.3 18.0 6 772.3 18.0 6 772.3 18.0 772.3	Average Meter Temperature	Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U 1.5 1.5 1.5 1.5 1.5 1.5	Pump Vacuum "Hg Gauge
Tube Identification: Spike Concentration Clock Time 0 5 10 15 20 25 30	Dry Gas Meter L 77.3 18.0 63.6 63.6 63.6 63.6 63.6 63.6 63.6 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 77.3 18.0 77.3 18.0 77.3 18.0 77.3 18.0 77.3 18.0 77.3 18.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.0 73.0 77.0 73.0 77.0 77.0 77.0 77	Average Meter Temperature	Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U 1.5 1.5 1.5 1.5 1.5 1.5 1.5 1.5	Pump Vacuum "Hg Gauge
Tube Identification: Spike Concentration Clock Time 0 5 10 15 20 25 30 35	Dry Gas Meter L 772.3 18.0 63.6 73.5 78.5 94.6 94.6 100.6	Average Meter Temperature	Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U 1.5 1.5 1.5 1.5 1.5 1.5 1.5 1.5	Pump Vacuum "Hg Gauge
Tube Identification: Spike Concentration Clock Time 0 5 10 15 20 25 20 25 30 35 40	Dry Gas Meter L 77.3 18.0 63.6 63.6 63.6 63.6 63.6 63.6 63.6 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 77.3 18.0 77.3 18.0 77.3 18.0 77.3 18.0 77.3 18.0 77.3 18.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.0 73.0 77.0 73.0 77.0 77.0 77.0 77	Average Meter Temperature	Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U 1.5 1.5 1.5 1.5 1.5 1.5 1.5 1.5	Pump Vacuum "Hg Gauge
Tube Identification:Spike ConcentrationClock Time051015202530354045	Dry Gas Meter L 77.3 18.0 63.6 63.6 63.6 63.6 63.6 63.6 63.6 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 77.3 18.0 77.3 18.0 77.3 18.0 77.3 18.0 77.3 18.0 77.3 18.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.0 73.0 77.0 73.0 77.0 77.0 77.0 77	Average Meter Temperature	Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U 1.5 1.5 1.5 1.5 1.5 1.5 1.5 1.5	COE 200 iS Pump Vacuum "Hg Gauge Control of the second secon
Tube Identification: Spike Concentration Clock Time 0 5 10 15 20 25 30 35 40 40 45 50	Dry Gas Meter L 77.3 18.0 63.6 63.6 63.6 63.6 63.6 63.6 63.6 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 6 77.3 18.0 77.3 18.0 77.3 18.0 77.3 18.0 77.3 18.0 77.3 18.0 77.3 18.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.3 19.0 77.0 73.0 77.0 73.0 77.0 77.0 77.0 77	Average Meter Temperature	Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U 1.5 1.5 1.5 1.5 1.5 1.5 1.5 1.5	Pump Vacuum "Hg Gauge 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7
Tube Identification:Spike ConcentrationClock Time0510152025303540455055	Dry Gas Meter L 772.3 18.0 63.0 63.0 63.0 772.3 18.0 63.0 63.0 772.3 18.0 63.0 63.0 772.3 18.0 63.0 63.0 772.3 18.0 63.0 63.0 63.0 63.0 772.3 18.0 63.0 63.0 772.3 18.0 63.0 772.3 18.0 772.3 19.0 772.3 19.0 772.3 19.0 772.3 19.0 772.3 19.0 772.3 19.0 772.3 19.0 772.3 19.0 772.3 19.0 772.3 19.0 772.3 19.0 772.3 19.0 772.3 19.0 772.3 19.0 772.3 19.0 772.3 19.0 772.3 19.0 772.3 19.0 772.3 19.0 772.3	Average Meter Temperature	Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U 1.5 1.5 1.5 1.5 1.5 1.5 1.5 1.5	COE 200 iS Pump Vacuum "Hg Gauge Control of the second secon
Tube Identification: Spike Concentration Clock Time 0 5 10 10 15 20 25 30 35 40 40 45 50	Dry Gas Meter L 772.3 78.0 63.0 63.0 772.3 78.0 63.0 772.3 78.0 772.3 7777.5 772.5 772.5 772.5 772.5 772.5 772.5 772.5 772.5 7777.5 777.5 7777.5 7777.5 77777.5 77777	Average Meter Temperature	Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U 1.5 1.5 1.5 1.5 1.5 1.5 1.5 1.5	Pump Vacuum "Hg Gauge 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7
Tube Identification: Spike Concentration Spike Concentration Clock Time 0 5 10 15 20 25 30 35 40 45 50 55 60	Dry Gas Meter L 772.3 18.0 63.6 772.3 18.0 63.6 772.3 18.0 772.3 19.0 772.3 10.0 772.3 10.0 772.3 10.0 772.3 10.0 772.3 10.0 772.3 10.0 772.3 10.0 772.3 10.0 772.3 10.0 772.3 10.0 772.3 10.0 772.3 10.0 772.5 10.0 10.0 10.0 10.0 10.0 10.0 10.0 10	Average Meter Temperature °C 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H H_2 U 1.5 1.5 1.5 1.5 1.5 1.5 1.5 1.5	COE 200 iS Pump Vacuum "Hg Gauge 7 7 7 7 7 7 7 7 7 7 7 7 7
O 5 10 5 10 15 20 25 30 35 40 45 50 55 60	Dry Gas Meter L 77.3 18.0 83.6 94.9 94.9 100.6 1	Average Meter Temperature °C 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U 1.5 1.5 1.5 1.5 1.5 1.5 1.5 1.5	Pump Vacuum "Hg Gauge 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7
O 5 10 5 20 25 30 35 40 45 50 55	Dry Gas Meter L 77.3 18.0 83.6 94.9 94.9 100.6 1	Average Meter Temperature °C 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U 1.5 1.5 1.5 1.5 1.5 1.5 1.5 1.5	Pump Vacuum "Hg Gauge 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7
O 5 10 5 10 15 20 25 30 35 40 45 50 55 60	Dry Gas Meter L 77.3 18.0 83.6 94.9 94.9 100.6 1	Average Meter Temperature °C 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	Average DGM Δ H: Measuring Device Control Module Meter Pressure Δ H "H ₂ U 1.5 <tr td="" tr<=""><td>Pump Vacuum "Hg Gauge 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7</td></tr>	Pump Vacuum "Hg Gauge 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7
Pump Vacuum "Hg Gauge 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7				

ant:	Clean Harbors		Test location:	Stack Breeching
ant Location:	Corunna		Date:	January 10, 2018
st No.:	6		Project No.:	21830
			Measuring Device	1 MII
ain A			Control Module	1010
be Identification: 01	JURG T	Spiked Yes (No)	Barometer	ENV. CAN.
ike Concentration	ng	·····		
			Barometric Pressure	29.29.
Clock	Dry Gas	Average	Meter	Pump
Time	Meter	Meter	Pressure	Vacuum
		Temperature	ΔH	"Hg
	al da batalan k ana bada da ba	°C	H ₂ U	Gauge
0	90.0	<u> </u>	2.6	2
5	<u>85.0</u>	<u> </u>	2.6	<u> </u>
10	<u> </u>	<u> 10</u>	2.6	¥
15	94.9		<u> </u>	
20	100.0		2.6	<u> </u>
25	1105.	10	2.6	1 7
30	110-0	/0	2.6	\mathbf{I}
35	114.7	10	2.6	<u> </u>
40	20-0		<u> </u>	<u> </u>
45	175.0		2.4	1 7
50	129 -	10	2.4	1 7
55	135.0	<u>10</u>	- 2.6	1
60			2.10	
nish Time: 1652			Average DGM Temp: Average DGM Δ H:	9.8
rain B		~		
ube Identification: n	_3364M	Spiked (Yes)No	Measuring Device	MII
oike Concentration	2600 ng	\sim	Control Module	COE 20018
Clock	Dry Gas	Average	Meter	Pump
Time	Meter	Meter	Pressure	Vacuum
		Temperature	ΔΗ	"Hg
	L	°C	"H ₂ U	Gauge
0	1 40.1			
	الاستخرار (¹ الر) (¹ ال	5	1.5	T
5	16.9		<u> </u>	- Y
5 10	46.9			¥
	46.9			74
10	40,9 56.4 66.4		1.5	24
10 15			1.5 1.5 1.5	and an and the test of the set of
10 15 20 25			1.5	10
10 15 20 25 30			15 15 15 15 15 15	10 10
10 15 20 25 30 35		55		10 10 10
10 15 20 25 30 35 40		55	15 15 15 15 15 15	10 10 10 10 10
10 15 20 25 30 35 40 45		55	15 15 15 15 15 15 15 15 15	10 10 10 10 10
10 15 20 25 30 35 40 45 50	40,9 36,4 61,0 64,6 77,0 77,0 77,0 77,0 77,0 77,0 77,0 77	mun mun han	(5) (5) (5) (5) (5) (5) (5) (5) (5) (5)	10 10 10 10 10
10 15 20 25 30 35 40 45 50 55	40,9 56,4 61,6 46,9 77,0 77,0 82,3 87,5	Innin inni	15 15 15 15 15 15 15 15 15	10 10 10 10 10
10 15 20 25 30 35 40 45 50	40,9 36,4 61,0 64,6 77,0 77,0 77,0 77,0 77,0 77,0 77,0 77	mun mun han	(5) (5) (5) (5) (5) (5) (5) (5) (5) (5)	10 10 10 10 10
10 15 20 25 30 35 40 45 50 55 60		mmmmmhilamhr	(3 (3 (3 (3 (3 (3 (3 (3 (5) (5) (5) (5) (5) (5) (5) (5) (5) (5)	10 10 10 10 10 10 10 10 10 10 10
10 15 20 25 30 35 40 45 50 55 60 itart Time: 1555	40.9 51.5 61.6 61.6 77.0 77.7 77.7 77.7 77.7 77.7 77.7 77	M@ (C "Hg	(.5 (.5 (.5 (.5 (.5 (.5) (.5) (.5) (.5)	10 10 10 10 10
10 15 20 25 30 35 40 45 50 55	40.9 51.5 61.6 61.6 77.0 77.7 77.7 77.7 77.7 77.7 77.7 77	mmmmmhilamhr	1.5 1.5	10 10 10 10 10 10 10 10 10 10 10



APPENDIX 3

ORTECH Equipment Calibration Data (4 pages)

Dry Gas Meter Calibration Data	N IIW	DGM	Gasometer	Barometer		Calibrated By
Dry Gas N						
	03-1004	Vost 2	January 8, 2017	29.32	<0 hpm @!Hg	
	Calibration Procedure	Meter Number	Date	Barometric Pressure	System Leak Check	

ORTECH Environmental

 $ft^3 = cm^* 1.332$ litres per cm/28.3168 litres per ft^3

Tstd °F+460 Tdgm[°]F+460 Vstd ft³ Vdgm ft³ DGMCF=

(Pbar in. Hg+DGMPressure/13.6) Pbar (in. Hg)

VIII V	MII NUMBERS
DGM	A10117
Gasometer	A01463
Barometer	COE20028
Calibrated By	David Utley
Signature	12:00
Reviewed and Accepted By	at Search &

6 1	min.	20	20.5	26.2
0	Factor			
DGM Outlet	°c,	26.0	26.0	26.0
 DGM Pressure	in. H ₂ 0	2.6	2.6	2.6
	`C	26.0	29.0	29.0
DGM Volume	ft ³	0.759	0.742	0.939
DGM Reading L	Initial Final	12.400 33.900	33.900 54.910	54.910 81.500
Gasometer Temperature	<u> </u>	21.0	21.0	21.0
g Gasometer Volume	f1 ³	0.734	0.720	0.894
 ading	cm	15.60	15.30	19.00
Gasometer Reading cm	Final	66.10	50.80	67.90
ß	Initial	81 70	66.10	86.90

Flow Rate niqi

1.0 []

1.0

Acceptance Criteria:

Individual values of DGM calibration factor must be within \pm 1.5% of the average value.

otherwise the meter must be repaired and/or adjusted as necessary and recalibrated prior to use. (Environment Canada Reference Method EPS 1/RM/8, Section 6) If not the calibration must be repeated. Also, the DGMCF average value must be 1.00 ± 0.05 ,

0.979 I Lpm

DGMCF AVERAGE

Revision June 5, 2007

ORTECH Environmental Trendicator Calibration

e de la companya de l	an an the standard frequencies and the second second
Calibration Procedure	03-J005
Trendicator Type	Nutech
MI	A10117
Date	January 8, 2017
Calibrated By	David Utley
Signature	Delle
Reviewed and Accepted By	15an

	Tredicator D	Percent		
Fluke Calibrator Output				
(COE 20024)	Before Adjustment	After Adjustment		
(°C)	(°C)	(°C)	(%)	
0	0	NA	0.0	
10	10		0.0	
20	20		0.0	
50	50		0.0	
75	75		0.0	
100	100		0.0	
125	126		-0.8	
150	151		-0.7	
200	200		0.0	
300	299		0.3	
400	399		0.3	
500	500		0.0	
600	600		0.0	

% Difference = (micromite - after adjustment reading)x 100

micromite

Acceptance Criteria:

Trendicator display must read within $\pm 1.5\%$ of the micromite value at each output. Otherwise, the Trendicator must be repaired and/or adjusted as necessary, and recalibrated prior to use. (MOE Source Testing Code, Version #2, Method 5)

ORTECH Environmental

Calibration Procedure 03-J004 Meter Number Vost 5 Date January 9, 2018 Reconstruct Descentes 79 74
--

 $ft^3 = cm^* 1.332$ litres per cm/28.3168 litres per ft^3

<0.01 lpm @ 21"Hg

System Leak Check

DGMCF= Vstd ft³ Tdgm ^oF+460 Vdgm ft³ Tstd ^oF+460

Tdgm °F+460Pbar (in. Hg)Tstd °F+460(Pbar in. Hg+DGMPressure/13.6)

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A01463	Gasometer Barometer
COE 20018	DGM
MII NUMBERS	M

ORTECH Environmental Dry Gas Meter Calibration Data

barometer	CUE 20040	
Calibrated By	David Utley	
Signature	$\mathcal{O} \mathcal{O} \mathcal{O}$	
Reviewed and Accepted By	ASit	
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Temperature L Volume Temperature Pressure Outlet Calibration °C Initial Final fr^3 °C in. H ₂ O °C Factor °C 122.22 144.83 0.798 25.0 1.5 25.0 0.988 21.0 51.56 74.70 0.817 24.0 1.5 24.0 1.088 21.0 97.50 122.22 0.817 25.0 1.5 24.0 1.008	Gasomet	Gasometer Reading	Gasometer Gasometer	Gasometer	DGM Reading	DGM	DGM Average	DGM		DGM	line.	Flow
°C Initial Final ft ³ °C in. H ₂ O °C Factor 21.0 122.22 144.83 0.798 25.0 1.5 25.0 0.988 21.0 51.56 74.70 0.817 24.0 1.5 24.0 1.088 21.0 97.50 122.22 0.817 24.0 1.5 24.0 1.008 21.0 97.50 122.22 0.873 25.0 1.5 25.0 1.07	3		Volume	Temperature		Volume		Pressure		Calibration		Rate
0.781 21:0 122.22 144.83 0.798 25:0 1.5 25:0 0.818 21:0 51:56 74.70 0.817 24:0 1.5 24:0 0.870 21:0 97:50 122.22 0.873 25:0 1.5 25:0	Initial Fi	inal cm	ft ³	°C	144 144 144	ft ³	°C	in. H ₂ O		Factor	min.	lpm
21.0 51.56 74.70 0.817 24.0 1.5 24.0 21.0 97.50 122.22 0.873 25.0 1.5 25.0	75.50 51	8.90 16.60	0.781	21.0			25.0	1.5	25.0	0.988	21	
21.0 97.50 122.22 0.873 25.0 1.5 25.0	54.20 4(6.80 17.40	0.818				24.0	1.5	24.0	1.008	21	1.1
	56.50 41	8.00 18.50	0.870		97.50 122.22		25.0	1.5	25.0	1.007	22	1.1

Acceptance Criteria: Individual values of DGM calibration factor must be within $\pm 1.5\%$ of the average value. If not the calibration must be repeated. Also, the DGMCF average value must be 1.00 ± 0.05 ,

otherwise the meter must be repaired and/or adjusted as necessary and recalibrated prior to use. (Environment Canada Reference Method EPS 1/RM/8, Section 6)

1.001

ILpm

Revision June 5, 2007

ORTECH Environmental Trendicator Calibration

Calibration Procedure	03-J005
Trendicator Type	Jenco 765
МП	COE 20018
Date	January 9, 2018
Calibrated By	David Utley
Signature	DUCE
Reviewed and Accepted By	Associa

Fluke Calibrator Output	Tredicator D	Display Value	Percent Difference
(COE 20024)	Before Adjustment	After Adjustment	
(°C)	(°C)	(°C)	(%)
0	0	NA	0.0
10	10		0.0
20	20		0.0
50	50		0.0
75	75		0.0
100	100		0.0
125	125		0.0
150	150		0.0
200	200		0.0
300	300		0.0
400	400		0.0
500	500		0.0
600	601		-0.2

% Difference = (micromite - after adjustment reading)x 100 micromite

Acceptance Criteria:

Trendicator display must read within $\pm 1.5\%$ of the micromite value at each output. Otherwise, the Trendicator must be repaired and/or adjusted as necessary, and recalibrated prior to use. (MOE Source Testing Code, Version #2, Method 5)



APPENDIX 4

Mercury Analytical Report (1 page)

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Project Number: 2012889

Turn-around: Standard

(905)-822-4120*235 dutley@ortech.ca David Utley Plant: Phone: Emaíl: Contact:

ORTECH Environmental

1/24/2018 Joe Simon EPA 7473 $\pm 10\%$ Date: Method Uncertainty: Analyst(s): Method:

Trap ID	AGS Mass (ng)	Section 1 Mass (ng)	Section 2 Mass (ng)	Total Mass (ng) ¹	Section 3 Mass (ng)	Spike Level (ng)	Breakthrough (%)²	Spike Recovery (%) ³	Source	Notes
0L421340		297.2	1.0	298.2		100	0.35%		Run 1	
01445633		164.0	0.0	164.0			0.00%		Run 1	
OL445644		148.2	0.3	148.5			0.19%		Run 2	
OLC038415		433.0	0.3	433.3		250	0.07%		Run 2	
OL426826		567.5	1.3	568.8		500	0.23%		Run 3	
OL445572		164.3	0.0	164.3			0.00%		Run 3	
OL445635		112.4	0.8	113.2			0.75%		Run 4	
0L331377		946.7	0.7	947.4		800	0.07%		Run 4	
01335256		1565	1.9	1567		1400	0.12%		Run 5	
OL445603		174.8	ΓO	174.9			0.06%		RUN S QL	CoC is blank
OL445677		145.4	6.0	146.3			0.64%		Rún 6	
OL336417		2759	0.8	2760		2600	0.03%		Run 6	
•										

LOQ = 5 ng MDL = 0.46 ng

R = Data invalidation qualifier. Refer to notes ² Breakthrough = S2 / (PF+AGS+S1) ³ Spike Recovery = S3 / Spike Level ¹ Totał Mass = PF+AGS+S1+S2 For PS-12B Only

OHIOLUMEX



APPENDIX 5

Clean Harbors Process Data (18 pages)

BH dP	mmH20	PDT-622	282.5	306.9	289.2	305.7	298.2	304.6	283.3	293.3	517.5	308.3	316.2	298.9	305.1	283.2	292.1	311.7	318.4	307.8	314.1	300.7	0.105	203.0	310.7	316.4	308.4	316.8	302.4	306.4	284.4 208 5	310.6	318.4	309.3	316.6	300.5	308.1	288.6	2121	291.0	312.6	271.1	301.7	261.7	284.9	274.9	312./	200./	2.67.8	304.6	264.6
BH Inlet	mmH20	PT-615	-85.5	-819	-91.6	-81.1	-100.2	-90.2	-78,5	-91.9	-92.3	6.46-	-86.1	-96.3	-88.2	-94.5	-87.9	-88.4	-82.3	-89.6	-80.6	-21.8	-04.5	000	9.68-	-82.8	-88.0	-80.0	-96.0	-80.4	C.UE-	5.68-	-85.1	-88.6	-80.0	-93.0	-88.7	-91.5	7.05-	-90.8	-85.8	-98.8	-91.5	-105.5	-88.2	-108.7	-83.4	-110.5	-112.3	-92.7	-111.8
SDA Inlet	mmH20	PT-249	00		0	0	0	5	0	5 0	0 0		0	0	0	0	0	0	0	0	- -		5	5 0		0	0	0	0	5				0	0	0	0	0		0	0	0	0	0	0	0	5 0		0	0	0
Incinerator SDA Inlet	mmH20	PT-242A	-3.00	08.6-	-8.65	-1.20	-15.20	-/.05	-12.20	-/.65	-8.35	-10.00	-5.30	-11.30	-5.55	-10.95	-5.30	-7.05	-1.65	-6.15	-2.55	C2.21-	- 0.35	0000	-7 80	-1.15	-5.50	-0.95	-12.00		-/./- 5 5 5	-6.15	-3.45	-6.30	-0.55	-9.25	-6.00	-6.85	26.2-	-4.45	-4.55	-14.25	-8.75	-18.95	-5.90	-19.75	-3.70	-21.50	-22.90	-7.70	-22.30
Stack 1			192.9	191.8	191.8	191.8	191.8	192.9	192.9	192.9	192.9	192.9	192.9	192.9	192.9	192.9	192.9	192.9	192.9	192.9	192.9	192.9	192.01	6,261	0.261	192.9	192.9	192.9	192.9	192.9	10.01	197.9	192.9	192.9	192.9	192.9	192.9	192.9	6.24L	192.9	192.9	192.9	192.9	192.9	192.9	192.9	192.9	192.9	192.9	192.9	192.9
SDA	U	TE-204	204.0	204.0	204.0	204.0	204.0	204.0	204.0	204.5	204.5	204.5	204.5	204.5	204.5	204.5	204.0	204.0	204.0	204.0	204.0	204.0	204.5	204.5	2.4.0	204.5	204.5	204.0	204.0	204.5	204.5	2.102	204.5	204.5	204.5	204.5	205.0	205.0	205.0	205.0	205.0	204.5	204.5	204.5	204.5	204.5	204.5	204.5 204.5	204.0	204.5	204.5
Quench	U	TE-203	496.3	496.3	496.7	496.8	496.4	496.6	496.9	496.8	496.9	490.7	496.8	496.8	496.9	497.0	497.0	496.9	497.0	496.9	497.2	497.5	491.2	496.8	420.2	497.1	497.2	497.0	497.4	497.4	49/.5	497.7	497.9	497.5	497.8	497.9	497.9	498.4	498.2	497.9	498.0	498.1	498.3	498.6	498.4	498.5	498.4	498.5	498.7	498.7	499.1
Secondary	U	TE-241	1132.8	1133.0	1134.5	1134.2	1136.3	1131.5	1131.2	1129.3	1129.8	1132.1	1131.6	1132.4	1130.2	1130.3	1126.5	1128.1	1129.5	1130.8	1130.6	1131.2	1129.2	71726./	1120.2	1130.8	1130.7	1132.6	1132.1	1131.0	1130.0	1130.4	1131.2	1131.2	1132.0	1131.1	1130.5	1129.8	1130.0	1132.4	1130.9	1132.7	1131.6	1130.8	1128.7	1130.9	1130.5	1134.1	1134.3	1132.4	1131.8
Primary S		TE-240	1581.1	0.2001	1582.8	1583.4	1584.9	1584.9	1583.5	1582.6	1584.5	1584.8	1583.0	1587.0	1585.3	1586.0	1583.6	1583.0	1585.1	1583.0	1583.6	1584.3	1282.4	1584.b	C.40CL	1584.8	1584.0	1585.1	1585.0	1584.9	1586.4	1585 3	1585.1	1585.0	1582.1	1583.5	1582.9	1584.5	1583.0 1505.0	1585.1	1582.9	1583.9	1587.1	1586.8	1585.6	1584.9	1584.9	1585.9	1583.3	1584.8	1583.6
Stack	- î	FT-260C	105594	105200	107036	103771	107057	107547	10/852	106636	106584	106657	106580	108575	107156	107820	106783	107466	106502	107984	106903	108392	1064//	10/42/	106291	105539	106825	106595	106983	106226	106582	C+COUT	105505	107346	105727	107556	106344	107269	10509/	105727	105937	110164	106242	109602	106813	110617	104909	109574	109965	106203	109929
Secondary				14011	14112	13899	14124	14011	14039	13978	13966	14073	13938	14169	14023	14157	13994	14084	-+	+	13944	1419/	139/8	13901	138/2	13916	13854	14011	14051	+	+	9200T	13860	13888	14045		+	-+	1401/	13994	14051	13966	14023	13876	14011	13792	13921	13989	13994	+	H
Primary S	m3/h	PV-236	14659	14014	14659	15979	14396	14921	15184	14921	14921	14921	14921	15184	15191	14652	14921	14659	15184	15972	15177	14921	14928	14659	15716	14928	15447	15184	14659	14659	14921	TATCT	15447	14659	14389	14928	14914	14928	14396	14666	14921	14921	14659	14928	15191	14396	14389	14921	14921	14396	14396
PAC	Lbs/h	Ę	21.6	0.12	22.8	23.0	22.4	22.9	21.7	21.8	23.0	21.5	22.9	22.9	21.7	22.8	21.7	22.0	23.0	21.6	22.2	22.8	21./	22.3	27.1	21.7	21.7	22.7	22.4	22.0	21.9	23.0	27.2	21.8	21.6	22.9	22.7	22.0	21.7	22.4	22.2	22.9	21.9	23.0	22.0	22.0	22.1	21.7	22.1	22.9	22.4
Leachate		11	28.2	28.2	27.7	28.0	27.5	28.7	28.1		27.8	27.8	27.8	28.1	28.1	27.1	28.5	28.0	28.1	28.2	28.2	27.5	27.0		8.12	28.1	28.8	28.7	28.2	27.8	28.6	E.12	28.4	27.6	28.1	28.9	28.8	27.9	28.6	27.8	27.2	28.6	28.1	28.2	28.2	28.2	25.7	28.4	27.9	29.0	28.1
	SCFM			233.4	+			+	-	+	_	234.8	-	-	-		_		_	+		+	-	+	233.0	+	-	-		+	_	C.452	+	-			-	+	+	235.3	_	<u> </u>	-	$\left - \right $		_	233.3	_	234.2 234.3	-	258.8
TDU Flow TDU Flow	LPM 5	B	3.9		-	3.9		+	╉	+	3.9	-	3.9	-	3.9	3.9		-	-	-+	+	╉	-	+	2.7	+	3.9			3.9	+	7 0 0	-	3.9			+	+	+	500	-		-			-+	3.9	+	6.E	+	4.3
Alkaline TD			220.1	1.022	218.6	219.4	218.2	219.2	217.8	219.4	219.4	221.2	221.0	220.2	219.1	217.2	219.1	218.7	219.6	218.0	219.2	218.5	219.2	219.0	219.5	220.5	219.8	220.6	220.3	220.3	220.5	219.4	718.6	218.9	219.7	219.9	218.9	221.0	220.0	218.9	20.1	219.2	219.3	217.6	219.2	219.3	220.9	218.3	220.4	219.6	218.0
Lean A	LPM		-	163 5	+	-		+	+	-	+	164.4	+	_	╞		-	164.1	_		+	+	-	+	167 0	+-		-		-+	+		+-	╀	163.7		-+	+	+	164.0	╀	\vdash	-			+	+	+	165.0	+	
Emulsion	LPM	U	_	12.1	+		\vdash	-	+	+	+	11 0	-	-	-	$\left \right $		11.9	_	+	+	+	+	+	11.0	+	+	┝		+	-	12.3						+	+	11.9			-			-	+	-	11.9	+	11.9
Rich En	LPM	6	+	50.6	-	51.1		_	+	+	50.9		+-	50.8	$\left \right $	50.5	_		-	-	-	+	+	+	50.7		50.9	-		+	50.8	+		50.7				-	_	50.8	+	50.4	-				+		50.7	╞	$\left - \right $
L			-	9:12:00	-	 	\square	_	_	_	_	9:25:00			-		_	9:32:00		_	-	4	_	_	9:39:00		4-	ļ		_	_	9:47:00	_	_				_	+	9-57-00	4	-	-				-		10:06:00		10:09:00
-				+	╈	+	┝─┼	+	+	+	+	+	+	╈	-		-	-		+		+	+	-	╈	+	╈	+		+	-+-	+	╈	+				+	╈	+-	+	┢	-	\square	\square	\dashv	+	+	+	1	\square
Test No. 1		\$Date	10/01/2018	8102/10/01	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	8102/10/01	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	8102/10/01 8102/10/01	8102/10/01	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	0107/10/01	810C/10/01 8107/10/01	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	8102/10/01	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018

Test No. 1	L	Rich	Emulsion	Lean	Alkaline	Alkaline TDU Flow	TDU Flow	Leachate	PAC	Primary	Secondary	Stack	Primary	Primary Secondary	Quench	SDA	Stack	Incinerator	SDA Inlet	BH Inlet	BH dP
	<u>1</u>	LPM	LPM	LPM	LPM	ГРМ	SCFM	LPM	Lbs/h	m3/h	m3/h	m3/h	Degrees C	Degrees C	Degrees C	Degrees C	Degrees C	mmH20		mmH20	mmH20
\$Date	\$Time	FT-229	FT-219C	FT-223	PV-207	FT-313B	FT-313	PV-211	SC-PAC-FT	PV-236	PV-209	FT-260C	TE-240	TE-241	TE-203	TE-204	TE-258	PT-242A	PT-249	PT-615	PDT-622
10/01/2018	10:10:00	50.6	11.9	164.5	219.2	3.9	233.6	27.8	22.7	14396	14079	107097	1584.9	1131.1	498.5	204.5	192.9	-5.35	0	-87.2	288.8
10/01/2018	10:11:00	50.4	11.8	164.9	218.0	3.9	234.8	27.5	22.6	14666	14073	109486		1131.9	498.6	204.5	192.9	-22.80	0	-111.3	276.0
10/01/2018	10:12:00	50.9	12.3	164.6	219.8	3.9	233.2	27.7	22.7	14928	13899	105834	1586.9	1132.0	499.1	205.0	192.9	-2.55	0	-82.8	310.6
10/01/2018	10:13:00	51.0	11.9	165.1	217.3	4.0	239.4	28.3	21.9	14396	14107	109489	1586.6	1135.0	498.7	204.5	192.9	-25.75	0	-113.1	274.8
10/01/2018	10:14:00	50.7	11.8	164.6	218.7	3.9	235.1	28.1	22.5	15716	13921	105568	1584.3	1133.6	498.6	204.5	192.9	-2.45	0	-82.5	313.7
10/01/2018	10:15:00	50.4	11.7	165.1	218.5	3.9	232.9	26.9	21.7	15191	14146	107928	1585.8	1135.6	498.7	204.5	192.9	-16.50	0	-102.6	288.3

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January 10/2018	Waste Flows	fS						Flows	Air Flows		Τe	Temperatures	s				Pressures		A DESCRIPTION OF A DESC	
	Rich	Emulsion	Lean	Alkaline	TDU Flow	TDU Flow	Leachate	8 1	Primary	Secondary	Stack		Secondary		SprayDryer	Stack	Incinerator SDA Inlet	SDA Inlet		Baghouse
Test 1	FT-229	FT-219C	FT-223	PV-207	PV-207 FT-3138 FT-313	FT-313	PV-211	SC-PAC-FT	PV-236	PV-209c	FT-260c		TE-241	TE-203	TE-204 1	E-258	PT-242A	PT-249	PT-615	PDT-622
Max	51.1	12.4	165.6	221.2	4.3	259.4	29.0		15979	14264	110617		1136.3		205.0	192.9	-0.55	0.0		318,4
Nin	50.1	11.7	161.3	217.2	3.9	232.7	25.7	6	14389	13792	103771		1126.5		204.0	191.8	-25.75	0.0		261.7
Average	50.7	12.0	164.3	219.3	3.9	235.5	28.0	22.3	14896	13997	107009	1584.5	1131.4		204.4	192.8	-8.38	0.0		298.6
Variance	0.0	0.0	0.6	0.9	0.0	29.0	0.3	0.3	136179	9398	1960568	1.8	3.5	0.7	0.1	0.1	37.33	0	73.6	234.1
Construction of the second	and the second sec	Protocol and the second s	Participation of the second se	Schemetrachenoounencere	Accession of the second s	The Designation of the Designati		The second s	Toologic and the second s	wante de schauten andere an	The substantial data and the	The fight and a support of the fight of the fight of the fight of the		and the second se	and the second se					

gh dp	07Hmm	PD1-622	283.9	9.905	316.9	305.1	314.1	300.3	308.5	283.0	291.5	312.1	318.1	310.4	319.1	299.1	306.8	284.6	294.8	311.9	317.4	310.3	1.125	298.0	309.4	200.0	313.1	316.9	310.9	318.1	303.6	278.9	286.3	273.1	311.9	269.2	0.215	302.3	263.3	291.4	278.6	317.6	271.4	314.2	702 .	303.4	1.002	304.8	6 31 6	303.3	317.3	300.2	305.9
BH Inlet	mmH20	PI-615	-96.5	-00.0	-83.4	-88.2	-79.7	-96.8	-89.7	-93.4	-86.4	-88.1	-81.3	-90.2	-83.2	-93.2	-88.4	-92.6	-86.6	-89.7	-81.8	-86.0	-83./	-89.9	-88.6	0.52-	2.98-	-82.2	-87.4	-86.2	-97.0	-97.7	-91.2	-102.9	-87.7	-106.7	-8/.3	-93.3	-113.7	-95.3	-115.1	-90.6	-116.9	-90.4	-114.8	-92.5	5.CLL-	1010	1 00	-00	-88.6	-106.4	-92.3
SDA Inlet	07Hmm	P1-249	0		0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	- 	0	- - -	0				0	0	0	0	0	0	0	0			0	0	0	0	0	0	0						0	0	0
Incinerator	mmH20	P1-242A	-11.30	00 5-	-3.30	-6.15	0.05	-13.80	-6.15	-9.70	-4.80	-6.85	-3.70	-6.55	-4.40	-10.30	-5.80	-8.75	-4.90	-6.20	-1.70	-3.95	-3.55	-/.05	-5.55	-9.00	-5.40	-2.00	-4.80	-5.20	-11.20	-13.30	-7.15	-18.25	-4.95	-18.60	-0.25 24 ED	-8.75	-25.00	-11.40	-26.20	-7.45	-27.35	-8.45	-26.65	-10.35	-20.30	15 70	D/107-	-17.00	-7.25	-18.15	-8.80
	Degrees C	TE-258	192.9	197.9	192.9	192.9	192.9	192.9	192.9	192.9	192.9	192.9	192.9	192.9	192.9	191.8	191.8	191.8	191.8	190.8	190.8	190.8	190.8	190.8	190.8	8'06T	189.8	188.8	188.8	187.8	187.8	187.8	187.8	186.8	186.8	186.8	105.0	185.8	185.8	185.8	184.7	184.7	184.7	184.7	184.7	184.7	104./	183.6	0.001	183.6	183.6	183.6	183.6
SDA	Degrees C	TE-204	205.0	205.0	205.0	205.0	205.0	205.0	205.5	205.0	205.0	204.5	204.0	203.5	203.0	202.5	202.5	202.0	202.0	201.5	201.5	201.0	201.0	200.5	200.5	200.0	198 5	197.5	197.0	196.5	196.0	195.5	195.5	195.0	195.0	194.5	102 E	193.5	193.0	193.0	192.5	192.5	192.5	192.5	192.5	192.5	5.24L	107 F	L721	192.0	192.0	192.0	192.0
Quench	Degrees C	TE-203	499.4	499.4	499.5	499.2	499.5	499.7	499.5	499.9	499.7	499.7	499.7	499.7	500.0	500.1	499.8	500.2	500.1	500.3	500.2	500.0	500.2	499.9	500.0	500.3	740 5	499.5	499.1	499.2	498.6	498.5	498.0	498.1	497.9	497.3	497.2	496.5	496.6	496.4	496.1	495.7	495.5	495.2	495.0	494.6	494.5	434.4	0.404	493.6	493.2	493.2	493.2
Primary Secondary	Degrees C	TE-241	1136.7	11365	1136.8	1138.4	1139.9	1140.1	1138.1	1137.4	1137.5	1139.2	1140.6	1140.8	1140.8	1141.1	1139.9	1139.1	1139.5	1139.1	1142.1	1141.6	1142.2	1140.1	1139.1	1136./	1135.6	1137.8	1137.3	1138.7	1136.6	1135.9	1135.3	1137.1	1136.6	1137.6	1136./	1133.2	1132.3	1130.7	1131.9	1131.2	1135.3	1133.9	1135.7	1132.9	6.7511	01211	C'TCTT	11341	1133.5	1135.0	1132.8
Primary	Degrees C	TE-240	1586,4	15851	1585.1	1587.1	1583.9	1588.3	1587.1	1585.0	1584.3	1584.4	1584.3	1587.0	1584.5	1584.1	1584.9	1584.6	1584.6	1584.9	1583.3	1582.9	1582.3	1585.1	1582.9	1584.U	1584 5	1587.9	1580.8	1581.8	1584.8	1584.9	1584.5	1583.4	1584.1	1582.5	1582.9	1583.4	1582.6	1584.5	1583.8	1584.1	1582.5	1582.5	1583.5	1582.6	1584.8	0.4001 1524 2	C'+0CT	C.1861	1584.1	1581.1	1582.9
Stack	m3/h	FT-260C	107434	105637	105321	105872	106230	107323	106977	107580	105872	106141	104835	106787	105731	107071	107010	108005	106493	106894	106155	106516	105692	108309	105871	10//03	107071	106595	107488	106839	108688	106726	107421	111219	108079	109995	1106954	108278	111222	107387	110327	107502	111858	106932	110618	108783	1104/0		100000	108065	106691	108890	108293
Secondary	m3/h	PV-209	14135	14056	14011	13949	13955	13933	13972	14084	13978	13989	13882	13826	13753	14017	13865	13860	13938	13893	14000	13893	14045	13865	14017	14000	7/601	13980	13989	13871	13978	13865	13966	13989	13933	14034	13910	13938	13910	13876	13955	13798	14023	13876	14079	13966	14180	11120	67747	14051	13781	14169	13955
Primary	m3/h	PV-236	14659	14133	14396	14659	14921	14666	14396	15723	15184	14659	15460	15454	14659	14396	14659	15454	14666	14921	15184	14659	14928	14396	14396	14666	14659	14971	14126	14133	14928	14928	14928	15191	15191	14659	14666	14403	14666	15191	14666	14396	14666	14921	14666	14659	14666	14550	74057	14035	14666	14666	14396
PAC	Lbs/h	SC-PAC-FT	22.8	21.7	22.9	21.9	22.4	23.0	22.2	22.9	22.7	22.8	22.5	21.7	21.8	22.7	21.7	22.5	22.8	22.1	22.9	22.1	22.7	22.3	22.5	21.6	03 U	23.U	21.8	21.6	22.9	22.1	21.6	23.0	22.9	21.7	22.8	21.1	21.7	22.9	21.8	22.2	21.7	22.0	21.9	22.9	22.9	6.22	22.0	0 57	22.7	22.8	22.4
Leachate	LPM	PV-211	28.8	20.4	97.9	27.6	28.4	26.7	27.5	28.1	28.2	28.0	27.7	27.7	27.9	28.1	28.1	27.7	28.0	28.1	27.9	28.3	27.6	28.3	27.8	8.82	20.4	28.0	27.9	27.3	28.6	27.0	28.6	27.3	28.6	27.8	27.6	C.02	28.5	27.8	27.3	28.5	28.5	27.8	28.4	28.3	28.4	9.12	2.82	28.2	28.3	28.0	28.1
TDU Flow	SCFM	FT-313	234.2	1.962	226.7	249.6	234.1	256.7	233.9	257.3	255.8	228.8	224.8	259.1	253.9	268.8	252.9	302.2	244.4	258.0	269.0	258.5	248.6	257.5	240.0	228.2	240.4	247.2	254.6	259.7	263.6	254.9	257.5	302.7	257.4	234.2	234.6	735.7	269.9	245.6	260.9	391.7	259.4	336.1	261.6	252.2	268.0	47/97 6 VVC	244.8	328.7	435.9	256.9	264.4
3	LPM	FT-313B	3.9	2.0	4.3	4.2	3.9	4.3	3.9	4.3	4.3	3.8	3.7	4.3	4.2	4.5	4.2	5.0	4.1	4.3	4.5	4.3	4.1	4.3	4.0	4.3	7.4	1.1	4.2	4.3	4.4	4.2	4.3	5.0	4.3	3.9	3.9	0.0 0 0	4.5	4.1	4.3	6.5	4.3	5.6	4.4	4.2	4.5	4.5	4.1	5.5	7.3	4.3	4.4
Alkaline	LPM	PV-207	219.2	219.6	719.7	218.1	220.5	217.8	219.8	224.9	226.2	224.3	226.4	225.5	225.9	227.1	227.8	226.1	227.7	227.6	226.1	225.7	224.6	225.5	226.0	225.6	2,23.0	V 300	226.0	225.5	225.3	223.9	226.7	225.3	226.6	225.9	226.7	776.1	224.6	225.5	223.7	225.7	224.3	225.5	224.1	226.3	225.4	0.122	0.522	226.7	225,9	223.2	225.7
Lean	LPM	FT-223	165.6	164.U	164.7	164.0	164.7	165.0	164.2	164.4	165.2	165.0	165.1	166.2	165.3	166.3	164.5	164.6	165.0	165.1	164.6	166.0	163.2	164.6	164.8	165.0	154.7	16A 3	165.4	164.6	165.1	164.5	165.6	163.6	165.5	164.3	164.6	165 0	165.3	163.6	163.3	164.0	164.3	164.7	165.1	165.5	164.1	165.0	164.9	164.3	165.2	165.1	165.2
Emulsion	LPM	FT-219C	12.1	12.2	12.0	11.9	12.1	11.7	11.8	11.8	11.8	12.0	12.0	11.8	12.2	12.2	12.0	12.2	12.2	12.1	12.0	12.0	12.0	12.0	11.9	12.1	0'TT	12.0	11.9	12.1	12.1	11.9	12.4	12.1	12.3	12.0	12.2	0.7T	11.8	11.9	11.6	12.0	12.0	11.9	12.1	12.1	12.1	17.1	11.9	12.3	12.1	12.1	12.2
Rich	Md	FT-229	50.8	50.7	2002	50.5	50.4	50.6	50.7	50.6	50.3	50.9	50.6	50.3	50.3	50.7	51.0	50.8	50.7	50.2	50.8	50.9	50.8	50.7	50.6	50.2	50.7	1.00	50.7	50.3	50.4	50.7	50.9	50.8	50.5	50.5	50.9	20.0	50.3	50.5	50.9	50.4	50.5	50.6	50.6	50.5	50.9	50.8	50.5	50.6	50.6		50.3
	-	\$Time	10:25:00	10:26:00	10-28-00	10:29:00	10:30:00	10:31:00	10:32:00	10:33:00	10:34:00	10:35:00	10:36:00	10:37:00	10:38:00	10:39:00	10:40:00	10:41:00	10:42:00	10:43:00	10:44:00	10:45:00	10:46:00	10:47:00	10:48:00	10:49:00	10:021-00	00.12.01	10:53:00	10:54:00	10:55:00	10:56:00	10:57:00	10:58:00	10:59:00	11:00:00	11:01:00	00:20:11	11:04:00	11:05:00	11:06:00	11:07:00	11:08:00	11:09:00	11:10:00	11:11:00	11:12:00	11:13:00	11:14:00	11:15:00	11:17:00	11:18:00	11:19:00
Test No. 2	<u>ydzych domiał każenie o strucziekie da skoli dotro z najwied</u>	\$Date	10/01/2018	10/01/2018	0102/10/01 0102/10/01	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	9T07/T0/01	01UC/1U/U1	8102/10/01	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	8102/10/01 8102/10/01	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018

BH dP	mmH20	PDT-622	281.6	295.1	306.9	314.3	307.2	314.1
BH Inlet	mmH20	PT-615	-101.0	-95.6	-95.0	-87.5	-97.2	-85.1
~'I	mmH20	PT-249	0	0	0	0	0	0
Incinerator	mmH20	PT-242A	-15.45	-10.50	-11.50	-5.70	-12.10	-4,60
Stack	Degrees C	TE-258	183.6	183.6	183.6	183.6	183.6	183.6
SDA							192.5	192.5
Quench	Degrees C	TE-203	493.0	493.1	492.7	493.1	492.6	492.1
Secondary	Degrees C	TE-241	1133.6	1130.9	1131.8	1132.4	1133.8	1134.4
Primary	Degrees C	TE-240	1585.1	1585.5	1584.8	1583.5	1582.4	1583.5
Stack		FT-260C	108681	108056	108084	107393	108162	107575
Secondary	m3/h	PV-209	14107	13994	13978	13989	13978	13944
Primary	m3/h	PV-236	14133	14928	14403	14666	14666	15723
PAC	Lbs/h	SC-PAC-FT	21.6	21.7	21.8	22.7	22.0	22.0
Leachate	LPM	PV-211	28.4	28.4	27.8	29.1	28.0	28.1
TDU Flow	SCFM	FT-313	397.1	214.8	332.6	309.1	271.8	242.3
Alkaline TDU Flow TDU Flow	LPM	FT-313B	6.6	3.6	5.5	5.2	4.5	4.0
Alkaline	LPM	PV-207	222.8	227.3	225.4	225.9	225.5	228.0
Lean	Ш	FT-223	164.9	165.6	164.5	165.0	165.6	165.6
Emulsion	LPM	FT-219C	12.0	12.2	12.0	12.1	12.2	12.4
Rich	LPM	FT-229	50.4	50.8	50.8	50.4	50.5	50.4
dentati		5Time	11:20:00	11:21:00	11:22:00	11:23:00	11:24:00	11:25:00
Test No. 2		SDate	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018

January 10/2018	Waste Flows	s						Flows	Air Flows		Te	Temperatures	S				Pressures	222	and the second second	
	Rich	Emulsion Lean Alkaline TDU Flow TDU Flow Leachate	Lean	Alkaline	TDU Flow	TDU Flow	Leachate	PACFlow		Primary Secondary	Stack	Primary	Secondary	Quench SprayDryer	prayDryer	Stack II	ncinerator SDA Inlet		SD Outlet B	Baghiouse
Test 2	FT-229	FT-219C	FT-223	PV-207	FT-313B	FT-313	PV-211	SC-PAC-FT	PV-236	PV-209c	FT-260c	TE-240	TE-241	TE-203	TE-204	TE-258	PT-242A	PT-249		PDT-622
Max	51.0	12.4	166.3	228.0	7.3	435.9	29.1	23.0	15723	14180	111858	1588.3	1142.2	500.3	205.5	192.9	0.05	0.0	-79.7	321.1
Min	50.2	11.6	163.2	217.8	3.6	214.8	26.4	21.6	14126	13753	104835	1580.8	1130.7	492.1	192.0	183.6	-27.35	0.0	-116.9	263.3
Average	50.6	12.0	164.8	224.8	4.4	265.4	28.0	22.4	14757	13966	107701	1584.1	1136.3	497.4	197.6	188.2	-9.87	0.0	-93.3	299.9
Variance	0.0	0.0	0.5	6.2	0.5	1666.3	0.3	0.3	130713	8060	2402030	2.1	10.1	7.4	25.8	13.3	46.08	0	84.7	259.6
A THE REAL PROPERTY AND A THE REAL	Non-to-the second s	seguence transformersonically							The Low Concerns to Mandata Street Street	Non-second second second second second										

BH dP	mmH20	PDT-622	309.3	283.5	293.3	313.7	317.9	310.1	219.2	V U12	9 70C C	296.8	313.3	317.7	311.1	322.6	302.1	310.6	284./	309.1	292.3	311.3	273.6	302.6	260.8	289.7	273.8	273.4	313.8	270.7	313.3	269.8	287.1	311.9	268.9	309.3	286.4	298.1	290.0	308.4	316.3	305.5	7.410	304.0	276.7	289.9	306.0	313.3	303.6	7.770	6.762
BH Inlet	mmH20	PT-615	-91.7	-95.9	-90.4	-89.9	-82.9	-91.2	7.05-	0.02-	CTE-	2.40-	-88.9	-82.8	-88.8	-84.5	-98.1	-91.3	-91.4	-85.8	-91.1	-91.8	-105.5	-95.2	-105.3	-96.6	-113.6	-117.8	-91.2	-118.7	-105.0	-120.9	-95.2	-86.1	-113.5	-86.9	-109.2	-92.1	-94.9	-98.1	-89.9	-9.6	-103.7	-96.0	-98.8	-95.1	-98.5	-93.4	-93.4	1001	-102.5
SDA Inlet	mmH20	PT-249	0	0	0	0	0	00					0	0	0	0	0	0	0,0	5 0		0	0	0	0	0	0	0 0	0	0	0	0	00		0	0	0	00		0	0	00	00	0	0	0	0	0	00		-
Incinerator	mmH20	PT-242A	-8.95	-13.05	-9.00	-6.80	-2.90	-7.80	-4.3U 17 05	0 50	10.00	-755 C-	-8.50	-3.30	-6.00	-4.90	-13.85	-8.60	-8.80	-7.65	-5.00	-11.00	-18.45	-12.85	-20.70	-14.90	-29.00	-13.20	-11.75	-33.85	-21.85	-33.70	-16.75	-32.70	-28.05	-8.25	-23.85	-12.70	-13.90	-15.90	-9.20	-16.50	19 60	-13,55	-13.90	-12.55	-13.85	-8.55	-13.15	-0.50	-14.05
Stack	Degrees C	A	183.6	183.6	183.6	182.6	182.6	182.6	107 6 107 6	0.201	102 7	183.7	183.7	183.7	183.7	182.6	182.6	183.7	183.7	182.6	182.6	182.6	182.6	182.6	182.6	181.6	180.6	180.6 180.6	179.6	178.5	178.5	178.5	178.5	177.4	177.4	177.4	177.4	177.4	177.4	177.4	177.4	177.4	177.4	178.4	178.4	178,4	178.4	178.4	178.4	+.0/1	1 7 X 4
SDA	Degrees C	TE-204	192.5	192.5	192.0	192.0	192.5	192.5	107 5	C-761	0.52L	193.0	193.0	193.0	192.5	192.5	192.5	192.5	192.5	192.0	191.5	191.5	191.0	191.0	190.5	189.5	189.0	187.0	186.0	185.5	185.0	185.0	184.5	184.0	184.0	184.0	184.0	184.5	185.0	185.5	185.5	186.0	C.001	187.0	187.5	187.5	187.5	187.5	187.5	C'/QT	2121
Quench	Degrees C		491.9	491.4	491.3	490.9	490.9	490.8	490.8	490.9	450.4	430.5	490.8	490.4	490.1	490.2	490.4	490.3	490.0	490.4	489.6	489.5	489.4	489.4	489.1	489.2	488.4	488.2	487.3	486.9	487.3	486.7	486.5	485.5	485.5	485.4	485.3	484.8	485.0	484.6	485.0	485.1	10.201	485.1	485.1	484.9	484.7	484.4	485.1	404.0	1 2 2 1
Secondary			1132.7	1131.7	1131.8	1133.8	1138.2	1141.2	1141.8	C 0711	C.0411	1137.0	1137.4	1138.2	1137.2	1138.0	1137.2	1136.1	1134.3	1136./	1132.2	1129.0	1129.8	1127.9	1124.7	1120.4	1120.4	1123.1	1121.3	1122.2	1118.7	1116.7	1119.3	1130.1	1136.3	1137.6	1141.1	1139.4	1140.2	1142.0	1141.4	1142.7	C.2411	1142.1	1140.3	1139.2	1139.7	1139.8	1141.4	2.1411	
Primary	Degrees C Degrees C	TE-240	1586.8	1585.3	1583.9	1583.8	1583.3	1584.1	1585.8	C.COCT	1501.5	1583 5	1585.0	1584.1	1587.0	1584.9	1586.3	1587.1	1589.9	1585.3 1588 A	1587.4	1588.6	1585.3	1589.0	1589.0	1590.5	1590.3	1592.0	1590.3	1588.5	1588.5	1590.0	1587.0	1588.0	1586.5	1585.4	1587.4	1587.3	1587.8	1588.3	1589.5	1585.0	1505.6	1588.9	1588.3	1589.6	1588.9	1588.8	1588.0	1280.4	2.1.1.1.1.1.1
Stack	m3/h	1.	108081	109474	106257	108956	107255	108275	571/0T	DTO/OT	107550	107681	108176	107976	107823	106396	108740	107778	109082	108312	106590	107286	110092	107516	112238	109454	111808	111664	108196	111766	110000	111621	107911	107777	110732	106602	108435	108216	106947	108490	106825	107870	100050	107526	108285	107534	107374	107598	107748 106695	100070	
Secondary	m3/h	PV-209	13775	13916	14006	13949	13848	13719	13848	HCOCT	138/6	13798	14017	13893	13899	13815	13927	13775	14034	13905	13865	13927	13876	13972	13978	13843	14023	13933	13876	13978	13949	14045	14017	13876 13876	14146	13820	14056	13905	13927	13916	14045	13938	14061	13809	13949	13837	13966	13826	13905	15933	
Primary 1	m3/h	PV-236	14928	15723	14928	15191	14921	14928	19191	14070	14928	15773	14403	14666	14928	15191	15993	15198	14666	14666	14928	14666	14140	14928	14396	14666	14666	14928	14403	14666	15191	14928	14403	15460	14928	14403	14666	14672	14935	14403	14928	14672	14070	14666	14403	14403	14403	14666	14140	14403	
PAC	Lbs/h	SC-PAC-FT	22.7	21.9	21.8	22.0	21.6	21.7	22.8	1.12	6.1.2	1 27	21.8	23.0	22.4	22.9	21.7	22.3	22.2	21.7	0 66	23.0	23.0	22.6	22.9	23.0	22.9	21./	22.3	22.0	22.9	23.0	22.9	22.4	22.9	22.0	22.8	22.6	22.8	21.8	22.9	21.7	27.3	2.22	22.4	23.0	22.9	21.7	23.0	27.8	
Leachate	LPM	11	~	27.2	28.1	29.1	28.2	28.8	1.62	2.02	7.97	28.7	28.0	28.5	28.7	28.6	28.1	28.2	28.0	28.1	28.8	28.2	29.0	28.3	28.2	28.0	28.4	29.1	28.0	28.5	28.2	28.7	28.7	28.2	28.3	28.3	27.9	28.2	28.1	28.5	27.3	28.1	28.0	1 80	28.4	28.6	28.5	28.4	28.5 27 a	6.12	
TDU Flow L		\vdash		259.7	194.9	259.7	322.7	250.1	241.8	T-0/7	436.3	347.2	245.7	435.5	435.2	436.0	308.3	436.1	436.1	340.4	287.6	241.7	289.1	436.1	287.6	296.7	435.8	273.5	254.1	214.5	299.5	420.2	239.4	259.1	365.0	259.5	262.1	436.6	319.6	265.4	247.5	264.3	281.0	2775	315.5	360.2	252.6	251.3	253.0	242.8	
TDU Flow T	÷	m	<u> </u>	4.3	3.2	4.3	5.4	4.2	4.0	0.4	/.3	2.0	4.1	7.3	7.3	7.3	5.1	7.3	7.3	5.7	4.4	4.0	4.8	7.3	4.8	4.9	7.3	4.6	4.2	3.6	5.0	7.0	4.0	4.3	6.1	4.3	4.4	7.3	4.4 5.3	4.4	4.1	4.4	4.7	4.4	5.3	6.0	4.2	4.2	4.2	4.1	
Alkaline 1	<u> </u>	L	┢──	225.0	225.4	225.4	226.6	227.0	226.4	0.022	1.122	1 1 2 2 2 2	225.0	225.1	227.1	225.8	225.3	226.1	226.8	226.3	V V C C	225.4	224.8	226.3	225.0	225.5	224.3	225.7 226.6	227.6	224.7	226.5	225.9	227.0	225.1	224.7	227.3	226.0	227.6	220.4	225.6	226.3	224.4	226.8	7.767	224.5	225.8	225.0	226.4	224.7	227.3	
Lean		FT-223	164.2	165.4	164.7	165.8	164.2	164.6	165.0	102.0	165.0	0.40T	165.7	164.3	165.1	162.2	164.3	163.8	164.4	165.8 164 E	V 164 A	163.6	161.8	164.7	161.9	157.9	153.7	155.0	159.1	159.5	160.2	159.8	147.9	148.3	156.0	156.0	155.6	155.9	156.8	156.3	159.4	157.5	158.4	47.71	159.8	157.5	159.0	158.4	159.3	160.1	
Emulsion	LPM	FT-219C	12.1	11.9	11.7	11.8	12.2	12.0	12.1	A.LL	12.2	110	12.0	12.0	12.0	12.1	12.0	12.0	12.1	12.0	11 0	12.0	11.6	12.0	11.7	12.0	11.8	11.8	17.3	11.9	12.1	12.2	11.9	11.6	11.8	12.2	12.1	12.2	10 3 17.7	12.0	12.0	11.7	12.0	12.0	11.8	11.9	11.9	11.9	11.9	12.2	
Rich E	\vdash	1	┢──	50.8	50.8	50.4	50.3	50.7	51.0	20.7	50.3	20.7	50.2	50.4	50.5	50.9	50.7	51.1	50.6	50.9	0.10	503	50.2	50.4	50.6	50.8	50.4	50.4	50.8	50.6	50.7	50.4	50.6	51.0	50.8	50.7	50.7	50.4	50.4	51.0	50.9	50.6	50.6	20.5	50.6	50.2	50.5	50.3	50.6	50.8	-
<u> </u>	1	\$Time	11:35:00	11:36:00	11:37:00	11:38:00	11:39:00	11:40:00	11:41:00	11:42:00	11:43:00	00'44'11	11:46:00	11:47:00	11:48:00	11:49:00	11:50:00	11:51:00	11:52:00	11:53:00	11-55-00	11-56-00	11:57:00	11:58:00	11:59:00	12:00:00	12:01:00	12:02:00	00-00-01	12:05:00	12:06:00	12:07:00	12:08:00	12:09:00	12:11:00	12:12:00	12:13:00	12:14:00	12:15:00	12:17:00	12:18:00	12:19:00	12:20:00	00.02.21	12:23:00	12:24:00	12:25:00	12:26:00	12:27:00	12:28:00	
Test No. 3		SDate	18	10/01/2018 1	10/01/2018 1			\uparrow	\uparrow	╈	10/01/2018 1	\uparrow	1	\top			-	-	+	10/01/2018 1	+	\uparrow	+	+	10/01/2018 1	1	+	10/01/2018 1	T	T	\square		+	10/01/2018 1	+	10/01/2018 1		\uparrow	1 10/01/2018 1	\uparrow			╈	F 8102/10/01	╈	\top	\vdash	10/01/2018 1		10/01/2018 1	•

ncinerator SDA inlet BH Inlet BH dP	mmH20 mmH20	42A PT-249 PT-615 PDT-622	-15.40 0 -104.6 281.3	-7.40 0 -94.7 288.2	-11.10 0 -98.1 306.3	0 -91.9	20 0 1 27 A 2020
Stack Incine	Degrees C mmH2O	TE-258 PT-242A	178.4 -15	178.4 -7.	178.4 -11	178.4 -6.95	170 0 0 0 0
SDA	Degrees C De	TE-204 T	187.5	187.5	187.5	187.5	187 C
/ Quench	Degrees C	TE-203	484.3	484.4	484.6	484.6	2 484 3
/ Secondary	C Degrees (TE-241	1139.8	1139.3	1141.2	1141.3	11119
Primary	Degrees C	TE-240	1590.1	1588.4	1587.4	1588.6	15875
ry Stack	m3/h	FT-260C	108623	107824	107946	108172	108620
y Secondary	m3/h	PV-209	13933	13815	13832	13815	13905
Primary	m3/h	PV-236	14672	14133	14672	14928	14403
PAC		SC-PAC-FT	21.6	21.9	21.8	23.0	31.8
Alkaline TDU Flow TDU Flow Leachate	LPM	PV-211	28.5	28.5	28.0	28.4	2 8 6
v TDU Flov	LPM LPM SCFM	FT-313	265.2	259.5	266.8	258.2	750.4
TDU Flov	LPM	FT-313E	4.4	4.3	4.4	4.3	· ·
	<u> </u>		1	225.9	225.4	225.8	-
n Lean	1	Ľ.	1	162.7	160.3	160.4	160 5
Emulsion	┢	Ľ	-	-	-		-
Rich	ПРМ	Ľ	_	0 50.6	0 50.4	0 50.2	
		\$Time	1		-	-	+
Test No. 3		\$Date	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2010

January 10/2018	Waste Flows	VS	Non-Contribution Contractor	The second s	No. of Concession, Name	Constant of Constant of Constant of Constant of Constant		Flows	Air Flows		Ì	Temperatures					Pressures			
	Rich	Rich Emulsion Lean Alkaline TDU Flow Leachate	Lean	Alkaline	TDU Flow	TDU Flow	Leachate	PACFlow	J	Primary Secondary	Stack	Primary	Primary Secondary Quench SprayDryer	Quench 5	brayDryer	Stack II	ncinerator SDA Inlet SD Outlet	SDA Inlet		Baghouse
Test 3	FT-229	FT-229 FT-219C	FT-223	PV-207	FT-3138	FT-313	PV-211	SC-PAC-FT	PV-236	PV-209c	FT-260c	TE-240	TE-241	TE-203	TE-204	TE-258	PT-242A	PT-249	PT-615	PDT-622
Max	51.1	12.3	165.8	227.6	7.3	436.6	29.1	23.1	15993	14146	112238	1592.1	1144.9	491.9	193.0	183.7	-2.90	0.0	-82.8	322.6
Min	50.2	11.6	147.9	224.3	3.2	194.9	27.2	21.6	14133	13697	106257	1581.3	1116.7	484.3	184.0	177.4	-33.85	0.0	-120.9	260.8
Average	50.6	12.0	160.4	225.9	5.0	300.9	28.4	22.4	14774	13907	108426	1587.2	1135.0	487.5	188.8	180.3	-13.32	0.0	-96.4	298.4
Variance	0.1	0.0	17.9	0.8	1.3	4738.9	0.2	0.3	140289	7798	1961977	4.8	57.2	7.0	10.1	6.2	60.00	0	81.8	244.3
Record and the second se		-	period of the second descent second			and the second	and the second s	STORANTI MINISTRATION AND STORAGO	ridenterations and a second se			-								

BH dP	mmH20	PDT-622	290.8	284.4	0.002	301 1	0 836	300.4	253.9	290.4	250.6	281.6	271.1	309.9	265.8	308.6	263.6	300.3	4.8C2	C 100	7100	243.8	308.1	291.0	297.5	273.7	282.4	301.3	309.0	298.6	0.000	296.6	274.5	287.2	296.4	305.9	308.4	299.1	308.9	0.622	283.7	304.6	312.1	303.4	312.1	298.0	304.0	283.2	292.4	319.8	305.0	315.8
BH Inlet	mmH20	PT-615	-98.3	-98.7	C.02-	2 V0-	1120	-93.9	-111.6	-96.8	-114.6	-98.4	-121.9	-97.0	-123.6	-96.8	-122.8	-103.9	7.621-	C 111	2 90	-111.6	-95.3	-113.1	-101.8	-107.5	-98.9	-102.7	-94.7	-101.4	-34./ -109.6	0.66-	-105.4	-102.0	-98.0	-95.7	-93.7	-97.2	-97.8	-100.9	-102.4	-99.4	-93.7	-92.2	-84.3	-98.6	-92.7	-97.7	-92.6	-90.4	-89.5	-84.7
SDA Inlet	mmH20	PT-249	0	0					0	0	0	0	0	0	0	0	0	5					0	0	0	0	0	0	0	0	5 0		0	0	0	0	0	0	00		0	0	0	0	0	0	0	0	0 0	00	, 0	0
Incinerator SDA Inlet	mmH20	PT-242A	-7.05	-7.05	00.2-	003	-17 45	-4.95	-15.90	-5.50	-18.25	-8.65	-25.55	-6.85	-26.80	-4.55	-25.90	-11./0	C7'07-	17 50	36 2	-16.25	-5.20	-19.95	-10.00	-14.25	-7.80	-10.35	-4.90	-11.35	13 70	-8.20	-14.50	-11.80	-8.65	-6.40	-7.75	-5.15	-5.70	-10.8-	-10.55	-10.30	-6.10	-10.95	-6.15	-16.45	-11.25	-15.15	-10.90	-9.55	00.6-	-5.90
Stack	Degrees C	TE-258	179.4	179.4	100.4	170.2	C'2/T	179.3	179.3	180.4	180.4	180.4	180.4	180.4	180.4	180.4	179.3	1/9.3	C 027	C'6/T	C.6/1	179 3	179.3	179.3	179.3	179.3	178.3	178.3	178.3	178.3	5.8/T	178.3	178.3	178.3	177.3	177.3	177.3	177.3	177.3	5.771	177.3	177.0	177.0	177.0	177.0	177.0	177.0	177.0	175.9	175.9	175.9	175.9
SDA	U	TE-204	189.0	189.0	0.001	190 F	180 E	189.5	189.5	189.5	189.5	189.5	189.5	189.5	189.0	189.0	188.5	188.5	1001	C.001	100 E	188.0	188.0	187.5	187.5	187.0	187.0	186.5	186.5	186.5	126.0	186.0	186.0	186.0	186.0	185.5	185.5	185.5	185.5	185.0	185.0	185.0	184.5	184.5	184.5	184.0	184.0	184.0	184.0	184.0	183.5	183.5
Quench	S	TE-203	484.1	484.2	484.2	484.0	181 6	484.4	484.5	484.4	484.5	484.4	484.9	484.8	484.8	484.8	484.4	484.3	484.8	404.7	404.2 101 E	404.7	484.2	483.9	484.2	484.0	483.6	483.5	483.2	483.5	483.2	482.7	482.6	482.8	483.0	482.4	482.2	482.2	482.3	402.4	481.8	481.5	481.5	481.4	481.1	480.9	480.9	480.8	480.8	480.8	480.2	479.8
Secondary	Degrees C	TE-241	1144.3	1144.1	1143,4	11/13 6	0.0411	1144.9	1146.6	1144.5	1144.5	1142.7	1143.7	1144.0	1146.1	1145.6	1146.1	1141.9	1141.8	776577	1120.0	C CT11	1139.5	1140.7	1136.6	1137.0	1135.2	1135.6	1137.0	1138.5	1140.7	1135.8	1134.3	1134.0	1134.4	1135.9	1136.8	1136.3	1136.8	1130.0	1132.3	1130.6	1132.8	1132.4	1133.1	1132.3	1131.8	1131.3	1131.4	1133.5	1133.3	1134.4
Primary [TE-240	1585.4	1585.8	1707 0	1583.8	1505 E	1584.3	1586.8	1586.3	1584.4	1585.6	1586.0	1584.9	1587.1	1587.3	1588.9	1589.3	158/.8	0.7001F	1.500 L	1587 Q	1588.1	1589.3	1590.6	1588.3	1589.9	1587.3	1586.6	1588.9	158/.4	2 7077	1588.9	1586.3	1589.0	1587.4	1585.3	1584.5	1585.4	0.08CL	1587.0	1585.9	1584.6	1584.8	1583.8	1584.1	1585.5	1585.8	1588.0	1586.5 1586.3	1586.8	1582.9
Stack		FT-260C	107288	106703	10044/	Tq/60T	T70/01	106673	110156	107141	110286	107689	110051	106811	109896	106554	110906	108688	109955	1004/3	106245	107731	107013	108875	108996	109783	107192	107438	106255	107498	10000E	10200T	108291	107861	108607	106801	106936	106752	107022	107528	108252	107351	107579	107519	107131	109481	107202	109038	107059	108693 107463	108552	106550
Secondary	m3/h	PV-209	13899	13860	13//2	13674	613C1	13612	13663	13787	13697	13685	13893	13680	13876	13758	13994	13663	13/8/	130/4	13989	13708	13860	13860	13876	13921	13758	13989	13758	13860	13635	13775	C7/CT	13736	13871	13753	13674	13685	13691	13752	13843	13781	13860	13747	13949	13860	13860	13961	13646	13860	13854	13854
Primary	m3/h	PV-236	14666	15986	14935	14000	16100	14140	14928	14928	14140	14666	14666	14672	14396	14403	14666	14410	14935	96TCT	14000	14000	14133	14928	14672	14935	15993	14666	14666	14672	14403	7/0+T	14075	14935	14935	14403	14935	14410	14666	16100	14935	14928	14666	14672	14403	15460	15460	14935	15198	15198	14935	14403
PAC	Lbs/h	SC-PAC-FT	21.6	21.7	5.22	23.0	0.22	22.8	23.1	23.0	21.6	22.0	21.8	22.9	21.7	23.1	23.1	22.4	21.8	8.77	8,77	6.77	03.0	22.7	22.0	23.0	22.5	21.7	21.8	21.7	22.8	0.22	0.62	23.0	21.7	22.7	21.7	22.7	22.4	1.1/	21.9	21.7	22.1	23.0	22.9	21.6	22.9	22.1	22.4	21.8	22.3	22.9
Leachate	LPM	PV-211 S(27.6	29.3	28.4	28.0	20.2	28.3	28.7	29.1	28.2	26.5	28.5	29.1	28.1	28.7	28.7	28.3	28.1	28.7	1.67	20.2	28.0	28.7	27.8	28.7	27.1	28.3	28.2	27.9	29.4 26 r	C.02	L 22.22	78.3	28.7	28.4	29.0	28.8	29.3	28.3	1 80	28.7	28.8	28.7	29.0	29.3	28.7	28.5	28.5	29.3 28 5	28.9	29.1
IU Flow Le		-		-	-	258.3 757 E	-	-	╞	+	-	╞	248.1				-+	234.5	+	+	+	47.72	+	+	+	-	-	235.7		-	258.9	+	250.0 0.00	+	260.0			_	234.2	-	234./ 235.4	-		-		233.3		258.8		235.6		257.6
TDU Flow TDU Flow	LPM	8	-	+	+	4.3	_	╇	+	4.3	╀	-	4.1					_	+	+	╉	5.4 0 0	╀	9.6	-	-			-		_	╉	2.0	╀	4.3			3.9		+	2.0	┼	┢	-						9.6 0 c	+-	4.3
e	LPM		228.0	226.2	226.0	225.4	7.022	0.622	224.7	227.3	224.9	227.8	226.4	227.4	225.3	228.3	227.4	226.4	225.2	225./	1.622	221.3	225.4 276.0	0.770	228.8	226.5	228.3	227.0	228.2	226.0	226.6	2,622	2.622	2.22.0	226.9	228.9	226.4	228.1	228.3	227.0	220.4 275 q	226.1	227.5	225.9	228.6	228.8	228.4	226.5	228.0	228.3	226.3	226.1
Lean A	LPM	FT-223	-	+	+	+	╋	163.9	+	+	╀	-	\vdash	-				\rightarrow	+	+	+	1.501	+	+	+	+	-		163.6	-+	-	+	4700T	+	+			165.4	+		165 7	+	-	+		163.0		164.2		161.7	+-	163.7
Emulsion	LPM	U	12.0	11.8	12.2	12.0			+	╀	┢	-						+	11.9	17.1	11.8	11.8	12 1	11 9	12.0	12.0	12.0	12.2	12.0	11.7	12.1	\$717	T.2L	V CL	12.2	12.4	11.9	12.2	12.3	12.1	11.7	11.9	12.2	11.9	12.2	12.3	12.2	12.2		12.2	+	12.0
Rich E	LPM	FT-229 F	50.8	50.5	50.8	50.6	50.5	20.2	50.8	50.8	50.6	50.6	50.6	50.7	50.6	50.6	50.3	50.0	50.1	50.7	50.3	1.02	5.UC	50.6	50.3	50.8	50.7	50.4	50.1	50.5	50.7	50.5	50.3	50 E	50.7	50.5	50.9	50.3	50.1	50.5	50.7	50.3	50.8	50.4	50.5	50.4	50.2	50.5	50.8	50.8	50.5	50.6
L		\$Time	12:53:00	12:54:00	12:55:00	12:56:00	00.01.01	12-59-00	13:00:00	13-01-00	13:02:00	13:03:00	13:04:00	13:05:00	13:06:00	13:07:00	13:08:00	13:09:00	13:10:00	13:11:00	13:12:00	13:13:00	00:47.01	13-16-00	13-17-00	13:18:00	13:19:00	13:20:00	13:21:00	13:22:00	13:23:00	13:24:00	13:22:00	12.27.00	13:28:00	13:29:00	13:30:00	13:31:00	13:32:00	13:33:00	13:34:00	13-36-00	13:37:00	13:38:00	13:39:00	13:40:00	13:41:00	13:42:00	13:43:00	13:44:00	13:45:00 13:46:00	13:47:00
Test No. 4		\$Date		+	\uparrow	+	╈	1 8102/10/01	\top	\uparrow	\top	\uparrow	\square	\vdash	\vdash			-	\uparrow	╈	\uparrow	T 8107/10/01	╈	1	1	+	┢	┢──	10/01/2018 1		+	╈	T 8T07/T0/01	+	1	┢		10/01/2018 1	\uparrow	╈	1 8102/10/01	╈	\uparrow		\square	\square		10/01/2018 1	\vdash	10/01/2018 1	+	10/01/2018

6	Rich	Emulsion	Lean	Alkaline	Alkaline TDU Flow TDU Flow	TDU Flow	Leachate	PAC	Primary	Secondary	Stack	Primary	Secondary	Quench	SDA	Stack	Incinerator 5	SDA Inlet	BH Inlet	BH dP
	1	LPM		ГРМ	LPM	SCFM	LPM	rbs/h	m3/h	m3/h	m3/h	112	Degrees C		Degrees C	Degrees C	I	mmH20	mmH20	mmH20
\$Time	FT-229	FT-219C	FT-223	PV-207	FT-313B	FT-313	PV-211	SC-PAC-FT	PV-236	PV-209	FT-260C		TE-241	TE-203	TE-204	TE-258		PT-249	PT-615	PDT-622
	50.7	12.1	162.5	226.4	-	234.7	28.2	21.9	14403	13966	108781	1584.8	1133.1	479.7	183.5	175.9	-17.60	0	-102.2	300.7
18	51.0	11.9	162.0	225.9	<u> </u>	257.7	28.3	21.8	14410	13837	107360	1584.1	1133.1	479.9	183.5	175.9	-10.70	0	-92.7	305.1
13:50:00	50.9	12.0	161.0	227.3		233.0	28.3	22.1	14666	13860	108003	1583.9	1130.9	479.4	183.5	175.9	-15.35	0	-98,2	284.5
13:51:00	50.7	12.1	160.5	227.2	4.3	258.5	28.3	22.0	14935	13837	108649	1585.0	1131.3	479.6	183.5	175.9	-16.65	0	-100.2	272.9
13:52:00	50.6	12.3	163.0	227.8	3.9	236.1	28.3	22.9	14410	13747	107857	1586.1	1131.8	479.2	183.0	175.9	-11.80	0	-94.2	310.7
13:53:00	50.4	11.9	160.6	227.7	4.3	258.2	28.7	22.7	14935	13624	108912	1583.3	1134.1	478.9	183.0	175.9	-20.70	0	-106.8	272.2

January 10/2018	Waste Flows							Flows	Air Flows		Чe.	Temperatures	th			1	ressures			
	Rich	Emulsion	Lean	Alkaline	TDU Flow	TDU Flow	Leachate		Primary	Secondary	Stack			Quench 5			icinerator SI	DA Inlet 5	_	aghouse
Test 4		FT-219C	FT-223	PV-207	FT-3138	FT-313	PV-211	SC-PAC-FT	PV-236	PV-209c	FT-260c	TE-240	TE-241	TE-203 TE-204		TE-258	PT-242A	oT-249	PT-615	PDT-622
Max	51.0	12.4	166.4	228.9	4.3	260.0	29.9	8	15993	13994	110906			484.9			-4.55	0.0	~~~~	319.8
Min		11.7	160.5	224.7	3.3	197.7	26.5	21.6	14133	13612	106255		1130.6	478.9	183.0	175.9	-26.80	0.0		250.6
Average	50.5	12.0	163.7	226.8	7 226.8 4.1 247.5	247.5	28.5	22.3	14764	13792	107968	1586.4	1137.8	482.8	186.5	178.2	-11.60	0.0		292.6
Variance	0.1	0.0	2.1	1.3	0.0	171.0	0.3	0.3	146914	10566	1365689	3.4	25.0	3.2	4.9	2.3	33.53	0	81.3	281.5
and a second contract of the second statement of the s	And and a second s	NOTIFIC TRANSPORTED IN THE OWNER WATER OF THE OWNER OF THE OWNER WATER OF THE OWNER WATER OF THE OWNER	which we are a set of the set of	STATISTICS IN CONTRACTOR OF STATISTICS	Non-sector sector secto	ten aucoren and alance vehicle me	Construction of the construction of the construction	Children and the second s	Traditional Statistics and a state	This and so that the second sec	The second state of the se	The second s	Total of the back							

BH dP	mmH20	PDT-622	281.3	308.9	313.9	305.3	275.8	294.9	259.3	278.4	262.6	303.3	258.4	302.3	254.8	294.3	257.8	286.6	266.0	307.9	1 012	170 5	1 100	204.1 2016	9 292	307.6	315.8	307.7	312.1	300.2	309.8	284.7	292.7	314.1	312.6	320.9	300.9	310.6	286.1	297.0	307.9	312.6	312.7	291.9	303.4	285.0	292.6	305.5	310.3	305.7	311.4	306.0	285.1
BH Inlet	-+		-98.6	-89.1	-89.1	-90.6	-92.1	-97.5	-104.3	-93.2	-106.4	-87.4	-107.8	-86.7	-108.4	-91.9	-112.5	-95.6	-113.0	-90.1	+'CTT-	110 0	0.00 0.00	-20.0	0 00-	-105.2	-92.9	-111.5	-93.8	-114.8	-106.6	-112.0	-102.9	-106.5	-79.9 109 6	-99.3	-111.8	-107.6	-112.1	-105.6	-102.9	-97.8	1 70-	-105.4	-99.8	-110.1	-102.0	-100.6	-93.6	-102.2	-93.4	-100.7	-108.0
SDA inlet		PT-249	0		0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0							0	0	0	0	0	0	0	0			0	0	0	0	0	00		, o	0	0	0	0	0	00	00	0	0
		PT-242A	-10.75	- 2000-	-2.80	-4.95	-6.15	-8.45	-12.25	-5.05	-15.20	-2.75	-16.30	-0.80	-14.95	-3.45	-18.80	-6.00	-18.25	-2.95	C7.02-	01 00	0T.62-	CD.C-	-14 70	-18.00	-8.10	-23.40	-9.25	-23.55	-19.20	-23.10	-16.95	-18.60	-1815	-11 95	-21.40	-17.25	-18.70	-14.20	-11.25	-9.40	7 75	-13.10	-9.70	-18.45	-11.30	-11.70	-5.90	-11.70	-5.70	-11.00	-13.85
Stack	0	TE-258	180.2	180.2	181.3	181.3	181.3	182.5	183.6	183.6	183.6	183.6	184.7	184.7	185.7	185.7	186.7	186.7	186.7	186.7	107 7	1.101	1.101	1.001	188.7	188.7	187.6	186.6	186.6	185.6	184.5	184.5	183.4	182.3	181 2	181 3	181.3	181.3	181.3	181.3	181.3	181.3	181 3	181.3	182.4	182.4	182.4	182.4	182.4	182.4	182.4	183.4	183.4
SDA		TE-204	191.5	192 5	193.0	194.0	194.5	195.0	196.0	197.0	198.0	198.5	198.5	199.0	199.5	200.0	200.5	201.0	201.5	202.0	3 000	2.202	C.2U2	2.202	C.202	2005	198.5	197.0	195.5	194.0	193.0	192.0	191.0	190.0	180 U	189.5	190.0	190.5	190.5	191.0	191.5	191.5	2 101 C'TCT	191.5	191.5	192.0	192.0	192.0	192.5	192.5	193.0	193.0	193.5
Quench	U	TE-203	480.4	480.5	481.1	481.2	481.3	482.2	482.6	482.6	483.2	483.8	483.8	484.4	485.1	485.5	486.0	486.2	486.6	487.0	481.2	0.104	48/.8	488.5	180.0	2.024	489.3	489.0	488.9	488.6	488.2	487.8	487.2	486.8	486.2	486.4	486.3	485.6	485.7	485.9	485.8	485.5	400.U	485.7	485.7	485.8	486.2	486.3	486.5	486.3	486.7	400.4	486.9
Secondary	U	TE-241	1146.2	1151 1	1155.6	1155.9	1159.5	1161.6	1165.6	1167.2	1169.6	1170.8	1172.7	1173.1	1174.2	1172.9	1172.8	1172.6	1173.0	1172.3	4175 C	0.0711	11/2.2	0.0/11	0.2111	1161 0	1151.8	1145.2	1142.1	1139.7	1135.7	1133.3	1129.3	1128.0	C.82LT	1135.3	1137.8	1137.2	1138.7	1139.5	1139.7	1143.6	2.0411	1146.8	1145.4	1143.3	1142.9	1142.5	1142.2	1143.0	1143.6	1142.4	1140.6
Primary	Degrees C	TE-240	1577.5	1578 5	1579.8	1577.4	1579.9	1579.1	1580.1	1578.3	1580.1	1580.0	1583.4	1581.9	1585.6	1581.6	1582.6	1581.9	1581.3	1580.5	1583.4	4-700TF	1583.6	8.28CL	C.0/CT	1574.0	1569.5	1567.6	1565.8	1561.6	1558.9	1553.9	1552.6	1552.1	1552.3	1558 0	1557.6	1561.1	1558.5	1560.4	1559.8	1559.4	0.156CL	0.00CT	1559.5	1560.9	1560.5	1559.1	1561.6	1560.1	1560.1	1559.0	1560.3
Stack	m3/h	FT-260C	106565	1/6001	105916	105698	105548	107269	105137	106666	109202	106235	109372	104920	108668	105970	110186	107346	109861	107100	110063	000007	110255	106958	106/201	107513	107130	107250	106952	108220	109193	108786	108460	108492	10/606	100901	109693	107852	109899	108378	108017	106101	TUESTO	0TOCUL	107757	108393	107258	108280	106390	107941	106681	106617	107476
Secondary	m3/h	PV-209	13854	040CT	13641	13792	13680	13832	13781	13708	13635	13618	13523	13770	13787	13702	13674	13657	13826	13567	13//U	/0007	13//0	13/53	QTAST	113871	13753	13848	13641	13994	13641	13775	13916	13809	13803	12524	13843	13719	13843	13702	13719	13708	C2/CT	4T/CT	13837	13854	13815	13815	13523	13792	13551	13/35	13787
Primary	m3/h	PV-236	14666	14147	14403	14928	14403	15993	14140	14672	14935	14403	14928	14403	14935	15198	14410	14666	14140	14410	15205	14735	14403	15198	14735	0T++T	14403	14928	14672	14672	14666	15198	14679	14942	14672	15773	15198	14666	14679	14403	14666	14403	149.28	14000	15730	15198	15198	14140	14928	14666	14410	144U3 14679	14928
PAC	Lbs/h	SC-PAC-FT	22.9	8.22	22.3	22.8	22.7	22.2	22.0	22.9	21.7	22.9	22.0	21.6	23.0	22.8	22.8	22.3	22.3	22.9	21.8	7.1.2	23.0	22.9	21.0	010	21.7	21.6	21.9	21.6	23.0	22.7	22.7	22.8	21.7	0.77	0.22	22.3	22.9	22.4	22.9	22.6	1.22	8'77 8'77	21.8	22.3	22.9	22.3	22.1	21.7	22.6	23.0	22.5
Leachate	LPM	PV-211	29.5	0.62 V DC	28.8	28.6	29.4	28.2	29.9	29.0	29.0	29.0	28.6	28.7	28.8	28.8	29.2	29.4	29.1	30.0	29,6	23.4	29.0	29.5	2.62	0 00	0.02	29.0	28.7	28.7	28.8	28.7	29.6	29.0	28.9	20.02	78.4	30.0	28.9	30.7	29.1	29.3	29.5	C.62	28.4	28.8	29.0	29.2	28.6	28.7	28.9	28.6	30.0
	SCFM	FT-313	234.4	1.822	234.3	258.8	258.4	258.2	251.7	257.2	234.8	234.2	233.0	258.7	258.2	233.3	258.5	259.3	258.4	258.5	259.2	228.3	257.6	259.3	0.862	234.2	133.4	235.7	235.8	235.1	234.4	233.0	235.7	233.9	234.6	7.002	1355	258.1	234.3	258.6	258.3	259.8	260.0	234.0	258.3	235.1	258.3	259.1	260.4	233.6	234.2	233.6	234.0
TDU Flow TDU Flow	LPM	FT-313B	3.9	4.3	5.6	4.3	4.3	4.3	4.2	4.3	3.9	3.9	3.9	4.3	4.3	3.9	4.3	4.3	4.3	4.3	4.3	4.3	4.3	4.3	4.3	2.2	0 0	202	3.9	3.9	3.9	3.9	3.9	3.9	3.9	6.4	2.0	4.3	3.9	4.3	4.3	4.3	4.3	4.7 0 0	4.3	3.9	4.3	4.3	4.3	3.9	3.9	9.5 9.5	3.9
Alkaline	LPM	PV-207	226.1	6.622	225.0	227.2	225.3	226.4	226.8	228.2	226.3	226.9	226.8	226.9	225.0	226.2	225.0	226.5	225.8	227.3	225.6	1./22	226.8	227.6	226.3	275.1	10900	E VCC	226.6	224.6	227.9	226.3	227.1	226.4	227.3	27077	C.122	226.4	225.3	226.2	225.5	228.1	227.4	6.822	278.7	227.5	226.3	226.4	226.5	226.2	227.3	226.8	226.8
Lean	LPM	FT-223	159.9	162.1	165.3	160.8	162.6	163.3	159.2	164.5	160.0	161.9	159.9	164.3	162.5	165.7	156.9	163.1	160.0	163.5	155.5	6./cT	154.0	154.7	151.1	153.1	161 3	156.7	159.1	156.8	161.0	159.9	159.4	160.0	158.5	7.TqT	3 191 0'TOT	160.2	162.7	162.6	155.2	157.4	157.9	160.6	164.8	156.3	163.8	160.9	161.7	162.3	165.5	166.U 163.7	166.3
Emulsion	LPM	FT-219C	12.1	11.9	10.1	12.0	11.7	12.2	12.1	12.5	12.0	12.2	12.0	12.2	11.7	11.8	12.0	12.0	11.8	12.1	12.0	12.3	12.2	12.1	12.2	14.7 14.7	12.0	011	17.3	11.8	12.0	12.1	12.2	12.2	12.3	1.21	C.21	12.0	12.0	11.8	12.0	12.4	12.6	12.2	1.21	12.1	11.9	12.0	12.1	12.0	12.2	11.9	12.1
Rich	LPM	FT-229	50.5	50.6	0.0c	50.5	50.5	50.3	50.2	50.6	50.4	50.3	50.2	50.6	50.4	50.6	50.4	50.6	50.6	50.7	50.7	50.4	50.6	50.5	48.0	46.3	40.0	0.04	45.4	45.8	46.2	46.0	45,8	46.1	47.8	41.1	0.64	47.6	47.9	47.4	48.0	47.9	48.1	48.3	41.0	48.2	47.6	47.8	48.3	47.4	48.3	48.5	47.9
Doctor		\$Time	14:45:00	14:46:00	14.47.00	14:49:00	14:50:00	14:51:00	14:52:00	14:53:00	14:54:00	14:55:00	14:56:00	14:57:00	14:58:00	14:59:00	15:00:00	15:01:00	15:02:00	15:03:00	15:04:00	15:05:00	15:06:00	15:07:00	15:08:00	15:09:00	00.01.51	00.11.01	15-13-00	15:14:00	15:15:00	15:16:00	15:17:00	15:18:00	15:19:00	15:20:00	00-CC-31	15-23-00	15:24:00	15:25:00	15:26:00	15:27:00	15:28:00	15:29:00	00:02:CT	15:32:00	15:33:00	15:34:00	15:35:00	15:36:00	15:37:00	15:38:00	15:40:00
Test No. 5		\$Date	10/01/2018	10/01/2018	8102/10/01	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	010C/10/01	0107/10/01	81UC/1U/UT	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	8107/10/01	810C/10/01	8102/10/01	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	8102/T0/01 8102/10/01	0102/10/01 8102/10/01	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	

BH dP	mmH20	PDT-622	291.0	309.6	317.9	304.1	317.6
BH Inlet	mmH20	PT-615	-87.6	-94.4	-89.4	-86.5	-89.0
SDA Inlet	mmH20	PT-249	0	0	0	0	0
Incinerator SDA Inlet	mmH20	PT-242A	-6.60	-12.95	-10.85	-7.85	-9.45
Stack	Degrees C	TE-258	183.4	183.4	183.4	183.4	182.3
SDA	Degrees C	TE-204	193.5	193.5	193.0	192.0	191.0
Quench	Degrees C	TE-203	486.9	487.2	486.7	486.9	486.9
Secondary	Degrees C	TE-241	1137.7	1138.4	1143.5	1144.9	1145.0
Primary	Degrees C	TE-240	1560.1	1559.9	1559.6	1557.5	1561.1
Stack	m3/h	FT-260C	106987	106742	106502	108812	106111
Secondary	m3/h	PV-209	13708	13764	13736	13657	13629
Primary	m3/h	PV-236	14140	14140	14942	14672	14140
PAC	Lbs/h	SC-PAC-FT	23.0	22.2	23.0	21.7	21.9
Leachate	LPM	PV-211	28.3	29.0	29.2	28.9	29.1
TDU Flow	SCFM	FT-313	235.7	258.2	259.1	258.5	257.3
Alkaline TDU Flow TDU Flow Leachat	IPM	FT-313B	3.9	4.3	4.3	4.3	4.3
	1	PV-207	226.7	227.8	227.3	228.3	227.8
Lean	LPM	FT-223	165.1	151.3	144.2	163.5	151.9
Emulsion	LPM	FT-219C	11.9	12.2	12.1	12.2	12.1
Rich	LPM	FT-229	48.2	48.2	47.9	47.8	48.1
B arranova	dotion on	\$Time	15:41:00	15:42:00	15:43:00	15:44:00	15:45:00
Test No. 5		\$Date	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018

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\$Date	\$Time	FT-229	FT-219C	FT-223	PV-207	FT-3138	FT-313	PV-211	SC-PAC-FT	PV-236	PV-209	FT-260C	TE-240	TE-241	TE-203	TE-204	TE-258	PT-242A	PT-249	PT-615	PDT-622
10/01/2018	15:41:00	48.2	11.9	165.1	226.7	3.9	235.7	28.3	23.0	14140	13708	106987	1560.1	1137.7	486.9	193.5	183.4	-6.60	0	-87.6	291.0
10/01/2018	15:42:00	48.2	12.2	151.3	227.8	4.3	258.2	29.0	22.2	14140	13764	106742	1559.9	1138.4	487.2	193.5	183.4	-12.95	0	-94.4	309.6
10/01/2018	15:43:00	47.9	12.1	144.2	227.3	4.3	259.1	29.2	23.0	14942	13736	106502	1559.6	1143.5	486.7	193.0	183.4	-10.85	0	-89.4	317.9
10/01/2018	15:44:00	47.8	12.2	163.5	228.3	4.3	258.5	28.9	21.7	14672	13657	108812	1557.5	1144.9	486.9	192.0	183.4	-7.85	0	-86.5	304.1
10/01/2018	15:45:00	48.1	12.1	151.9	227.8	4.3	257.3	29.1	21.9	14140	13629	106111	1561.1	1145.0	486.9	191.0	182.3	-9.45	0	-89.0	317.6
10/2018		Waste Flows	2	okozanozninozonozmu složske			Nor-Annanalisation considerated and	-	Flows	Air Flows		Te	Temperatures	S	ALL-SCIED SALLSONCONCOUNTS IN A VI	Wednesdawaria a contraction of the second		Pressures	and the second		
tot I mains		Rich	Emulsion	Lean	Alkaline	Alkaline TDU Flow TDU Flow		Leachate	PACFlow	Primary	Secondary	Stack	Primary	Primary Secondary	Quench SprayDryer	prayDryer	Stack Ir	Incinerator SDA Inlet SD Outlet	SDA Inlet S		Baghouse
Test 5		FT-229	FT-219C	FT-223	PV-207	FT-313B	FT-313	PV-211	SC-PAC-FT	PV-236	PV-209c	FT-260c	TE-240	TE-241	TE-203	TE-204	TE-258	PT-242A	PT-249	PT-615	PDT-622
Max		50.8	12.6	166.3	229.3	4.3	260.4	30.7	23.0	15993	14017	110253	1585.6	1179.9	489.3	202.5	188.7	-0.80	0.0	-86.5	320.9
Min		45.4	11.7	144.2	224.3	3.9	233.0	28.2	21.6	14140	13523	104920	1552.1	1128.0	480.4	189.0	180.2	-26.80	0.0	-119.7	254.8
Average		48.6	12.1	159.9	226.6	4.1	247.3	29.1	22.4	14717	13745	107509	1568.4	1152.0	485.9	194.8	183.7	-12.33	0.0	-100.7	296.8
Variance		2.8	0.0	19.5	1.1	0.0	146.3	0.2	0.2	159595	11619	1722050	118.8	238.3	5.2	17.6	6.2	41.01	0	80.8	293.9
and the second se	and a second sec		of the second		www.www.www.www.www.www.		Supercontent internet super-	-	Non-the second sec	And a subsection of the subsec	-	Parameter contractor and the second	WARRY LOUIS CONTRACTOR DURING CONTRACTOR		distinguisticon and a state	NOTITIESEMENT	and the second se				

BH dP	mmH20	PDT-622	261.1	288.1	272.1	312.1	271.0	310.8	263.8	303.0	260.7	288.1	288.1	307.5	281.3	308.2	294.6	302.7	278.3	288.8	305.5	313.1	300.4	309.6	293.1	301.5	277.3	287.9	307.6	310.4	302.2	311.1	294.2	301.3	278.7	289.5	306.4	311.0	301.4	311.4	292.4	301.0	281.1	290.0	300.0	307.4	305.1	311.2	294.3	300.7	277.2	286.4	305.2	311.0	303.2	287.6	294.1
BH Inlet	mmH20	PT-615	-112.8	-96.3	-112.2	-91.1	-117.0	-88.8	-113.3	-97.3	-113.7	-95.0	-110.8	-87.6	-109.4	-88.1	-107.8	-93.9	-101.0	-90.5	-92.9	-86.4	-94.0	-84.8	-99.5	-92.1	-97.2	-88.8	-90.7	-83.3	-90,3	-82.7	-97.2	-89.7	-93.9	-90.7	-90.8	-84.6	-88.6	-82.6	-94.2	-89.0	-96.1	-89.2	-86.6	-80.3	-90.7	-81.6	-93.8	-87.3	-87.8	-84.6	-85.6	-81.6	-85.1	-89.6	-93.5
SDA Inlet	mmH20	PT-249	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Incinerator SDA Inlet	mmH20	PT-242A	-25.45	-13.55	-24.75	-9.80	-29.25	-7.80	-27.60	-14.10	-26.65	-13.35	-27.45	-7.60	-25.20	-8.05	-23.35	-11.30	-18.55	-9.75	-11.00	-7.80	-12.30	-5.10	-15.85	-9.85	-14.20	-8.65	-00.6-	-4.40	-8.55	-4.40	-13.15	-7.80	-12.55	-10.05	-8.90	-5.50	-6.90	-2.90	-10.65	-7.15	-13.55	-8.55	-7.90	-3.80	-9.30	-2.30	-10.50	-5.75	-5.50	-4.45	-5.05	-4.45	-5.35	-6.00	-11.80
Stack	Degrees C	TE-258	182.4	182.4	182.4	182.4	182.4	182.4	182.4	182.4	183.4	183.4	183.4	183.4	183.4	183.4	183.4	183.4	183.4	183.4	183.4	183.4	183.4	184.4	184.4	184.4	184.4	184.4	184.4	184.4	184.4	184.4	184.4	184.4	185.4	185.4	185.4	185.4	185.4	185.4	185.4	185.4	185.4	185.4	185.4	185.4	185.4	185.4	185.4	185.4	185.4	185.4	185.4	185.4	185.4	185.4	185.4
SDA	$\overline{\mathbf{O}}$	TE-204	192.0	192.5	192.5	192.5	192.5	193.0	193.0	193.0	193.0	193.5	193.5	193.5	193.5	193.5	193.5	194.0	194.0	194.5	194.5	195.0	194.5	195.0	195.0	195.0	195.0	195.0	195.0	195.0	195.5	195.5	195.5	196.0	196.0	196.0	196.0	196.0	196.0	196.0	196.0	196.0	196.0	196.0	196.0	196.0	196.0	196.0	196.5	196.5	196.0	196.0	196.5	196.0	196.0	196.0	195.5
Quench	Degrees C	TE-203	486.7	487.1	487.0	486.6	486.9	487.0	487.2	487.2	487.1	487.1	487.4	487.1	487.4	487.3	487.3	487.5	487.7	487.9	488.4	488.1	488.7	488.2	488.2	488.6	488.9	488.7	488.8	488.9	488.8	489.1	489.6	489.6	489.6	489.8	489.8	489.8	489.8	489.8	490.1	490.2	490.4	490.6	490.2	490.2	490.6	490.4	490.8	490.5	490.8	490.5	490.9	490.9	491.0	491.2	491.3
Secondary	Degrees C	TE-241	1139.5	1138.5	1138.8	1138.3	1140.7	1140.9	1142.1	1139.5	1139.2	1137.6	1137.7	1137.4	1141.2	1140.6	1141.7	1141.2	1140.7	1139.6	1140.5	1140.8	1142.7	1142.2	1144.3	1142.1	1142.0	1141.3	1142.7	1143.8	1146.3	1145.1	1146.3	1145.1	1144.0	1143.5	1143.9	1145.4	1145.9	1146.5	1146.6	1145.3	1144.2	1144.4	1144.3	1145.2	1146.1	1145.6	1144.7	1144.7	1143.5	1145.5	1145.6	1146.9	1145.7	1147.3	1143.1
Primary	Degrees C	TE-240	1556.6	1557.9	1555.4	1556.0	1558.9	1557.4	1557.6	1557.8	1558.0	1557.1	1556.4	1557.1	1556.5	1555.5	1555.6	1554.6	1556.1	1555.8	1555.5	1556.8	1556.4	1559.5	1557.4	1558.0	1559.5	1557.5	1558.4	1558.4	1558.9	1559.8	1557.6	1555.9	1559.3	1559.9	1559.5	1558.1	1559.5	1559.1	1560.4	1559.6	1556.3	1556.8	1556.9	1559.4	1556.4	1559.4	1558.4	1557.3	1556.5	1555.5	1555.5	1557.4	1558.3	1558.4	1557.3
Stack	m3/h	FT-260C	111468	106818	110596	106603	109319	106239	109516	107851	110966	107464	109793	107825	109980	106853	108572	107663	108744	106551	106280	106951	107221	105685	108248	106627	107359	106578	107186	106104	107131	106914	107375	106282	107919	105356	106825	106086	107338	105798	108293	106307	106349	105539	105959	106054	107639	105493	107503	106945	106540	105016	107279	105276	106135	104408	106970
Primary Secondary	m3/h	PV-209	13747	13747	13876	13652	13798	13770	13888	13781	13770	13646	13848	13590	13742	13775	13848	13747	13972	13607	13888	13680	13787	13685	13860	13607	13714	13601	13764	13528	13646	13680	13927	13657	13629	13775	13624	13635	13747	13618	13775	13674	13528	13669	13579	13697	13618	13500	13736	13635	13848	13753	13635	13635	13646	13674	13596
Primary	m3/h	PV-236	14935	14140	14666	14403	15198	14666	14935	14666	14659	15198	14672	14666	15191	14935	14403	14666	14935	14666	14403	14431	15986	14403	15198	15191	15460	14666	14140	16249	14140	14666	15198	14672	15730	14396	15191	14140	15198	15723	15205	14666	14396	14403	14140	14935	14666	14403	14396	14928	15454	15460	14403	15198	14672	14403	14666
PAC	Lbs/h	SC-PAC-FT	21.8	22.1	21.7	22.6	21.8	22.0	22.0	23.0	22.9	22.7	22.5	22.9	22.5	22.0	21.7	22.3	22.9	23.0	23.0	22.8	23.0	217	9.00	23.0	23.0	22.1	21.7	23.0	21.7	22.1	22.4	23.0	22.9	22.3	22.0	21.8	22.9	21.6	21.9	22.7	23.1	23.0	22.7	22.1	22.1	22.3	21.7	21.7	22.4	22.5	21.7	22.7	21.9	21.9	22.5
Leachate	LPM	PV-211	29.7	29.5	29.0	29.3	29.1	28.9	28.8	29.2	29.4	28.5	29.0	29.7	28.8	28.8	29.3	28.9	29.4	28.8	29.2	28.7	28.8	0.60	20.1	20.6	30.1	28.7	29.1	29.2	28.9	28.8	29.1	29.4	29.4	29.8	28.7	30.7	29.0	28.9	29.4	29.5	29.4	29.4	29.4	29.4	28.7	29.0	29.0	29.1	29.0	29.0	30.0	27.6	29.3	29.2	29.3
	SCFM	FT-313	257.4	258.0	257.5	259.2	234.9	233.1	235.1	234.5	234.9	233.6	233.2	235.9	258.9	258.7	252.5	257.6	257.8	258.0	259.0	259.6	259.6	259 D	758 9	726.2	250.2	259.3	235.2	246.0	249.2	218.5	257.9	256.1	261.4	258.6	258.3	258.4	258.3	252.5	253.8	259.7	258.2	228.8	241.1	254.7	257.9	254.6	252.9	248.3	256.7	259.5	257.5	259.0	255.7	223.6	230.1
TDU Flow TDU Flow	LPM	FT-313B	4.3	4.3	4.3	4.3	3,9	3.9	3.9	3.9	3.9	3.9	3.9	3.9	4.3	4.3	4.2	4.3	4.3	4.3	4.3	4.3	4.3	4 2	4.2	0 2	4.3	4.3	9.6	4.1	4.2	3.6	4.3	4.3	4.4	4.3	4.3	4.3	4.3	4.2	4.2	4.3	4.3	3.8	4.0	4.2	4.3	4.2	4.2	4.1	4.3	4.3	4.3	4.3	4.3	3.7	3.8
Alkaline	Md1	PV-207	225.5	228.2	226.5	228.0	227.2	226.8	225.7	226.1	224.9	226.2	224.8	228.0	225.9	228.9	226.8	228.7	226.2	226.1	224.1	226.2	224.8	2276	275.0	778 E	1 976	227.8	7.7.0	227.9	226.6	226.3	226.0	226.8	226.4	227.3	224.7	228.2	227.0	227.9	226.3	228.4	228.0	226.5	225.7	226.7	226.3	226.4	226.4	227.2	228.0	227.2	226.8	227.1	227.4	225.5	226.5 1
Lean	LPM	FT-223	162.1	163.6	162.3	163.4	161.6	162.2	162.7	163.6	164.2	163.4	164.6	163.7	163.7	164.6	163.5	163.6	164.3	163.6	163.2	163.0	163.8	164.2	162.0	2 V31	163.7	164.1	164.0	164.5	163.6	163.5	163.5	164.4	165.1	164.8	165.3	164.8	165.1	165.0	165.4	164.8	164.9	164.5	164.9	165.6	165.8	164.8	164.8	165.4	165.3	164.6	165.3	163.9	165.0	165.0	165.2
Emulsion	LPM	FT-219C	12.0	12.2	12.2	12.2	11.9	12.0	11.9	11.8	11.6	12.3	11.7	12.1	12.1	12.2	12.0	12.1	12.1	12.1	11.6	12.0	117	12 3	110	C C L	101	12.2	10.1	12.2	12.1	12.1	11.9	12.1	11.6	12.3	12.0	12.2	12.3	12.1	12.0	12.3	12.1	11.9	11.9	12.1	11.9	11.9	11.9	12.2	12.1	11.9	12.0	12.2	11.8	11.4	11.8
Rich	LPM	FT-229	48.4	47.6	47.7	47.6	47.7	47.6	48.2	48.0	47.9	47.6	47.9	48.1	47.9	48.4	47.9	47.7	47.6	47.7	47.6	47.6	47.7	C 81	17.5	376	0.14 C L V	48.2	47.8	47.4	47.8	48.0	48.2	48.5	47.3	48.2	48.0	47.9	47.6	47.5	47.6	48.3	47.5	47.4	48.1	48.0	47.5	48.3	47,4	47.7	47.6	48.0	47.8	47.5	48.2	47.1	47.1
boosts	deconcourse	\$Time	15:55:00	15:56:00	15:57:00	15:58:00	15:59:00	16:00:00	16:01:00	16:02:00	16:03:00	16:04:00	16:05:00	16:06:00	16:07:00	16:08:00	16:09:00	16:10:00	16:11:00	16:12:00	16:13:00	16:14:00	16-15-00	16.16.00	00.01.01	00.01.31	16-10-00	16-20-00	16-21-00	16:22:00	16:23:00	16:24:00	16:25:00	16:26:00	16:27:00	16:28:00	16:29:00	16:30:00	16:31:00	16:32:00	16:33:00	16:34:00	16:35:00	16:36:00	16:37:00	16:38:00	16:39:00	16:40:00	16:41:00	16:42:00	16:43:00	16:44:00	16:45:00	16:46:00	16:47:00	16:48:00	16:49:00
Test No. 6		\$Date	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	010C/10/01	010C/10/01	010C/10/01	0102/10/01 0102/10/01	10/01/2018	8102/TO/0T	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018

BH dP	mmH20	PDT-622	261.3	280.4	268.3	312.4	266.7	309.9
BH Inlet	mmH20	PT-615	-99.0	-90.4	-106.8	-91.0	-110.1	-89.2
SDA Inlet	mmH20	PT-249	0	0	0	0	0	0
ncinerator	mmH20	PT-242A	-15.25	-9.35	-21.80	-11.50	-24.30	-10.40
Stack	Degrees C	TE-258	185.4	185.4	185.4	185.4	184.3	184.3
SDA	Degrees C	TE-204	195.5	195.0	194.5	194.5	194.0	193.5
Quench	Degrees C	TE-203	491.3	491.1	491.4	491.6	491.2	491.1
Secondary	Degrees C	TE-241	1140.9	1137.8	1136.7	1134.5	1133.9	1132.4
Primary	Degrees C	TE-240	1555.3	1553.6	1555.4	1552.0	1553.5	1554.5
Stack	m3/h	FT-260C	109988	106844	109921	107222	109969	107776
Secondary	m3/h	PV-209	13618	13702	13607	13635	13641	13539
Primary	m3/h	PV-236	14403	14140	14140	14403	14140	14133
PAC	Lbs/h	SC-PAC-FT	23.0	22.0	22.7	21.7	22.6	22.2
Leachate	LPM	PV-211	28.4	29.3	29.3	28.7	29.3	29.5
TDU Flow	SCFM	FT-313	248.2	259.0	258.8	259.3	259.0	257.5
Alkaline TDU Flow TDU Flow	MGJ	FT-313B		4.3	4.3	4.3	4.3	4.3
Alkaline	LPM	PV-207	224.9	225.5	225.6	226.3	226.0	227.3
Lean	LPM	FT-223	1	165.7	165.0	164.9	165.1	164.5
Emulsion	LPM	FT-219C	11.3	11.5	11.4	11.8	11.4	11.9
Rich	Mdl	FT-229	47.0	47.1	47.0	47.3	46.5	46.6
lourna.	- <u> </u>	STime	16:50:00	16:51:00	16:52:00	16:53:00	16:54:00	16:55:00
Test No. 6		SDate	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018	10/01/2018

January 10/2018	Waste Flows	5					enste	Flows	Air Flows		Te	Temperatures	s		annan a sandijan a sana	-	Pressures			
	Rich	Emulsion	Lean	Alkaline	TDU Flow	TDU Flow	Leachate		Primary	Secondary	Stack	Primary	Secondary	Quench 5	t		ncinerator S	SDA Inlet S		saghouse
Test 6	FT-229	FT-219C	8 i i	PV-207	FT-313B	FT-313	PV-207 FT-3138 FT-313 PV-211	SC-PAC-FT	PV-236	PV-209c	FT-260c	TE-240	TE-241	TE-203	TE-204	TE-258	PT-242A	5	PT-615	PDT-622
Max		12.3	165.8	228.9	4,4	261.4	30.7		16249	13972	111468	1560.4		491.6			-2.30	0.0		313.1
Min	1	11.3	161.6	224.1	3.6	218.5	27.6	21.6	14133	13500	104408	1552.0		486.6	192.0	182.4	-29.25	0.0		260.7
Average	47.7	12.0	164.3	226.6	4.2	250.9	29.1		14763	13702	107336	1557.2	1142.2	489.2	194.8	184.4	-11.75	0.0		294.1
Variance	0.2	0.1	1	1.2	0.0	127.3	0.2	0.2	241907	10971	2361945	3.1	11.9	2.4	1.6	1.2	49.88	0	84.9	232.0
Considered and a second s	and the second s	and the second s	NAMES OF TAXABLE PARTY		STORE	Charles of the second s	ADDRESS AND ADDRESS AD	The second s	CONTRACTOR DO NOT THE OWNER OF THE OWNER OWNER OF THE OWNER	www.wateringenetics.com	And a second s	and a second sec	Contraction of the State Sta							

Test No. 1		со	HCI	CO2	H2O	тнс	02	Opacity	SO2
		PPM	PPM	%	%	PPM	%	%	PPM
\$Date	\$Time	AT-205corr		AT-213B	*****	AT-259corr	AT-261	AT-263	AT-264
10/01/2018	9:15:00	52.2	18.7	7.64	43.82	1.7	11.26	1.7	229.1
10/01/2018	9:16:00	50.7	18.1	7.60	43.42	1.6	11.30	2.3	227.7
10/01/2018	9:17:00	51.4	18.1	7.71	43.56	1.6	11.29	2.0	233.7
10/01/2018	9:18:00	52.6	19.6	7.78	44.05	1.6	11.26	2.1	237.5
10/01/2018	9:19:00	50.5	20.6	7.85	44.44	1.7	11.24	1.7	240.9
10/01/2018	9:20:00	48.5	18.9	7.83	44.15	1.7	11.19	2.3	239.2
10/01/2018	9:21:00	47.6	18.4	7.87	43.75	1.7	11.07	2.3	241.0
10/01/2018	9:22:00	54.7	18.4	7.74	43.65	1.8	11.07	2.0	227.9
10/01/2018	9:23:00	55.0	18.2	7.63	43.44	1.7	11.17	1.8	221.1
10/01/2018	9:24:00	57.1	16.2	7.56	43.57	1.8	11.47	2.0	221.2
10/01/2018	9:25:00	59.6	16.8	7.67	44.06	1.8	11.61	2.1	225.7
10/01/2018	9:26:00	55.1	18.6	7.74	44.09	1.6	11.40	1.9	229.7
10/01/2018	9:27:00	55.9	19.3	7.75	44.10	1.7	11.29	1.7	233.9
10/01/2018	9:28:00	57.2	19.5	7.73	43.86	1.7	11.25	2.2	233.9
10/01/2018	9:29:00	56.4	18.5	7.79	43.90	1,7	11.22	2.3	233.6
10/01/2018	9:30:00	57.6	18.9	7.81	44.12	1.6	11.25	1.8	231.1
10/01/2018	9:31:00	60.2	18.5	7.67	43.92	1.7	11.36	1.8	224.1
10/01/2018	9:32:00	60.5	18.4	7.56	43.68	1.7	11.45	2.0	220.4
10/01/2018	9:33:00	58.8	19.7	7.65	44.15	1.7	11.59	2.2	224.1
10/01/2018	9:34:00	57.6	21.8	7.81	44.55	1.7	11.45	1.8	235.0
10/01/2018	9:35:00	57.1	21.2	7.84	44.46	1.8	11.33	1.8	235.0
10/01/2018	9:36:00	53.8	0.0	7.75	44.05	1.7	11.28	2.2	232.6
10/01/2018	9:37:00	56.4	19.7	7.73	44.06	1.7	11.22	2.3	229.9
10/01/2018	9:38:00	57.7	17.5	7.70	43.66	1.8	11.19	1.6	225.7
10/01/2018	9:39:00	58.6	16.8	7.60	43.52	1.9	11.36	1.8	221.9
10/01/2018	9:40:00	57.3	18.2	7.55	43.15	1.7	11.36	2.0	221.9
10/01/2018	9:41:00	58.1	17.2	7.65	43.21	1.6	11.30	2.1	226.1
10/01/2018	9:42:00	59.6	17.4	7.71	43.57	1.7	11.29	1.6	229.5
10/01/2018	9:43:00	59.2	18.8	7.82	43.80	1.7	11.15	1.8	235.4
10/01/2018	9:44:00	58.6	17.6	7.84	44.20	1.9	11.19	2.1	242.3
10/01/2018	9:45:00	57.8	18.0	7.85	44.31	1.8	11.17	2.3	242.3
10/01/2018	9:46:00	57.4	19.0	7.82	44.47	1.8	11.18	1.6	233.3
10/01/2018	9:47:00	56.5	18.1	7.75	44.21	1.9	11.22	1.7	229.8
10/01/2018	9:48:00	59.0	17.5	7.74	44.22	1.8	11.40	1.9	233.4
10/01/2018	9:49:00	57.9	19.4	7.82	44.53	1.8	11.29	2.1	236.7
10/01/2018	9:50:00	58.1	18.3	7.82	44.40	1.8	11.28	1.6	239.7
10/01/2018	9:51:00	56.0	17.1	7.77	43.95	1.8	11.19	1.7	238.5
10/01/2018	9:52:00	55.1	18.5	7.73	43.65	1.7	11.14	2.1	238.5
10/01/2018	9:53:00	58.0	0.0	7.81	43.95	1.7	11.10	2.2	237.8
10/01/2018	9:54:00	57.4	17.5	7.82	43.97	1.8	11.11	1.5	234.2
10/01/2018	9:55:00	61.4	17.4	7.70	43.75	1.9	11.22	1.6	232.6
10/01/2018	9:56:00	60.4 F0.F	18.8	7.77	43.67	1.8	11.31	1.9	234.6
10/01/2018	9:57:00	59.5	18.9	7.82	43.89	1.8	11.23	2.0	237.1
10/01/2018	9:58:00	57.1	16.7	7.84	44.41	1.9	11.17	1.6	
10/01/2018	9:59:00	55.4	16.2	7.82	44.36	1.8	11.14	1.6	240.6 240.6
10/01/2018	10:00:00		16.7 18.9	7.80	44.14 43.94	1.9 1.8	11.22 11.15	2.1	233.9
10/01/2018	10:01:00		18.9	7.69	43.94	2.1	11.15	1.6	233.9
10/01/2018	10:02:00		19.1	7.69	43.51	1.9	11.12	1.8	227.0
10/01/2018	10:03:00		17.7	7.62	43.18	1.9	11.27	1.9	220.1
10/01/2018	10:04:00		16.7	7.03	43.49	1.8	11.41	2.1	237.8
10/01/2018			16.1	7.80	44.08	1.8	11.35	1.6	240.6
10/01/2018	10:06:00		10.8	7.80	43.85	1.9	11.11	2.0	240.6
10/01/2018	10:07:00		17.2	7.90	44.15	1.9	11.10	2.0	240.0
10/01/2018			15.5	7.90	44.10	1.9	11.17	2.0	243.4
10/01/2018	10:09:00		18.5	7.90	44.19	1.9	11.10	1.6	234.6
10/01/2018	10:10:00		16.4	7.61	44.23	1.9	11.18	2.1	234.0
10/01/2018	10:11:00		16.4	7.61	43.41	1.9	11.25	1.9	229.3
10/01/2018		· f	17.5	7.76	43.41	1.9	11.35	2.0	232.9
10/01/2018	10:13:00		17.1	7.78	43.89	1.9	11.18	1.6	232.5
10/01/2018	10:14:00		10.0	7.78	43.89	1.8	11.15	2.0	238.4
10/01/2010	1 10:13:00	1 00.0	1 1/1	1.75	1 77.13	1 1.0	<u></u>	1 2.0	1 270.5

January 10/2018	Analyzers							
	CO	HCI	CO2	H2O	THC	02	Opacity	SO2
Test 1	AT-205	AT-213A	AT-213B	AT-213C	AT-259	AT-261	AT-263	AT-264
Max	61.4	21.8	7.90	44.55	2.1	11.61	2.3	243.4
Min	47.6	0.0	7.55	43.15	1.6	11.07	1.5	220.4
Average	56.9	17.5	7.75	43.92	1.8	11.25	1.9	233.2
Variance	8.6	12.1	0.01	0.12	0.0	0.01	0.1	39.6

Toothin 3		CO 1		<u> </u>	1120		02	Onacity	502
Test No. 2		CO	HCI PPM	CO2	H2O	THC	02 %	Opacity %	SO2 PPM
ćData	C.T.	PPM	WINDOW CONTRACTOR	%	%	-	and a second		
\$Date	\$Time	AT-205corr		AT-213B		AT-259corr	AT-261	AT-263	AT-264
10/01/2018	10:25:00	60.1	16.6	7.91	43.96	1.9	10.99	1.9	239.5
10/01/2018	10:26:00	59.7	17.6	7.82	43.85	1.9	10.99	1.6	234.7
10/01/2018	10:27:00	61.3	17.3	7.70	43.57	1.8	11.17	1.9	233.5
10/01/2018	10:28:00	61.1	16.1	7.77	43.81	1.8	11.28	2.0	234.6
10/01/2018	10:29:00	63.6	16.6	7.86	44.57	1.9	11.31	1.7	239.3
10/01/2018	10:30:00	61.7	17.4	7.86	44.72	1.8	11.23	1.6	244.0
10/01/2018	10:31:00	60.2	18.3	7.84	44.55	1.9	11.20	2.0	245.6
10/01/2018	10:32:00	58.1	18.7	7.88	44.64	2.1	11.16	2.2	249.5
10/01/2018	10:33:00	56.0	17.6	7.83	44.72	2.1	11.14	1.6	236.3
10/01/2018	10:34:00	58.2	17.5	7.77	44.69	1.8	11.33	1.7	236.3
10/01/2018	10:35:00	59.0	17.0	7.77	44.48	1.9	11.38	1.8	242.7
10/01/2018	10:36:00	59.5	17.5	7.94	44.56	1.9	11.25	2.0	246.6
10/01/2018	10:37:00	59.0	17.5	8.05	44.85	2.1	11.05	1.5	251.8
10/01/2018	10:38:00	59.4	17.9	7.94	44.79	1.8	10.99	1.6	250.8
10/01/2018	10:39:00	58.0	18.3	7.88	44.89	1.8	11.16	2.0	250.8
10/01/2018	10:40:00	54.7	18.9	7.93	44.96	1.8	11.12	2.1	249.1
10/01/2018	10:41:00	58.6	18.2	7.93	45.00	1.8	11.12	1.5	244.9
10/01/2018	10:42:00	63.9	16.0	7.83	44.76	1.9	11.25	1.7	239.7
10/01/2018	10:43:00	61.2	16.1	7.74	44.20	1.9	11.21	1.8	236.9
10/01/2018	10:44:00	59.1	16.8	7.80	44.18	1.9	11.13	2.0	238.7
10/01/2018	10:45:00	66.2	18.5	7.90	44.43	2.1	11.12	1.5	248.4
10/01/2018	10:46:00	68.8	18.5	7.90	44.95	1.9	11.15	1.6	248.4
10/01/2018	10:47:00	61.8	17.8	7.86	44.40	1.9	11.08	2.1	245.1
10/01/2018	10:48:00	59.4	17.0	7.89	44.17	2.1	10.97	2.2	243.3
10/01/2018	10:49:00	60.0	17.4	7.85	44.39	2.1	11.02	1.5	236.6
10/01/2018	10:50:00	58.3	17.7	7.74	44.14	1.9	11.07	1.6	232.9
10/01/2018	10:51:00	61.6	17.9	7.77	44.77	2.1	11.35	1.9	236.7
10/01/2018	10:52:00	67.4	16.1	7.89	45.24	1.9	11.31	1.9	242.6
10/01/2018	10:53:00	67.9	15.2	7.89	45.34	1.9	11.25	1.5	246.2
10/01/2018	10:54:00	66.6	15.7	7.81	44.94	1.9	11.10	1.6	246.3
10/01/2018	10:55:00	65.3	0.0	7.80	44.87	1.9	11.15	2.0	247.9
10/01/2018	10:56:00	60.2	15.3	7.89	45.02	1.9	11.16	2.2	244.1
10/01/2018	10:57:00	59.4	14.8	7.77	44.61	2.1	11.13	1.6	234.2
10/01/2018	10:58:00	62.6	14.0	7.70	44.34	1.9	11.21	1.6	234.2
10/01/2018	10:59:00	63.5	14.2	7.80	44.62	1.9	11.35	1.9	240.5
10/01/2018	11:00:00	61.9	14.6	7.84	44.72	2.1	11.21	2.0	242.2
10/01/2018	11:01:00		14.6	7.89	45.15	2.2	11.18	1.6	248.4
10/01/2018	11:02:00	71.9	15.3	7.84	45.47	2.1	11.27	1.8	248.4
10/01/2018	11:03:00	70.3	14.6	7.81	45.29	2.1	11.25	2.0	245.6
10/01/2018	11:04:00	69.2	14.9	7.79	44.93	1.8	11.08	2.1	237.6
10/01/2018	11:05:00		14.3	7.77	44.82	1.9	11.09	1.6	233.4
10/01/2018	11:06:00	69.3	15.4	7.70	44.48	2.1	11.25	1.9	229.8
10/01/2018	11:07:00	67.4	16.0	7.72	44.48	1.9	11.31	1.9	232.0
10/01/2018	11:08:00		15.5	7.86	45.16	1.9	11.30	2.0	238.7
10/01/2018	11:09:00		14.7	7.85	45.14	1.9	11.16	1.5	243.8
10/01/2018	11:10:00		16.3	7.84	45.09	2.1	11.16	1.9	243.8
10/01/2018	11:11:00		16.6	7.94	45.71	1.9	11.29	2.2	247.5
10/01/2018	11:12:00		15.1	7.91	45.39	1.9	11.14	2.1	244.1
10/01/2018	11:13:00		14.8	7.79	44.95	1.9	11.10	1.6	234.9
10/01/2018	11:14:00		14.7	7.71	44.62	1.9	11.27	2.1	233.6
10/01/2018	11:15:00		15.0	7.83	45.18	2.0	11.43	2.0	238.2
10/01/2018	11:16:00		15.6	7.91	45.50	2.2	11.24	2.0	242.6
10/01/2018	11:17:00		15.6	7.90	45.40	1.9	11.14	1.6	245.8
	11:18:00		16.1	7.87	45.13	1.9	11.03	2.1	247.1
			16.7	7.92	44.90	2.1	10.97	2.1	247.1
10/01/2018	11:19:00		1 10.7			2.1	10.98	1.9	243.5
10/01/2018	11:19:00	******	172	7 97				1 1.2	1
10/01/2018 10/01/2018	11:20:00	63.2	17.2	7.92	45.24			1.6	235.8
10/01/2018 10/01/2018 10/01/2018	11:20:00 11:21:00	63.2 64.6	16.4	7.80	44.54	2.1	10.99	1.6	235.8
10/01/2018 10/01/2018 10/01/2018 10/01/2018	11:20:00 11:21:00 11:22:00	63.2 64.6 65.5	16.4 15.4	7.80 7.76	44.54 44.36	2.1 1.9	10.99 11.08	2.0	234.0
10/01/2018 10/01/2018 10/01/2018	11:20:00 11:21:00	63.2 64.6 65.5 67.6	16.4	7.80	44.54	2.1	10.99		

January 10/2018	Analyzers							
	СО	HCI	CO2	H2O	THC	02	Opacity	SO2
Test 2	AT-205	AT-213A	AT-213B	AT-213C	AT-259	AT-261	AT-263	AT-264
Max	71.9	18.9	8.05	45.71	2.2	11.43	2.2	251.8
Min	54.7	0.0	7.70	43.57	1.8	10.97	1.5	229.8
Average	63.7	16.1	7.84	44.77	2.0	11.17	1.8	241.6
Variance	17.9	6.1	0.01	0.20	0.0	0.01	0.0	32.8

Test No. 3		CO	HCI	CO2	H2O	THC	02	Opacity	SO2
	*****	PPM	PPM	%	%	PPM	%	%	PPM
\$Date	\$Time	AT-205corr	AT-213A	AT-213B		AT-259corr	AT-261	AT-263	AT-264
10/01/2018	11:35:00	75.3	0.0	7.85	45.03	2.1	11.14	2.2	241.6
10/01/2018	11:36:00	75.1	17.5	7.74	44.81	2.1	11.13	1.5	233.4
10/01/2018	11:37:00	74.7	16.4	7.68	44.68	2.1	11.21	1.7	233.4
10/01/2018	11:38:00	72.7	16.2	7.77	44.84	1.8	11.25	1.9	238.7
10/01/2018	11:39:00	70.1	18.0	7.85	45.00	2.2	11.17	2.0	241.9
10/01/2018	11:40:00	77.2	18.4	8.01	45.38	2.2	11.02	1.5	257.9
10/01/2018	11:41:00	78.9	0.0	8.04	45.57	2.1	10.93	1.6	262.7
10/01/2018	11:42:00	74.4	17.9	8.00	45.30	2.0	10.87	2.0	259.2
10/01/2018	11:43:00	75.4	16.8	8.04	45.76	2.0	10.89	2.2	255.3
10/01/2018	11:44:00	73.2	16.3	8.02	45.81	2.1	10.91	1.5	249.1
10/01/2018	11:45:00	69.3	16.7	7.90	45.30	1.9	11.01	1.7	239.8
10/01/2018	11:46:00	66.7	17.1	7.85	45.07	2.1	11.06	1.9	237.9
10/01/2018	11:47:00	65.0	17.7	7.90	44.94	1.9	10.94	2.0	241.3
10/01/2018	11:48:00	65.5	19.2	8.02	44.92	2.0	10.77	1.6	247.7
10/01/2018	11:49:00	68.5	19.0	8.03	45.21	2.0	10.81	1.7	249.1
10/01/2018	11:50:00	69.3	19.2	8.00	45.46	2.0	10.88	2.0	250.4
10/01/2018	11:51:00	69.5	19.1	8.03	45.60	2.0	10.86	2.2	248.7
10/01/2018	11:52:00	65.4	18.4	7.93	45.40	2.1	10.93	1.5	236.7
10/01/2018	11:53:00	64.1	18.5	7.81	44.82	1.9	10.94	1.7	229.7
10/01/2018	11:54:00	66.3	17.9	7.82	44.56	2.1	11.06	1.9	212.3
10/01/2018	11:55:00	82.8	19.3	7.90	45.35	2.1	11.08	2.0	164.8
10/01/2018	11:56:00	89.8	18.4	7.89	45.61	2.1	11.14	1.5	150.7
10/01/2018	11:57:00	91.9	16.9	7.80	45.21	1.9	11.08	1.7	136.0
10/01/2018	11:58:00	95.1	16.9	7.82	45.31	1.9	11.15	2.1	128.9
10/01/2018	11:59:00	108.0	14.9	7.85	45.24	2.1	11.06	2.1	97.4
10/01/2018	12:00:00	122.8	16.4	7.75	44.97	2,1	11.06	1.6	59.6
10/01/2018	12:01:00	125.3	0.0	7.68	44.97	1.9	11.23	1.8	53.2
10/01/2018	12:02:00	108.1	14.2	7.58	44.56	2.2	11.41	1.9	46.4
10/01/2018	12:03:00	90.7	13.3	7.57	44.59	1.9	11.39	1.9	46.4
10/01/2018	12:04:00	74.7	13.9	7.57	44.40	2.1	11.35	1.5	48.4
10/01/2018	12:05:00	89.1	13.3	7.59	44.32	2.2	11.35	1.9	48.4
10/01/2018	12:06:00	96.6	12.8	7.66	44.55	2.1	11.39	2.0	48.4
10/01/2018	12:07:00	127.9	12.4	7.70	44.53	2.2	11.27	2.0	45.1
10/01/2018	12:08:00	146.1	13.3	7.62	44.40	2.1	11.31	1.6	43.0
10/01/2018	12:09:00	112.1	13.7	7.47	44.34	2.2	11.57	2.0	104.3
10/01/2018	12:10:00	62.0	12.1	7.54	44.32	2.2	11.59	1.9	164.2
10/01/2018	12:11:00	51.8	13.1	7.59	44.18	2.2	11.50	2.0	173.2
10/01/2018	12:12:00	48.5	13.6	7.72	44.49	1.9	11.35	1.6	193.2
10/01/2018	12:13:00	49.9	13.0	7.77	44.75	1.9	11.31	2.0	199.0
10/01/2018	12:14:00	51.5	13.7	7.91	45.28	2.1	11.25	2.1	209.0
10/01/2018	12:15:00	54.0	13.5	7.88	45.22	1.9	11.12	2.0	207.3
10/01/2018	12:16:00	51.9	13.0	7.76	44.57	2.1	11.00	1.6	199.7
10/01/2018	12:17:00	50.9	14.0	7.71	44.78	2.2	11.22	2.1	201.1
10/01/2018	12:18:00	52.4	14.4	7.74	44.96	2.2	11.30	2.0	203.5
10/01/2018	12:19:00		14.7	7.79	44.95	2.1	11.19	1.9	205.1
10/01/2018	12:20:00	52.4	13.5	7.82	45.19	2.1	11.16	1.6	210.4
10/01/2018	12:21:00		13.6	7.80	45.40	1.9	11.16	2.1	213.4
10/01/2018	12:22:00		14.9	7.96	45.58	1.8	11.07	2.2	216.5
10/01/2018	12:23:00		14.3	7.90	45.05	1.9	10.95	1.9	209.5
10/01/2018	12:24:00	57.2	12.9	7.76	44.67	2.2	11.10	1.6	201.5
10/01/2018	12:25:00		13.5	7.77	44.94	2.2	11.24	1.9	201.5
10/01/2018	12:26:00		14.9	7.82	45.25	2.2	11.27	2.0	206.2
10/01/2018	12:27:00		14.9	7.92	45.34	2.3	11.14	1.7	211.2
10/01/2018	12:28:00		13.9	7.95	45.26	2.2	11.04	1.7	211.2
10/01/2018	12:29:00		14.9	8.02	45.56	2.3	11.05	2.0	
10/01/2018	12:30:00		15.5	8.08	45.98	2.3	11.08	2.3	222.2
10/01/2018	12:31:00		15.6	8.07	45.94	2.5	10.94	1.6	217.5
10/01/2018	12:32:00		14.4	7.89	45.60	2.4	11.00	1.7	214.4
10/01/2018	12:33:00		14.1	7.86	45.25	2.4	11.00	2.1	212.5
10/01/2018	12:34:00		15.7	8.00	45.59	2.5	10.93	2.1	217.3
10/01/2018	· 12:35:00	62.1	16.1	8.04	45.78	2.5	10.90	1 1.0	1 210.5

January 10/2018	Analyzers							
	CO	HCI	CO2	H2O	THC	O2	Opacity	SO2
Test 3	AT-205	AT-213A	AT-213B	AT-213C	AT-259	AT-261	AT-263	AT-264
Max	146.1	19.3	8.08	45.98	2.5	11.59	2.3	262.7
Min	48.5	0.0	7.47	44.18	1.8	10.77	1.5	43.0
Average	72.8	14.7	7.83	45.08	2.1	11.12	1.9	187.6
Variance	470.5	15.6	0.02	0.20	0.0	0.03	0.0	4577.5

	Test No. 4		CO ·	HCI	CO2	H2O	THC	02	Opacity	SO2
P	and the second second second second	possessesses	PPM	PPM	%	%	PPM	%	%	PPM
L	\$Date	\$Time	AT-205corr	AT-213A	AT-213B		AT-259corr	AT-261	AT-263	AT-264
	10/01/2018	12:53:00	68,1	15.3	8.22	46.57	2.2	10.66	2.1	238.1
	10/01/2018	12:54:00	67.7	14.7	8.24	46.73	2.2	10.60	2.3	238.1
	10/01/2018	12:55:00	62.5	13.8	8.13	46.05	2.1	10.47	1.6	224.2
	10/01/2018	12:56:00	60.9	13.5	8.05	45.84	2.2	10.69	1.8	221.2
-	10/01/2018	12:57:00	63.7	13.2	8.12	46.31	2.3	10.85	2.0	226.4 229.8
	10/01/2018	12:58:00	60.6	13.6	8.23	46.31 46.47	2.3	10.66	2.1	229.8
	10/01/2018 10/01/2018	12:59:00 13:00:00	60.3 67.2	14.0 14.5	8.28 8.36	46.50	2.3	10.57 10.45	2.0	234.5
le l	10/01/2018	13:00:00	67.3	14.3	8.33	46.60	2.2	10.43	2.0	236.4
	10/01/2018	13:02:00	64.7	14.7	8.28	46.28	2.3	10.30	2.2	231.0
	10/01/2018	13:02:00	58.3	15.3	8.17	45.93	2.2	10.35	1.7	221.8
F	10/01/2018	13:04:00	61.0	15.4	8.12	46.12	2.3	10.58	2.1	221.8
ŀ	10/01/2018	13:05:00	64.2	0.0	8.19	46.53	2.4	10.88	2.1	224.6
F	10/01/2018	13:06:00	66.2	15.5	8.20	46.48	2.3	10.62	2.1	224.6
F	10/01/2018	13:07:00	68.2	15.8	8.23	46.39	2.2	10.60	1.7	229.3
F	10/01/2018	13:08:00	70.8	14.2	8.19	46.16	2.4	10.62	2.2	228.3
F	10/01/2018	13:09:00	72.5	14.2	8.22	46.44	2.4	10.68	2.2	231.0
F	10/01/2018	13:10:00	72.9	13.7	8.21	46.32	2.4	10.55	2.1	225.2
-	10/01/2018	13:11:00	71.9	14.1	8.13	45.96	2.4	10.53	1.7	218.3
ł	10/01/2018	13:12:00	76.4	16.1	8.09	46.22	2.4	10.82	2.3	217.0
	10/01/2018	13:13:00	71.9	14.4	8.20	46.40	2.5	10.77	2.1	221.3
l l	10/01/2018	13:14:00	72.1	14.6	8.24	46.87	2.7	10.74	2.1	225.4
	10/01/2018	13:15:00	73.8	15.1	8.20	46.60	2.6	10.58	1.7	228.1
Γ	10/01/2018	13:16:00	76.7	14.7	8.16	46.25	2.6	10.54	2.2	226.6
	10/01/2018	13:17:00	76.7	16.0	8.26	46.84	2.7	10.69	2.2	230.0
	10/01/2018	13:18:00	80.6	16.4	8.23	46.85	2.8	10.62	2.0	221.3
	10/01/2018	13:19:00	79.3	14.6	8.09	46.13	2.7	10.56	1.7	214.7
	10/01/2018	13:20:00	73.7	13.2	7.98	45.52	2.7	10.71	2.1	212.9
	10/01/2018	13:21:00	71.4	13.1	8.07	45.92	2.8	10.82	2.1	215.6
	10/01/2018	13:22:00	70.2	14.8	8.13	46.29	2.8	10.68	1.9	220.1
	10/01/2018	13:23:00	72.1	15.7	8.16	46.39	2.8	10.62	1.7	225.3
	10/01/2018	13:24:00	72.7	14.3	8.15	46.25	2.6	10.54	2.1	227.1
	10/01/2018	13:25:00	77.2	13.7	8.32	46.82	2.7	10.59	2.3	228.5
	10/01/2018	13:26:00	75.1	13.7	8.22	46.40	2.6	10.47	1.8	222.9
· ·	10/01/2018	13:27:00	77.1	14.6	8.06	45.96	2.6	10.53	1.7	214.6
	10/01/2018	13:28:00	81.6	14.3	8.05	46.01	2.5	10.67	1.9	214.6
	10/01/2018	13:29:00	79.0	13.4	8.13	45.95	2.5	10.67	2.0	217.1
	10/01/2018	13:30:00	77.9	13.3	8.22	46.56	2.7	10.69	2.0	222.9
	10/01/2018	13:31:00	77.9	12.1	8.24	46.65	2.8	10.63	1.6	226.2
, i i i i i i i i i i i i i i i i i i i	10/01/2018	13:32:00	80.3	11.7	8.17	46.44	2.6	10.56	1.8	229.0
	10/01/2018	13:33:00	81.1	12.8	8.18	46.48	2.4	10.58	2.2	230.4
	10/01/2018	13:34:00	82.7	14.6	8.21	46.67	2.4	10.52	2.3	226.8 219.8
	10/01/2018	13:35:00	80.5 81.3	13.8 14.4	8.18	46.56	2.6	10.51 10.79	1.7	219.8
· · · · · · · · · · · · · · · · · · ·	10/01/2018	13:36:00	77.5	14.4	8.07	45.62	2.5	10.79	2.0	207.4
	10/01/2018	13:37:00 13:38:00	77.5	15.4	8.07	45.44	2.7	10.71	1.6	209.5
l l l l l l l l l l l l l l l l l l l	10/01/2018	13:38:00	85.2	14.9	8.10	46.39	2.5	10.79	1.0	218.0
	10/01/2018	13:40:00	81.6	12.8	8.12	46.28	2.5	10.70	2.1	218.4
	10/01/2018	13:40:00	81.0	12.7	8.14	45.92	2.3	10.07	2.1	219.5
ŀ	10/01/2018	13:41:00	90.3	13.1	8.09	45.52	2.4	10.55	1.6	215.5
	10/01/2018	13:43:00	89.2	13.9	8.05	46.77	2.7	10.82	1.7	216.7
ŀ	10/01/2018	13:44:00	84.2	12.2	8.06	46.38	2.8	10.92	1.9	216.7
ŀ	10/01/2018	13:45:00	82.1	12.4	8.10	46.31	2.8	10.76	2.0	215.2
h h h h h h h h h h h h h h h h h h h	10/01/2018	13:46:00	76.3	12.5	8.13	46.35	2.8	10.76	1.6	215.2
ŀ	10/01/2018	13:47:00	76.9	12.1	8.08	46.49	2.7	10.81	1.7	218.1
	10/01/2018	13:48:00	79.6	11.8	8.11	46.51	2.7	10.84	2.1	221.4
	10/01/2018	13:49:00	79.1	12.4	8,13	46.58	2.7	10.75	2.2	217.9
	10/01/2018	13:50:00	80.1	11.9	8.11	46.27	2.5	10.73	1.5	212.4
	10/01/2018	13:51:00	76.6	10.8	7.97	45.64	2.5	10.86	1.7	207.4
ŕ	10/01/2018	13:52:00	77.6	12.0	7.98	45.85	2.5	11.03	1.9	208.2
.	10/01/2018	13:53:00	77.6	11.3	8.03	45.99	2.6	10.94	2.0	210.7
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January 10/2018	Analyzers							
	СО	HCI	CO2	H2O	THC	O2	Opacity	SO2
Test 4	AT-205	AT-213A	AT-213B	AT-213C	AT-259	AT-261	AT-263	AT-264
Max	90.3	16.4	8.36	46.87	2.8	11.03	2.3	238.1
Min	58.3	0.0	7.94	45.44	2.1	10.38	1.5	207.4
Average	74.5	13.6	8.15	46.30	2.5	10.66	1.9	222.1
Variance	54.6	4.8	0.01	0.11	0.0	0.02	0.1	57.5

Test No. 5		СО	HCI	CO2	H2O	THC	02	Opacity	SO2
		PPM	PPM	%	%	PPM	%	%	PPM
\$Date	\$Time	AT-205corr		AT-213B		AT-259corr	AT-261	AT-263	AT-264
10/01/2018	14:45:00	77.2	12.5	8.56	47.11	2.5	10.06	1.6	244.0
10/01/2018	14:46:00	76.1	12.5	8.50	47.08	2.5	10.16	1.7	244.0
10/01/2018	14:47:00	79.3	12.3	8.53	47.16	2.7	10.31	1.9	249.5
10/01/2018	14:48:00	79.2	12.2	8.58	47.06	2.5	10.08	2.0	255.9
10/01/2018	14:49:00	80.0	13.1	8.61	47.07	2.3	9.98	1.6	261.9
10/01/2018	14:50:00	79.7	14.0	8.71	47.35	2.5	9.87	1.7	270.4
10/01/2018	14:51:00	82.6	13.2	8.78	47.51	2.3	9.86	2.1	279.3
10/01/2018	14:52:00	82.3	13.3	8.84	47.65	2.4	9.65	2.4	283.7
10/01/2018	14:53:00	85.8	14.1	8.86	47.53	2.2	9.62	1.6	279.7
10/01/2018	14:54:00	89.1	14.7	8.76	47.44	2.4	9.76	2.0	281.2
10/01/2018	14:55:00	90.9	15.6	8.84	47.67	2.5	9.89	2.0	286.3
10/01/2018	14:56:00	95.3	14.3	8.86	47.75	2.4	9.70	2.1	291.0
10/01/2018	14:57:00	100.2	13.5	8.92	48.11	2.5	9.55	1.6	300.9
10/01/2018	14:58:00	104.6	15.1	8.95	48.09	2.4	9.53	2.0	298.5
10/01/2018	14:59:00	107.0	16.1	9.00	48.41	2.4	9.59	2.2	302.7
10/01/2018	15:00:00	92.6	15.8	8.99	48.15	2.5	9.42	2.1	294.4
10/01/2018	15:01:00	83.9	15.2	8.92	47.98	2.6	9.46	1.6	284.1
10/01/2018	15:02:00	84.6	15.2	8.73	47.38	2.5	9.75	2.2	270.4
10/01/2018	15:03:00	81.8	15.6	8.68	46.86	2.5	9.79	2.0	269.3
10/01/2018	15:04:00	83.0	16.3	8.79	46.91	2.5	9.66	2.1	273.5
10/01/2018	15:05:00	103.4	15.7	8,85	47.78	2.5	9.63	1.7	287.5
10/01/2018	15:06:00	94.0	15.1	8.77	47.54	2.4	9.64	2.1	280.2
10/01/2018	15:07:00	66.7	13.2	8.70	46.99	2.4	9.77	2.2	265.5
10/01/2018	15:08:00	63.9	12.5	8.68	46.76	2.5	9.76	2.1	260.1
10/01/2018	15:09:00	52.0	13.9	8.64	47.04	2.7	9.98	1.6	252.6
10/01/2018	15:10:00	44.4	14.4	8.24	46.02	2.8	10.25	2.1	221.8
10/01/2018	15:11:00	43.3	14.5	8.17	46.21	2.8	10.58	1.9	206.0
10/01/2018	15:12:00	52.6	16.0	8.10	46.79	2.9	10.81	1.9	197.0
10/01/2018	15:13:00	54.6	15.5	8.10	47.14	3.0	10.81	1.6	199.9
10/01/2018	15:14:00	63.2	14.5	8.08	46.90	3.0	10.80	2.1	197.5
10/01/2018	15:15:00	63.5	14.8	8.07	46.60	3.1	10.79	2.1	197.5
10/01/2018	15:16:00	71.7	13.3	8.05	46.33	3.1	10.72	1.8	191.4
10/01/2018	15:17:00	84.1	13.8	7.92	46.05	3.0	10.85	1.7	185.1
10/01/2018	15:18:00	88.4	14.5	7.91	45.96	3.1	10.95	1.9	185.1
10/01/2018	15:19:00	91.8	14.1	7.99	46.20	3.1	10.96	1.9	192.4
10/01/2018	15:20:00	91.0	13.7	8.00	46.28	3.0	10.88	1.8	195.4
10/01/2018	15:21:00	76.9	13.7	8.14	46.13	2.9	10.64	1.6	207.3
10/01/2018	15:22:00	70.2	12.2	8.29	46.26	3.0	10.60	2.0	216.5
10/01/2018	15:23:00	67.9	12.6	8.37	46.34	3.1	10.55	2.1	217.9
10/01/2018	15:24:00	77.5	15.2	8.33	46.36	3.0	10.46	1.7	212.9
10/01/2018	15:25:00	78.4	15.0	8.17	45.97	3.1	10.44	1.7	209.9
10/01/2018	15:26:00	74.5	14.7	8.05	45.18	3.1	10.52	1.9	209.9
10/01/2018	15:27:00	66.1	14.4	8.27	46.08	3.1	10.58	2.0	216.0
10/01/2018	15:28:00	61.4	14.2	8.36	46.52	3.0	10.55	1.7	222.3
10/01/2018	15:29:00		14.3	8.43	46.78	3.1	10.33	1.7	230.0
10/01/2018	15:30:00	59.8	14.3	8.42	46.91	3.0	10.32	2.1	231.3
10/01/2018	15:31:00	59.6	13.9	8.48	46.88	2.9	10.19	2.2	232.7
10/01/2018	15:32:00	60.5	15.0	8.44	46.40	2.9	10.10	1.6	224.2
10/01/2018	15:33:00	62.2	14.1	8.34	46.29	2.8	10.14	1.7	220.2
10/01/2018	15:34:00	71.4	13.9	8.28	46.48	2.9	10.47	1.9	220.3
10/01/2018	15:35:00	68.4	14.1	8.35	46.49	2.8	10.48	2.1	220.3
10/01/2018	15:36:00	66.2	13.4	8.41	47.03	2.8	10.42	1.6	228.8
10/01/2018	15:37:00	68.4	13.5	8.44	47.24	2.8	10.39	1.7	232.9
10/01/2018	15:38:00	69.0	14.7	8.47	46.87	2.8	10.28	2.2	234.2
10/01/2018	15:39:00	70.6	16.3	8.45	46.77	2.8	10.21	2.3	229.3
10/01/2018	15:40:00	76.6	16.3	8.43	46.69	2.8	10.21	1.6	224.5
10/01/2018	15:41:00	75.5	14.4	8.29	45.99	2.8	10.27	1.7	218.3
10/01/2018	15:42:00	75.5	14.6	8.21	45.81	3.0	10.33	2.0	216.0
10/01/2018	15:43:00	70.8	15.3	8.42	46.45	2.9	10.37	2.0	225.9
10/01/2018	15:44:00		14.0	8.35	46.59	2.8	10.27	1.5	223.7
10/01/2018	15:45:00	48.5	13.2	8.03	45.79	2.9	10.31	1.7	206.7

January 10/2018	Analyzers	***************************************		alle and a superior a				
	СО	HCI	CO2	H2O	THC	O2	Opacity	SO2
Test 5	AT-205	AT-213A	AT-213B	AT-213C	AT-259	AT-261	AT-263	AT-264
Max	107.0	16.3	9.00	48.41	3.1	10.96	2.4	302.7
Min	43.3	12.2	7.91	45.18	2.2	9.42	1.5	185.1
Average	74.7	14.3	8.46	46.84	2.7	10.20	1.9	238.8
Variance	214.9	1.2	0.09	0.46	0.1	0.18	0.1	1145.0

Test No. 6		CO	HCI	CO2	H2O	THC	02	Opacity	SO2
Á		PPM	PPM	%	%	PPM	%	%	PPM
\$Date	\$Time	AT-205corr		AT-213B		AT-259corr	AT-261	AT-263	AT-264
10/01/2018	15:55:00	78.5	14.0	8.35	46.54	2.9	10.41	2.2	224.6
10/01/2018	15:56:00	78.9	16.3	8.24	46.30	2.9	10.38	1.6	218.3
10/01/2018	15:57:00	77.4	15.7	8.21	46.19	2.8	10.45	2.0	218.3
10/01/2018	15:58:00	78.9	15.1	8.33	46.70	2.9	10.64	2.0	223.8
10/01/2018	15:59:00	75.4	15.1	8.43	46.79	2.8	10.51	2.1	225.3
10/01/2018	16:00:00	70.2	13.2	8.52	46.86	2.8	10.32	1.6	232.7
10/01/2018	16:01:00	69.7	14.4	8.42	46.87	2.6	10.24	2.1	232.7
10/01/2018	16:02:00	66.8	15.3	8.45	46.86	2.6	10.23	2.2	232.7
10/01/2018	16:03:00	70.6	14.2	8.53	46.73	2.6	10.14	2.1	225.4
10/01/2018	16:04:00	75.5	13.7	8.45	46.56	2.5	10.18	1.6	220.7
10/01/2018	16:05:00	84.8	14.9	8.32	46.88	2.6	10.45	2.2	222.6
10/01/2018	16:06:00	81.1	14.2	8.46	47.00	2.4	10.44	1.9	228.3
10/01/2018	16:07:00	73.6	15.4	8.50	46.57	2.6	10.24	2.1	228.3
10/01/2018	16:08:00	72.8	16.1	8.55	47.00	2.4	10.11	1.7	235.5
10/01/2018	16:09:00	75.3	15.1	8.55	47.24	2.3	10.16	2.2	235.5
10/01/2018	16:10:00	75.2	15.0	8.57	47.12	2.3	10.13	2.2	238.0
10/01/2018	16:11:00	76.5	15.8	8.60	46.99	2.3	10.03	2.0	236.5
10/01/2018	16:12:00	77.9	15.8	8.53	46.73	2.3	10.01	1.7	230.0
10/01/2018	16:13:00	75.3	15.9	8.48	46.95	2.3	10.23	2.0	230.4
10/01/2018	16:14:00	74.1	15.3	8.54	46.99	2.3	10.29	2.1	230.4
10/01/2018	16:15:00	73.2	16.7	8.57	46.90	2.3	10.13	2.0	233.7
10/01/2018	16:16:00	74.2	16.8	8.58	47.03	2.2	10.08	1.6	238.6
10/01/2018	16:17:00	74.2		8.52	46.99	2.2	10.08	2.1	238.0
****			15.3		47.44		10.08	2.1	237.2
10/01/2018	16:18:00	78.5	14.0	8.61		2.4			}
10/01/2018	16:19:00	77.3	15.7	8.67	47.43	2.3	10.13	1.9	235.2
10/01/2018	16:20:00	75.9	15.3	8.51	46.84	2.3	10.15	1.8	229.4
10/01/2018	16:21:00	77.4	14.7	8.42	46.62	2.3	10.22	2.0	227.7
10/01/2018	16:22:00	73.6	15.5	8.57	46.83	2.4	10.22	2.1	232.6
10/01/2018	16:23:00	73.5	16.1	8.67	47.40	2.4	10.11	1.7	243.8
10/01/2018	16:24:00	72.3	16.3	8.64	47.21	2.3	9.98	1.7	243.8
10/01/2018	16:25:00	70.4	15.9	8.59	46.88	2.5	9.93	2.1	243.8
10/01/2018	16:26:00	70.2	15.5	8.65	47.28	2.3	10.02	2.2	246.5
10/01/2018	16:27:00	70.8	15.4	8.66	47.28	2.3	9.99	1.6	236.0
10/01/2018	16:28:00	72.6	15.3	8.46	47.15	2.5	10.18	1.7	231.6
10/01/2018	16:29:00	73.1	14.2	8.44	46.81	2.5	10.20	1.9	231.6
10/01/2018	16:30:00	78.1	14.4	8.62	47.09	2.3	10.16	2.0	236.5
10/01/2018	16:31:00	77.4	15.6	8.65	47.27	2.4	10.14	1.6	240.1
10/01/2018	16:32:00	74.5	16.0	8.65	47.17	2.2	10.02	1.7	243.1
10/01/2018	16:33:00	78.0	17.3	8.63	47.12	2.3	10.03	2.1	244.7
10/01/2018	16:34:00	80.9	15.9	8.65	47.43	2.3	9.98	2.2	247.9
10/01/2018	16:35:00	75.5	14.5	8.56	46.91	2.2	9.92	1.6	235.1
10/01/2018	16:36:00	74.5	15.1	8.53	46.77	2.2	10.05	1.8	232.7
10/01/2018	16:37:00	77.1	15.9	8.51	47.00	2.3	10.29	1.9	235.4
10/01/2018	16:38:00	76.9	16.1	8.57	47.01	2.3	10.21	2,0	237.3
10/01/2018	16:39:00	78.4	15.1	8.70	47.67	2.3	10.11	1.5	244.9
10/01/2018	16:40:00	78.1	13.1	8.67	47.32	2.1	9.98	1.6	243.5
10/01/2018	16:41:00	76.2	13.5	8.66	47.34	2.2	10.04	2.1	243.5
10/01/2018	16:42:00	76.1	15.4	8.64	47.30	2.2	10.02	2.2	239.1
10/01/2018	16:43:00	77.6	16.4	8.61	47.47	2.1	10.02	1.5	238.1
10/01/2018	16:44:00	80.1	16.0	8.51	47.12	2.2	10.03	1.6	235.8
10/01/2018	16:45:00	81.6	15.6	8.51	46.72	2.2	10.12	1.9	235.8
		+			÷				
10/01/2018	16:46:00	76.7	16.5	8.60	46.99	2.3	10.03	2.0	238.1
10/01/2018	16:47:00	76.6	14.8	8.60	47.25	2.1	9.95	1.6	243.9
10/01/2018	16:48:00	76.2	14.3	8.61	47.06	2.2	9.92	1.6	242.5
10/01/2018	16:49:00	74.8	15.0	8.69	47.64	2.2	10.09	2.0	245.9
10/01/2018	16:50:00	75.2	15.7	8.63	47.70	2.2	10.02	2.2	241.4
10/01/2018	16:51:00	74.8	13.9	8.46	47.08	2.1	10.08	1.6	220.5
10/01/2018	16:52:00	75.3	12.0	8.36	46.58	2.1	10.34	1.7	215.7
10/01/2018	16:53:00	74.8	12.0	8.39	46.50	1.9	10.39	1.9	217.3
10/01/2018	16:54:00	80.6	13.2	8.46	46.74	2.1	10.31	2.0	217.3
10/01/2018	16:55:00	82.9	13.5	8.52	47.23	2.0	10.38	1.6	220.7

January 10/2018	Analyzers	Analyzers							
	СО	HCI	CO2	H2O	THC	02	Opacity	SO2	
Test 6	AT-205	AT-213A	AT-213B	AT-213C	AT-259	AT-261	AT-263	AT-264	
Max	84.8	17.3	8.70	47.70	2.9	10.64	2.2	247.9	
Min	66.8	12.0	8.21	46.19	1.9	9.92	1.5	215.7	
Average	75.9	15.1	8.53	47.01	2.4	10.16	1.9	233.7	
Variance	11.3	1.2	0.01	0.10	0.0	0.03	0.1	71.4	